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## 300-FF-1 Operable Unit Remedial Investigation Phase II Report: Physical Separation of Soils Treatability Study

Date Published April 1994





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### ACRONYMS

	·
ARAR	applicable or relevant and appropriate requirements
ART	Alternative Remedial Technologies
ASTM	American Society for Testing and Materials
CERCLA	Comprehensive Environmental Response, Compensation,
D05	and Liability Act
DOE	U.S. Department of Energy
dpm	disintegration per minute
DQO	data quality objectives
ECN	Engineering Change Notice
Ecology	Washington Department of Ecology
EII	environmental investigation instructions
EPA	U.S. Environmental Protection Agency
FS	feasibility study
HEIS	Hanford Environmental Information System
ICP-OES	inductively coupled plasma - optical emission spectrometry
ICP-MS	inductively coupled plasma - mass spectrometry
	incremental cancer risk
ICR	
IT	International Technologies Laboratories low specific activity
LSA	TOW Specific activity
MTCA	Model Toxics Control Act
ORR	operational readiness review
PCB	polychlorinated biphenyls
PNL	Pacific Northwest Laboratory
QA	quality assurance
QC .	quality control
RCRA	Resource Conservation and Recovery Act
RESRAD	Residual Radioactivity Program
RI	remedial investigation
RL	Richland Operations
ROD	record of decision
TCLP	Toxicity Characteristic Leaching Procedure
WHC	Westinghouse Hanford Company
XRD	x-ray diffraction
XRF	x-ray fluorescence

#### UNITS OF MEASURE

### Radiation

- Roentgen (R) The roentgen is a unit for measuring exposure. It
  is defined only for effect on air. It applies only to gamma and
  x-rays. It does not relate biological effects of radiation to the
  human body.
- Rad (radiation absorbed dose) The rad is a unit for measuring absorbed does in any material. Absorbed dose results from energy being deposited by the radiation. It is defined for any material. It applies to all types of radiation. It does not take into account the potential effect that different types of radiation have on the body.
- Rem (roentgen equivalent man) The rem is a unit for measuring dose equivalence. It is the most commonly used unit and pertains to man. The rem takes into account the energy absorbed (dose) and the biological effect on the body due to the different types of radiation.

### Milli-Units

Units in roentgen, rad, and rem can be broken down into smaller, more usable units called milli-units. Milli-units are one one-thousandth of a whole unit. An example is:

### Dose Rate

Dose is the amount of radiation you receive. Dose rate is the rate at which you receive the dose.

### Contamination/Radioactivity

- Contamination units:
  - disintegrations per minute (dpm) or per second (dps)
  - counts per minute (cpm)
- Radioactivity is measured in the number of disintegrations radioactive material undergoes in a certain period of time.

One curie (unit of radioactivity) =

```
2,200,000,000,000 (2.2 \times 10<sup>12</sup>) dpm or 37,000,000,000 (3.7 \times 10<sup>10</sup>) dps.
```

For the radioactivity in air and water, the curie (Ci) or microcurie ( $\mu$ Ci) is most often used. One curie equals one million microcuries.

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#### 1.0 INTRODUCTION

This report describes the approach and results of physical separations treatability tests conducted under the *Comprehensive Environmental Response*, *Compensation*, and *Liability Act* (CERCLA) at the Hanford Site (Figure 1-1) in the North Process Pond of the 300-FF-1 Operable Unit (Figure 1-2). The report is in fulfillment of *Hanford Federal Facility Agreement and Consent Order* (Tri-Party Agreement) (Ecology et al. 1989) Milestone M-15-03B to submit the draft 300-FF-1 remedial investigation (RI) Phase II report to the U.S. Environmental Protection Agency (EPA) and Washington Department of Ecology (Ecology) for review by December 15, 1993.

Physical separation of soils was identified in the Phase I and II Feasibility Study Report for the 300-FF-1 Operable Unit (DOE-RL 1993a) as an alternative for remediation for which treatability studies were required to demonstrate effectiveness and provide information for the Phase III feasibility study (FS) to be submitted to EPA and Ecology by August 15, 1994 in fulfillment of Tri-Party Agreement Milestone M-15-03C. Physical separation of soils was identified as a remediation alternative due to the potential to significantly reduce the amount of contaminated soils prior to disposal. Additional treatment of fines by chemical extraction or other means was not tested due to the small fraction of fine soils that would require treatment, increased cost, system complexity, and concerns associated with potential environmental impact.

The scope of this report is limited to investigations and discussions of tests conducted in the north process pond. However, because contaminated soils are similar in the south process pond, process trenches, scraping disposal area, and sanitary trenches (DOE-RL 1993a), test results are expected to apply to these sites also. The volume of contaminated material in these areas and the north process pond is estimated at 645,000 yd³ (DOE-RL 1993a, Table C-1). Physical separation may also be used to reduce the amount of contaminated soils removed in burial grounds, and for radioactive surface soils (hot spots) throughout the 300-FF-1 Operable Unit.

Tests were conducted by Westinghouse Hanford Company (WHC), Richland, Washington, personnel using a system developed at Hanford consisting of modified EPA equipment integrated with screens, hoppers, conveyors, tanks, and pumps from the Hanford Site. The EPA equipment was transferred to the U.S. Department of Energy (DOE) by the EPA Risk Reduction Engineering Laboratory, Edison, New Jersey. Tests were conducted per 300-FF-1 Physical Separations CERCLA Treatability Test Plan (DOE-RL 1993b). Under CERCLA, no federal, state, or local permits were required (40 CFR 300.400[e][1]).

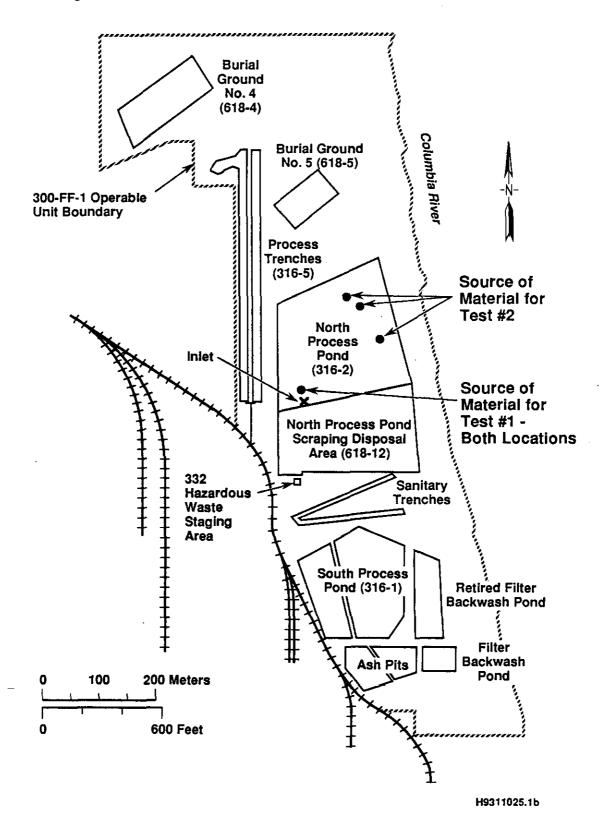
Except for toxic characteristic leaching procedures (TCLP) conducted by Thermo Analytical Inc. (TMA), Richmond, California, all offsite analytical support for testing of soil and process effluent samples was provided by International Technologies, Richland, Washington, and Data-Chem, Salt Lake City, Utah, laboratories. Offsite analysis of samples collected during water treatment tests was conducted by TMA. Soil sieving, screening analyses during physical separation and water treatment tests, and laboratory attrition scrubbing (high energy mixing of soils resulting in a scrubbing of particles as they attrite against each other) were conducted onsite by Pacific Northwest Laboratory (PNL), Richland, Washington.

Washington State Spokane Richland Portland 100 KW and KE Areas Gable Min. Route 11A Washington Public Hanford Ske Boundary Power Supply System 400 Area (FFTF) 5 Miles 3000 Area 5 Kilometers Richiand

Figure 1-1. The Hanford Site, Richland, Washington.

BP Map-1A

Figure 1-2. The 300-FF-1 Operable Unit, North Process Pond.



Because of contract delays, tests scheduled to be conducted by an off-site vendor using a commercial system will not be performed until after preparation of this report. The purposes of the vendor test are to demonstrate use of a commercial system, compare results with this report, show that attrition scrubber laboratory tests discussed in this report can be duplicated in the field, and to obtain additional scale-up and cost information for a full-scale system. A contract has been placed with Alternative Remedial Technologies, (ART), Tampa, Florida, to perform this work, currently scheduled to start in March 1994. On completion, a supporting document will be prepared by ART to document test results.

The treatability tests discussed in this report consisted of four parts, in which an estimated 84 tons of soil was processed: (1) a pre-test run to set up the system and adjust system parameters for soils to be processed; (2) a baseline run to establish the performance of the system - Test #1; (3) a final run in which the system was modified as a result of findings from the baseline run - Test #2; and (4) water treatment.

### 1.1 SITE DESCRIPTION

The 300-FF-1 Operable Unit is located north of the city of Richland, Washington, and borders the Columbia River (see Figure 1-1). It covers an area of 0.57 km² and consists of approximately 0.14 km² of liquid disposal waste sites. Waste sites within the 300-FF-1 Operable Unit are shown on Figure 1-2. Each of the sites is posted as a surface contamination area. The depth to groundwater beneath the 300-FF-1 Operable Unit ranges from 12 to 20 m (DOE-RL 1990).

The sanitary trenches received sewage from the 300 Area. The sewage is routed through vitreous tile pipes to septic tanks located between the north and south process ponds. Septic tanks are cleaned periodically and the sludge deposited in an adjacent pit near the southwest end of the trenches.

Burial grounds No. 4 and No. 5 are located on the northwest corner of the operable unit. Burial ground No. 4 contains elongated pits filled with solid waste and backfilled with clean soil. The burial ground is known to contain miscellaneous uranium-contaminated materials. Burial ground No. 5 was used for incineration and burial of uranium-contaminated and nonradioactive trash collected from the 300 Area. In addition, radioactive crucibles with aluminum-silicon or lead were disposed in burial ground No. 5.

The north and south process ponds and trenches were used between 1943 and 1975 to receive process sewer waste that included process water from nuclear fuels fabrication operations, cooling water, steam condensate, water treatment salts, and a wide variety of waste liquids from laboratory drains throughout the 300 Area. The north pond was constructed in 1948 when a dike in the south pond failed. As with the south pond, the north pond had no outlet; water was allowed to evaporate or infiltrate into the soils underlying the pond. The ponds were dredged periodically to improve infiltration. The dredged soils were spread on the dikes or buried in the north pond scrapings disposal area. Parts of the north process pond were used to dispose of fly ash from the 300 Area ash pits (Dennison et al. 1989). The ponds were deactivated in 1975 and currently do not contain any liquids.

The process trenches were constructed in 1975 to replace the process ponds to receive laboratory waste. In 1991, sediments were removed from the trenches and stockpiled at the north end as part of an expedited response action (ERA) in an effort to prevent the mobilization of soil-adsorbed contaminants to the groundwater. The process trenches are currently in use, but scheduled to be discontinued when the 300 Area Effluent Treatment Facility is on-line.

The north process pond scraping disposal area extends approximately 60 m south of the north process pond. It was used to dispose of uranium-contaminated sediment from the pond. The site has been backfilled with fly ash from the ash pits and covered with fill.

Other waste sites shown on Figure 1-2 include: the retired backwash filter pond, ash pits, and filter backwash pond. These are classified as no-hazard sites (DOE-RL 1993a).

A more detailed description of the 300-FF-1 Operable Unit is included in the Remedial Investigation/Feasibility Study Work Plan for the 300-FF-1 Operable Unit, Hanford Site, Richland, Washington (DOE-RL 1990) and the Phase I Remedial Investigation Report for the 300-FF-1 Operable Unit (DOE-RL 1993c).

### 1.2 WASTE STREAM DESCRIPTION

1

Phase I RI field activities to characterize the 300-FF-1 Operable Unit waste sites were completed February 1992. Soils investigations included surface radiation surveys and analysis of samples collected from boreholes and test pits. Results of these investigations are reported by DOE (DOE-RL 1993c).

### 1.2.1 Performance Levels and Risk Drivers

In these soil investigations and the risk assessment presented in the Phase I RI report (DOE-RL 1993c), uranium was found to be the primary contaminant of concern for 300-FF-1 Operable Unit. Uranium-238 and -235 pose the highest lifetime incremental cancer risk (ICR) (2E-03 and 1E-03, respectively [DOE-RL 1993c]). Cobalt-60 is also an important contaminant with a lifetime cancer risk of 2E-04.

Uranium-238, uranium-235, and cobalt-60 are the only contaminants in the operable unit with ICRs over 1E-04. According to the National Oil and Hazardous Substances Contingency Plan (40 CFR 300.430[c][2][i][A][2]) and Hanford Site Baseline Risk Assessment Methodology (DOE-RL 1993d), acceptable exposure levels are generally concentration levels that represent an ICR of between 1E-04 and 1E-06. It is noted that a radioactive contaminant concentration level associated with an ICR of 1E-04 or less is small enough to ensure satisfaction of any current radiation protection standards (e.g., DOE Order 5400.5) pertinent to the Hanford Site (DOE-RL 1993d).

The highest ICR posed by inorganic contaminants is due to chromium (2E-05); this risk is two orders of magnitude less than that for uranium-238, and assumes all chromium detected is hexavalent chromium (chromium remaining

in the process ponds after years of flushing is actually expected to be the less toxic trivalent chromium). The remaining inorganic and organic contaminants (including polychlorinated biphenyls [PCB]) are associated with ICRs more than two orders of magnitude less than the risk calculated for uranium-238.

According to the National Oil and Hazardous Substances Contingency Plan (40 CFR 300.430[c][2][i][A][2]) and DOE-RL (1993d), acceptable exposure levels of systemic toxins are concentration levels to which human populations, including sensitive subgroups, may be exposed without adverse effects during a lifetime or part of a lifetime (i.e, the hazard quotient has a value less than or equal to one). For the 300-FF-1 Operable Unit, the largest hazard quotient is 0.4, indicating that none of the contaminants pose a systemic toxic hazard.

### 1.2.2 Radioactivity of Soils

Radioactivity levels in soils near the inlet end and on the west side of the north process pond ranged from 15,000 to 35,000 disintegrations per minute  $(\text{dpm})/100~\text{cm}^2)$  as measured in the field in tests conducted during June 1993. Based on field observations, it is estimated that soils containing this level of radioactivity comprise <0.25 of the volume of the contaminated soils in the process ponds shown in Figure 1-2.

The surface radioactivity levels of soils in the remaining portions of the north pond were measured at near-background levels (500 dpm, as determined by Health Physics technicians at the site using hand-held instruments). These measurements are consistent with Phase I RI sampling results showing near-background radioactivity levels in test pits in the middle and east side of the trench.

The highest radioactivity in the north process pond is found in particles, visible as a "green material", containing uranium-238 and -235 isotopes. The green material is deposited in thin layers at a depth of 1 to 1.5 m below the pond surface on the west side of the pond (Dennison et al. 1989) and distributed as discrete particles and flakes in soils near the inlet of the ponds. This material resulted in many test complications.

### 1.2.3 Soil Characterization and Treatment Tests

Bench-scale, wet-sieving, and soil characterization tests using material from the north process pond were performed by PNL (Gerber et al. 1991). In the PNL tests, small soil particles were washed through sieves using water and chemical solutions. The results suggest that it is possible to separate coarse soil particles from fine soil particles with higher concentrations of contaminants. Although concentrated, contaminant levels of the fine particles were still low enough (Gerber et al. 1991) that there were no added problems related to handling or exposure to these soils. Also, in these tests, contaminants did not dissolve into the wash water; thus, water treatment needs were expected to be minimal. Testing of larger scale equipment was recommended to assess application of the technology to more coarse soils (Gerber et al. 1991).

X-ray diffraction (XRD) tests (Dennison et al. 1989) show that the mineralogical composition of the sediment is typical of sediments found throughout the Pasco Basin that consist predominantly of quartz and feldspar with small amounts of clay and mica.

Soil samples collected from the north process pond as part of Phase I RI for the 300-FF-1 Operable Unit were dry sieved and analyzed by Serne et al. (1992) to determine soil particle size distribution and contaminant distribution. Results, summarized in Tables 1-1, 1-2, and 1-3, show that the highest concentration of contaminants is in the fine soil particles. Based on performance levels specified in the test plan for this test, physical separation with water only and without the use of chemical additives at a size fraction of 0.425 mm may reduce the amount of contaminated soil in the north process pond by 90% (by weight) or more. A greater reduction in the amount of contaminated soils will be realized if soils can be separated at <0.425 mm.

### 1.3 REMEDIAL TECHNOLOGY DESCRIPTION

In this document, physical separation refers to a simple and comparatively low-cost water-based technology to separate soil particles by size fraction without the use of chemical processes so that the coarse fraction of soil will meet cleanup limits (test performance levels for the treatability test) and the amount of contaminated soils is significantly reduced.

Physical separation processes for soils are used extensively in the mining and mineral industries to assist in the recovery of valuable constituents. These physical separation processes have been demonstrated by the EPA Superfund Innovative Technology Evaluation Program for Hazardous Waste Remediation (EPA 1989) and used by the Defense Nuclear Agency to remediate radiologically contaminated coral sands (Kochen 1986). The technology was successfully applied in September 1993 to remediate chromium-contaminated soils at the King of Prussia Superfund Site in Winslow County, New Jersey (Rubin 1993).

A typical physical separations system includes: processes to separate coarse soils by particle size or density; additional processes to separate and/or scrub sand and sometimes silt-size particles; dewatering processes for each solids stream; and in-line water treatment processes to recycle and reuse water and thereby minimize the amount of contaminated water generated in the process. Following processing, contaminated soils (typically the fine fraction of soils) and water are disposed of or further treated, and those soils that meet regulatory cleanup limits are returned to the site.

Additional information on physical separation processes is provided by EPA in Technological Approaches to the Cleanup of Radiologically Contaminated Superfund Sites (EPA 1988).

Table 1-1 300-FF-1 North Pond Particle Size Distribution. (Serne et al. 1992)

	Fraction Sizes, mm												
Sample, g	>50	50 to 37.5	37.5 to 25	25 to 13.2	13.2 to 4.75	4.75 to 2	2 to 0.425	0.425 to 0.25	0.25 to 0.15	0.15 to 0.075	0.075 to 0.045	<0.045	Totals
1	238.48	655.89	690.83	495.57	153.95	206.92	556.20	47.43	21.26	12.54	5.38	1.76	3,086.21
2	1,050.08	270.96	387.31	278.75	244.93	125.78	488.21	145.39	57.63	46.32	28.77	46.51	3,170.64
3	620.32	127.61	917.82	358.37	174.51	138.45	812.37	28.55	44.54	31.62	22.66	39.25	3,316.07
Tot wt	1,908.88	1,054.46	1,995.96	1,132.69	573.39	471.15	1,856.78	221.37	123.43	90.48	56.81	87.52	9,572.92
% by wt	19.94	11.02	20.85	11.83	5.99	4.92	19.40	2.31	1.29	0.95	0.59	0.91	100.00

Table 1-2. 300-FF-1 North Pond Radiochemical Contaminants by Size Fraction. (Serne et al. 1992)

		Fraction Sizes, mm										
Constituent, pCi/g	>50	50 to 37.5	37.5 to 25	25 to 13.2	13.2 to 4.75	4.75 to 2	2 to 0.425	0.425 to 0.25	0.25 to 0.15	0.15 to 0.075	0.075 to 0.045	<0.045
Uranium-235												
Sam. 1	0.0408	0.0618	0.213	0.275	0.352	1.29	2.95	10.20	14.70	23.00	26.50	34.10
Sam. 2	0.0158	0.0765	0.113	0.117	0.291	1,13	1.02	3.05	5.07	6.69	7.99	8.09
Sam. 3	0.0362	0.0135	0.184	0.184	0.523	1.21	0.81	1.95	1.56	2.41	4.23	3.63
Avg.	0.0256	0.0597	0.180	0.207	0.378	1.22	1,51	4.44	5.46	7.45	8.24	6.61
Uranium-238												
Sam. 1	0.484	0.394	2.01	2.11	9.09	18.40	45.10	138.00	195.00	384.00	493.00	592.00
Sam. 2	0.254	0.576	2.74	1.10	1.39	14.10	15.50	51.90	105.00	158.00	151.00	167.00
Sam. 3	0.409	0.159	0.73	1.14	2.48	9.63	7.01	37.60	30.20	44.80	52.20	59.60
Avg.	0.333	0.412	1.56	1.55	3.79	14.67	20.65	68.50	93.51	149.76	143.98	127.38
Cobalt-60												
Sam. 1	0.10	0.10	0.10	0.10	0.10	0.10	0.66	0.100	0.10	0.10	0.10	0.10
Sam. 2	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.599	0.10	0.10	0.10	0.10
Sam. 3	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.100	0.10	1.20	3.57	0.10
Avg.	0.10	0.10	0.10	0.10	0.10	0.10	0.27	0.428	0.10	0.48	1.48	0.10
Cesium-137					,							
Sam. 1	0.10	0.104	0.16	0.10	0.10	0.10	0.742	0.100	0.10	0.10	0.10	0.10
Sam. 2	0.10	0.115	0.10	0.10	0.10	0.10	0.100	0.785	2.42	0.10	0.10	0.10
Sam. 3	0.10	0.100	0.10	0.10	0.10	0.10	1.440	0.100	0.10	2.07	0.10	0.10
Avg.	0.10	0.106	0.12	0.10	0.10	0.10	0.879	0.550	1.18	0.79	0.10	0.10

<u>1-9</u>

Table 1-3. 300-FF-1 North Pond Chemical Contaminants by Size Fraction. (Serne et al. 1992)

				Analyses	of Metals	in Each Si	ze Fractio	n (weighte	d averages)	a		
Contaminants, ppm	Fraction Sizes, AMR											
	>50 <sup>b</sup>	50 to 37.5 <sup>b</sup>	37.5 to 25 <sup>b</sup>	25 to 13.2 <sup>b</sup>	13.2 to 4.75	4.75 to 2	2 to 0.425	0.425 to 0.25	0.25 to 0.15	0.15 to 0.075	0.075 to 0.045	<0.045
Chromium	42.52	73.56	61.86	64.97	52.42	43.45	79.16	164.35	257.37	386.28	496.81	776.74
Manganese	985.59	1,271.05	1,290.62	1,259.52	1,098.24	2,489.10	1,504.14	1,296.83	1,627.82	1,560.16	1,554.08	1,585.17
Nickel	46.65	65.76	58.53	60.46	52.74	58.70	90.60	114.70	171.17	223.41	261.10	372.98
Copper	180.60	366.61	282.95	307.96	237.64	483.87	1,137.89	1,521.44	2,312.87	3,018.11	3,162.26	3,007.98
Zinc	80.14	97.30	110.04	102.74	88.88	111.11	133.54	114.13	147.38	163.46	185.03	227.04
Mercury	2.48	2.71	2.72	2.70	2.57	2.84	3.00	2.87	2.95	5.17	6.41	8.62
Selenium	0.78	0.85	0.85	0.84	0.81	0.88	0.91	0.83	0.80	1.04	0.87	0.98
Lead	9.33	8.15	8.40	8.37	8.92	12.55	13.26	21.84	31.26	40.90	50.98	64.96
Arsenic	1.45	1.48	1.45	1.46	1.45	2.29	2.70	4.41	6.36	8.18	9.74	10.67
Silver	5.22	5.63	5.83	5.70	5.41	5.30	8.56	33.57	66.51	92.84	119.36	177.45
Cadmium	5.11	5.15	5.31	5.23	5.15	5.51	5.12	5_14	5.50	5.47	7.10	6.14
Barium	274.45	135.00	316.03	241.72	251.76	846.12	660.69	743.81	843.61	840.05	840.98	923.60
Uranium	11.19	23.42	18.44	19.84	15.03	19.64	55.06	161.18	255.14	366.45	402.16	418.16

<sup>&</sup>lt;sup>a</sup>To simplify the table, only average values are shown; for more details refer to Serne et al. 1992.

background but the four largest size fractions were not analyzed due to the size of the material. Values are assumed to equal that of the largest fraction analyzed (13.2 to 4.75) (Serne et al. 1992).

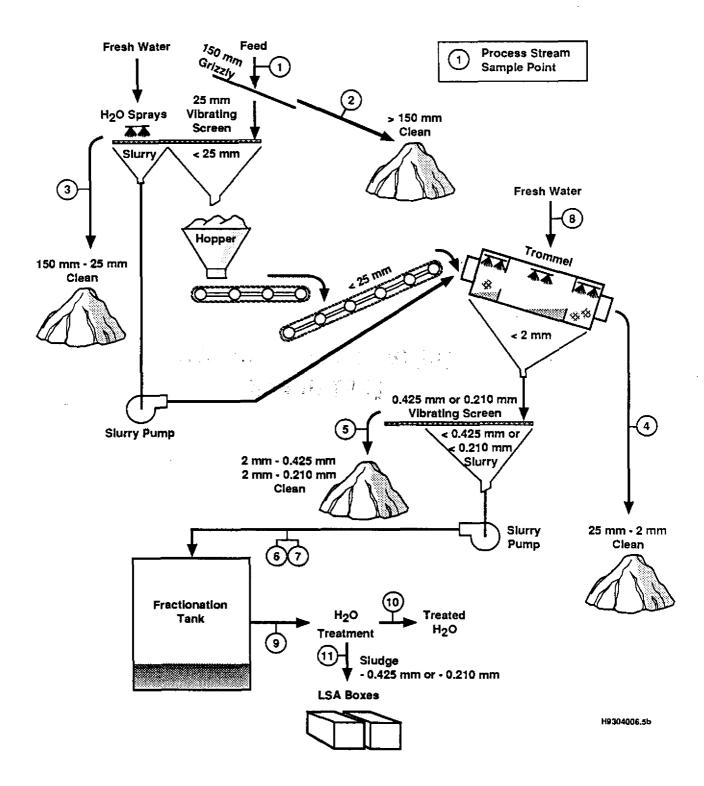
Many physical separations systems are commercially available, but were not used because services and equipment could not be obtained in a timely manner to meet the Tri-Party Agreement milestone for the test. Therefore, a system was designed and assembled by WHC personnel (Figure 1-3) composed of modified EPA equipment and components available on the Hanford Site. The system was not designed for long-term use, or as a well-integrated system.

The system consisted of the following:

- 150-mm bar screen (grizzly) to separate out material >150 mm
- hopper and 25-mm vibrating screen with water sprays to separate material >25 mm
- belt conveyor to move <25-mm size particles from hopper to a trommel
- trommel with water knives to wash >2-mm soils and screen material
   2 mm in diameter
- second vibrating screen with a U.S. National Bureau of Standards #40 (0.425-mm) or #70 (0.212-mm) wire mesh screen to separate particles
- fractionation tanks to contain effluent and fines <0.425 mm and serve as settling tanks
- off-line water treatment process
- fresh water supply tanks filled by truck
- B-25, low specific activity (LSA) boxes to contain <0.425-mm particles (per 49 CFR 173.403).

It is estimated that contaminated soil volumes in the 300 Area at Hanford could be reduced by 90% or more by separating coarse "clean" soils from contaminated soils (Serne et al. 1992). The "clean fractions" that meet cleanup or release limits (to be determined by EPA and Ecology) would be returned to their original locations. Less than 10% of the soil residuals would require additional treatment/disposal. It is estimated that there are over 600,000 yd<sup>3</sup> of contaminated soils in the 300-FF-1 Operable Unit alone (DOE-RL 1993a).

Figure 1-3. EPA Modified Physical Separation/Soil-Washing System.



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### 2.0 TEST OBJECTIVES AND RATIONALE

### 2.1 OBJECTIVES

The objective of these tests was to evaluate the use of water-based physical separations systems as a means of concentrating chemical and radio-chemical contaminants into fine soil fractions and thereby minimizing the amount of contaminated soils.

To date, no specific applicable, relevant, or appropriate requirements (ARAR) have been established for radioactive soils in the 300-FF-1 Operable Unit at Hanford. Therefore, DOE orders and WHC control manual standards were used as minimum goals for the test. The only potential ARAR for soils that is chemical-specific is the Model Toxics Control Act (MTCA) (RCW 70.105D), but no cleanup levels have been established for soils in the 300-FF-1 Operable Unit at Hanford. Per agreement between DOE, Richland Operations (DOE-RL), EPA, and Ecology (documented in February 27, 1992, 300-FF-1 meeting minutes), MTCA, Method C, industrial levels were selected as test performance levels. The test performance levels established as a goal for the test and background levels for contaminants identified in the test plan (DOE-RL 1993b) are shown in Table 2-1. These contaminants were determined to include the primary risk drivers identified in Phase I RI (DOE-RL 1993c).

Minimum goals for the treatability test included:

- 90% or greater weight reduction of contaminated soils (based on Serne et al. 1992).
- The clean fraction (90%) must meet test performance levels shown in Table 2-1. Test performance levels are less than or equal to:
  - <20  $\mu$ R/hr above background radioactivity (DOE 1990)
  - The Residual Radioactivity (RESRAD) Program, Versión 4.0, <25 mrem/hr (Gilbert et al. 1989).
  - WHC radioactive threshold concentrations for accessible soils (WHC 1991)
  - MTCA, Method C, industrial levels.
  - These test performance levels should not be considered as cleanup levels, which are yet to be established for Hanford soils.
- Perform analyses consistent with applicable EPA methods (EPA 1990) and test plan requirements.

Table 2-1. Background Levels of Contaminants and Test Performance Levels for Soil Treatability Tests.

Analyte	Units	Background Levels <sup>c</sup>	Test Performance Levels
Metals (inorganics) <sup>a</sup>	mg/kg		
Aluminum Antimony Arsenic Beryllium Cadmium Chromium Copper Iron Lead Manganese Mercury Nickel Silver Zinc		3,070 5.01 0.59 0.25 0.59 5.0 10.7 11,300 1.55 189 0.049 3.8 1.53 11.5	NA 1,400 188 31 1,750 3,200,000 130,000 NA NA 17,500 1,050 70,000 10,500 1,050,000
<u>Organics<sup>a</sup></u>	mg/kg	;	
1,2-dichloroethylene Methylene chloride Tetrachloroethylene Trichloroethylene		0 0 0 0	35,000 17,500 2,570 11,900
<u>PCB</u>	mg/kg (ppm)	0	17
Radiochemical Contaminants <sup>b</sup>	pCi/g		
Cesium-137 Cobalt-60 Uranium-235 Uranium-238		0 0 0 0	30 7.1 170 370

<sup>a</sup>Test performance levels for inorganic and organic contaminants are MTCA, Method C, industrial levels (Ecology 1993).

<sup>b</sup>Test performance levels for radionuclides are from WHC (1991).

<sup>c</sup>Background levels are values used for risk calculations from Phase I RI report (DOE-RL 1993c). A value of "O" was used for risk assessments for all organics, PCBs, and radionuclides.

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Water treatment was a secondary objective for the test. The primary goal of water treatment tests was to treat processed effluent to meet purgewater acceptance standards (Appendix A) so that water can be recycled in a full-scale system, and process water generated during the tests can be handled as purgewater (DOE-RL 1993b). The reason for selecting purgewater standards as test performance levels for treated water was that these levels were required by WHC personnel to discharge treated water to solar evaporation units onsite. The purgewater acceptance levels were also a reasonable and convenient criteria to recycle and reuse water in the soil treatment process. Purgewater acceptance standards are mostly 10 times drinking water criteria (maximum contaminant levels [MCL]) (WHC 1991). There is no regulatory requirement for selecting this as a test performance level.

### 2.2 POTENTIAL ARARS

Table 2-2 lists potential chemical- , location- , and action-specific ARARs to the soil treatability test. A final set of ARARs will be identified in the 300-FF-1 Operable Unit Phase III FS to be written at a later date.

### 2.3 DATA QUALITY OBJECTIVES

The primary sampling and analysis data quality objectives (DQO) were to:

- determine physical characteristics of soils
- determine the distribution and concentration of contaminants in the soils before and after a physical separation is made between the coarse material and the fine material
- evaluate separation efficiencies in relation to process parameters
- after processing, determine the concentration of contaminants of concern in the process water, both suspended and dissolved, and evaluate the effectiveness of water treatment methods
- obtain samples and analytical results of sufficient quality to document performance of the system or systems tested and determine if cleanup criteria can be met.

Samples collected during the test were analyzed using: EPA methods (EPA 1990), approved radioanalytical procedures, and the American Society for Testing and Materials (ASTM) procedures for measuring physical parameters. This meets EPA Level III DQO. Additional DQO for this test are defined in the 300-FF-1 Operable Unit work plan (DOE-RL 1990).

Table 2-2. Potential ARARs for the Soil Treatability Test. (Sheet 1 of 2)

Regulation	Citation	Applicability
FEDERAL		
Safe Drinking Water Act	40 CFR 141	Potentially Relevant
Federal Water Pollution Control Act (FWPCA), as amended by the Clean Water Act of 1977	33 USC 1251 et seq.	Potentially Relevant and Appropriate
Wild and Scenic Rivers	PL 100-605	Applicable
Clean Air Act	42 USC 7401 et seq.	Applicable
National Ambient Air Quality Standards	40 CFR 50	Applicable
National Emissions Standards for Hazardous Air Pollutants	40 CFR 61	Applicable
New Sources Performance Standards	40 CFR 60	Potentially Relevant and Appropriate
Toxic Substances Control Act	15 USC 2601 et seq.	Potentially Relevant and Appropriate
PCB Restrictions	40 CFR 761	Potentially Relevant and Appropriate
Atomic Energy Act	42 USC 2011 et seq.	Potentially Relevant and Appropriate
The Uranium Mill Tailings Control Act of 1978	PL 95-604, as amended	Potentially Relevant and Appropriate
Environmental Standards for Management, Storage and Disposal of Low Level Radioactive Waste	40 CFR 193	Applicable
Radiation Protection of the Public and the Environment	DOE Order 5400.5	To Be Considered
Radioactive Waste Management	DOE Order 5820.2A	To Be Considered
Safety Requirements for the Packaging of Fissile and Other Radioactive Materials	DOE Order 5480.3	To Be Considered
Radiation Protection for Occupational Workers	DOE Order 5480.11	To Be Considered
National Historic Preservation Act	16 USC 470 et seq.	Applicable
Endangered Species Act	16 USC 1531 et seq.	Potentially Relevant and Appropriate
Solid Waste Disposal Act as amended by the Resource Conservation and Recovery Act (RCRA)	42 USC 6901 et seq.	Applicable
TATE <sup>a</sup>		
Dangerous Waste Regulations	Ch. 173-303 WAC	Applicable
MTCA Cleanup Regulations	Ch. 173-340 WAC	Applicable
Minimum Functional Standards for Solid Waste Handling	Ch. 173-304 WAC	Applicable
Water Pollution Control	ch. 90.48 RCW	Applicable
State Waste Discharge Permit Program	Ch. 173-216 WAC	Applicable
, i		

Table 2-2. Potential ARARs for the Soil Treatability Test. (Sheet 2 of 2)

Regulation	Citation	"Applicability
STATE <sup>a</sup> (Cont.)		
Water Quality Standards for the State of Washington	Ch. 173-201 WAC	Applicable
Ambient Air Quality Standards and Emission Limits for Radionuclides	Ch. 173-480 WAC	Applicable
Radiation Protection - Air Emissions	Ch. 246-247 WAC	Applicable
Toxic Air Pollutants	Ch. 173-460 WAC	Applicable
Washington Clean Air Act	ch. 70.94 RCW	Applicable

<sup>&</sup>lt;sup>a</sup>As proposed by Ecology.

The primary data users include:

- DOE, EPA, and Ecology remedial project managers
- DOE, EPA and Ecology unit managers
- RI and FS coordinators
- technical contributors.

Data will be used to support final remediation decisions in FS. Evaluations and decisions will include the following categories:

- site characterization
- occupational health and safety
- risk assessments
- evaluating alternatives
- design of alternatives
- monitoring during remedial actions.

The following questions were answered by the treatability tests. (applicable sections that address these areas are in parentheses):

- Are agglomerates completely dispersed during processing? If not, what means are necessary to separate agglomerated material adequately? (Sections 6.4 and 7.2)
- 2. Are the coarse fractions cleanly separated from the fines? (Sections 6.2.1 and 7.2.1)
- What, if any, treatment is required for large materials? (Sections 6.1 and 7.1)
- 4. What are the operating costs (Section 14.0)

- 5. To what extent do soluble contaminants build up in the recycle water? (This is key to determining what water treatment will be required for internal water recycle streams and for the reject water stream.) (Sections 6.2, 7.2 and 8.0)
- 6. How much will it cost to purchase and operate a full-scale (>100 t/hr) plant? (Sections 14.0 and 15.0)
- 7. As a preliminary assessment only, is there any possibility that indicator analytes, such as uranium-238, uranium-235, and/or specific inorganic constituents could be used during final remediation to verify cleanup standards are met, thus eliminating the need and cost to analyze for all contaminants of concern? (Section 15.0)

### 3.0 EQUIPMENT AND MATERIALS

The following equipment was required for the tests:

- soil washing system one  $1-m^3$  hopper (from EPA) modified to include 150-mm
  - grizzly one  $5-m^3$  hopper and feed conveyor
  - two belt conveyors (one from EPA)
  - 25-mm vibrating screen
  - Kinergy secondary vibrating screen (from EPA)
  - two #40 (0.425-mm) and two #60 (0.210-mm) screens
  - 1.37-m dia. by 6.4-m long trailer-mounted trommel (from EPA)
  - generator (from EPA)
  - three 75,000-L fractionation tanks
- two plastic water tanks 24,600 L, and 34,000 L (from EPA)
- one 6-kW gasoline pump -
- miscellaneous hoses and connections
- water truck
- backhoe
- front-end loader
- field/hand-held radiation monitoring instruments
- anticontamination clothing (anti-C's)
- miscellaneous tools
- sampling containers and equipment
- change trailer
- dust monitoring instruments
- wind and temperature gages
- first aid/safety equipment
- radios/cellular phone
- logbook.

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### 4.0 SAMPLING AND ANALYSIS

The following samples and analyses were performed for Test #1 and Test #2. Samples were collected in accordance with the test plan (DOE-RL 1993b) and the work plan (DOE-RL 1990, FSP and QAPP). Sample numbers and locations for each of the tests are shown in Tables 4-1 and 4-2.

### 4.1 PRE-PROCESS SAMPLES

Prior to processing, a clean process water sample was taken from clean water holding tanks. This sample received chemical and radiochemical analysis to establish initial conditions for the water.

Table 4-1. Samples and Hanford Environmental Information System (HEIS) Numbers for Test #1.

Stream <b>Number,</b> Material Size, Sample Period	Laboratory Analysis Chemical and Radiological (Offsite)	Physical Analysis XRF & Gamma Spectrometry (Onsite)	TCLP Analysis (Offsite)
Stream #1, Raw Feed, Processing	B07C09, B07C10, B07C11, B07C67 (dup to B07C11), B07C38, B07C39, B07C40	B08MN6, B08NM2	
Stream #2, Plus 150 mm, Post-Process		B08MN8 <sup>a</sup> , B08NM4 <sup>a</sup>	
Stream #3, 150 to 25 mm, Post-Process		B08MN9, B08NM5	
Stream #4, 25 to 2 mm, Post-Process	B07C14, B07C15, B07C16, B07C17, B07C18, B07C19, B07C20, B07C21, B07C22, B07C23, B07C24, B07C25, B07C43, B07C44, B07C45, B07C46	B08MP0, B08NM6, B08NM8	
Stream #5, 2 to 0.425 mm, Post-Process	B07c26, B07c27, B07c28, B07c29, B07c30, B07c31, B07c32, B07c68 (dup to B07c31), B07c55, B07c56, B07c57, B07c58	B08MP1, B08NM7, B08NM9	
Stream #6, Minus 0.425-mm Slurry Water, Processing	B07C75, B07C76, B07C77, B07C85 (dup to 807C76), B07C79, B07C80, B07C81		
Stream #7, Minus 0.425-mm Slurry Soils, Processing	B07C91, B07C92, B07C93, B07C95, B07C96, B07C97, B07CB1 (dup to B07C97),	B08MN7, B08NM3	B08MNO, B08NL6
Stream #8, Fresh Water, Pre-Process	B07C70, B07C73 (trip blank), B08MM8, B07C71, B07C72 (dup to B07C71), B08NL4		
Trip Blanks	B07C74, B07C87, B07CB2, B07C83		

<sup>&</sup>lt;sup>a</sup>Analysis of only fine soils washed off the rocks. >150-mm material was not analyzed.

Stream Number, Material size, Sample period	Laboratory Analysis Chemical and Radiological (Offsite)	Physical Analysis XRF & Gamma Spectrometry (Onsite)	TCLP Analysis (Offsite)
Stream #1, Raw Feed, Processing	B07DP9, B07DQ0, B07DQ1, B07DQ2, B07DQ3	B09758	
Stream #2, Plus 150 mm, Post-Process			
Stream #3, 150 to 25 mm, Post-Process		B09761	
Stream #4, 25 to 2 mm, Post-Process	BO7DV2, BO7DV3, BO7DV4, BO7DV5, BO7DV6, BO7DV7, BO7DV8, BO7DV9, BO7DW0, BO7DW1, BO7DW2, BO7DW3	B09762	
Stream #5, 2 to 0.425 mm, Post-Process	BO7DW4, BO7DW5, BO7DW6, BO7DW7, BO7DW8, BO7DW9, BO7DX0, BO7DX1, BO7DX2, BO7DX3, BO7DX4, BO7DX5	B09763	
Stream #6, Minus 0.425-mm Slurry Water, Processing	BO7DT2 (UF) <sup>a</sup> , B07DT3 (F) <sup>a</sup> , B07DT4 (UF), B07DT5 (F), B07DT6 (UF), B07DT7 (F), B07DT8 (UF), B07DV0 (UF)	в09760	
Stream #7, Minus 0.425-mm Slurry Soils, Processing	BO7DS7, B07DS8, B07DS9	B09759 B09757 (split to B07DS9)	
Stream #8, Fresh Water, Pre-Process	B07DQ4, B07DX8 (dup.to B07DQ4), B07DQ5, B07DX9 (dup.to B07DQ5)		
		1	

Table 4-2. Samples and HEIS Numbers for Test #2.

B07DY5, B07DY6 B07DY0, B07DY1

### 4.2 PROCESS SAMPLES

Trip Blanks

During processing, the feed material stream and the final process slurry stream were sampled. The first effluent sampling event occurred after the material appeared at the sampling point described in this section. The final sample was collected just prior to completion of processing. Process soil and effluent samples taken included the raw feed soils, slurry water, and slurry soils shown in Tables 4-1 and 4-2.

Samples volumes and types were as follows:

- 500-mL samples of the feed soils were sent offsite for chemical and radiochemical analysis.
- 3,500-mL samples of the feed soils received onsite screening analysis. A sub-sample was composited, weighed, dried, and weighed again to determine moisture content. The remaining sample was wet-sieved. Individual size fractions were analyzed for metals and radionuclides.

 $<sup>^{</sup>a}$ UF = unfiltered; F = filtered with a 0.2- $\mu$ m filter.

- 3,500-mL samples of the process effluent with suspended solids were sent offsite. Samples were taken at a minimum after every hour of continuous processing throughout the processing period. Effluent samples for Test #1 were not filtered by the laboratory. In Test #2, effluent samples were filtered in the field using a 0.2-µm filter prior to being sent to the laboratory for analysis. Solids in the effluent were analyzed separately for both tests.
- 3,500-mL samples of the process effluent with suspended solids were sent to onsite laboratories for analytical screening. Solids were then filtered from the effluent using a 0.45-μm membrane. The solids from the composite were wet-sieved, and each fraction was weighed. Individual fractions were mixed with size separates from post-process samples to provide enough material for adequate analysis and to reduce the number of analyses that were required (It was assumed that mineralogical and contaminant characteristics would be the same for particles of the same size fraction in each of the process and post-process samples.) Each of these fractions was analyzed for chemical and radiochemical constituents. Filtered effluent was analyzed by inductively coupled plasma (ICP) and by ICP/mass spectrometry (MS) to get measurements of major cations.
- 2,000-mL samples of the process effluent and suspended solids were sent to an offsite laboratory for TCLP analysis. A 0.6- to 0.8- $\mu$ m borosilicate glass fiber filter (EPA 1990, method 1311) was used in the TCLP analysis.

### 4.3 POST-PROCESS SAMPLES

After processing, samples were taken from random locations in each process pile. This is described in the following paragraphs. Post-process samples taken are shown in Tables 4-1 and 4-2.

### 4.3.1 >150-mm Material

One 22-L (5-gal) sample for Test #1 was sent to an onsite laboratory where fine soils were washed off the rock. The rocks and soils were then dried and weighed to show the size distribution of soils and rocks screened by the 150-mm grizzly. Rinsate was collected in a carboy, then wet-sieved, dried, weighed, and mixed with similar sized material from other process piles. As for effluent process samples, individual fractions were mixed with size separates from other process and post-process samples to provide enough material for adequate analysis. Fine soils were analyzed for metals and radionuclides. Rocks were not analyzed.

#### 4.3.2 150- to 25-mm Material

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Samples were sent to an onsite laboratory for analysis. The samples were composited to make up 22 L (5 gal) of material. The composited material was weighed and wet-sieved. Each fraction was then dried, weighed, and mixed with similar sized material from other process piles and analyzed for metals (9.5 mm and smaller) and radionuclides.

### 4.3.3 25- to 2-mm Material

Two 300-mL samples were taken from each of 16 locations. One sample from each location was sent to an onsite laboratory. Onsite samples were composited, weighed, and wet-sieved. Each fraction was then dried, weighed, and mixed with similar sized material from other process piles and analyzed for metals (9.5 mm and smaller) and radionuclides. The other 16 samples were sent offsite for chemical and radiochemical analysis.

#### 4.3.4 2- to 0.425-mm Material

Two 300-mL samples were taken from each of 16 locations. One sample from each location was sent to an onsite laboratory for analytical screening. Samples were composited, weighed, and wet-sieved. Each fraction was then dried, weighed, and mixed with similar sized material from other process piles and analyzed for metals (9.5 mm and smaller) and radionuclides. The other 16 samples were sent offsite for chemical and radiochemical analysis.

### 4.3.5 < 0.425-mm Material

All samples of this material were taken during processing (see Section 4.2).

### 4.4 ANALYSES AND VALIDATION

EPA analytical Level III and Level V analyses (EPA 1990) were performed by offsite laboratories in accordance with the test plan. Samples were analyzed for metals using EPA methods, for total uranium using fluorimetry, and for other radionuclides using gamma spectrometry. Water samples were analyzed for these constituents and volatile organic compounds VOC) using the EPA methods (1990).

Per agreement between DOE-RL, EPA, and Ecology documented in March 4, 1993 meeting minutes, all offsite sample analyses except TCLP were validated using WHC Level B Resource Conservation and Recovery Act (RCRA) data validation procedures (WHC 1990). Review requirements included:

- requested versus reported analyses
- analyses holding times
- matrix spike/matrix spike duplicate analysis
- surrogate recoveries
- duplicate analysis
- analytical blank analysis.

Samples sent to onsite laboratories were sieved and analyzed by size fraction using EPA Level II. The following sieve sizes (mm) were used: 25, 13.2, 9.5, 2, 1, 0.425, 0.212, 0.150, and 0.075. After being wet-sieved and air-dried, each size fraction was analyzed for metals using x-ray fluorescence (XRF) and for radionuclides using gamma spectrometry. Additional discussion of onsite sample analyses is provided by Serne et al. (1993).

### 5.0 PRE-TEST

The pre-test was conducted in a clean, uncontaminated area located approximately 3.2 km northwest of the 300-FF-1 Operable Unit (see Figure 1-1). The pre-test was a "shakedown run" of the physical separations prototype system. The pre-test was conducted to prepare the system for Test #1 and Test #2 by making adjustments, repairs, modifications, and screen changes, and to familiarize operators with the system. Table 5-1 summarizes the processing activities for the pre-test.

Date	Processed	Material	Processing Time (approx.)
05/28/93 (a.m.)	1.7 tons	Uncontaminated soils	60 min
05/28/93 (p.m.)	1.7 tons	Uncontaminated soils	15 min
06/01/93 (a.m.)	11.9 tons	Uncontaminated soils	68 min
06/01/93 (p.m.)	11.9 tons	Uncontaminated soils	56 min
06/02/93 (a.m.)	7.7 tons	Uncontaminated soils	48 min
06/02/93 (p.m.)	4.6 tons	Uncontaminated soils	22 min
06/02/93 (p.m.)	6.6 tons	Uncontaminated soils	30 min

Table 5-1. Summary of Pre-test Processing Activities.

Approximately 46 tons of uncontaminated soil was processed during the test conducted May 28 to June 2, 1993. Material processed was excavated from uncontaminated soils stockpiled at the pretest site. Soils were removed from the stockpile and trickled from a 1-m³ backhoe bucket onto a 150-mm grizzly. Two spray nozzles were mounted at the end of the 25-mm vibrating screen to spray rocks 150 to 25 mm to remove fine soil particles. Effluent coming off these sprays was discharged to a nearby trench. Soil particles <25 mm in diameter were conveyed to the trommel where they were separated by a 2-mm wire mesh screen. Particles 25 to 2 mm in diameter were sprayed, soaked, and rinsed in the trommel, then stockpiled. Particles <2 mm were sprayed and passed through the screen in the trommel, then transferred from the trommel to a second vibrating screen. Both a US #40 (0.425-mm) and US #70 (0.212-mm) screen were tested on the secondary vibrating screen. Soil fines and slurry passing through the screen were discharged at a rate of about 380 L/min to a series of cascading water tanks.

Water used during the pre-test was tap water trucked to the site and pumped into two clean plastic holding tanks. Dust was controlled by spraying the stockpile with water before excavating. Modifications were made during the testing period to reduce water splash and enhance dust control.

Processed soil piles were flattened out and blended into the surrounding landscape after the pre-test was completed.

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Random samples were taken to estimate or measure physical properties such as approximate flow rates, percent solids, percent moisture, and degree of separation. Dry sieving in the laboratory of soils separated by the system during this test indicated 96% by weight of 25- to 0.212-mm fraction of soils was >0.212 mm. Based on these results, equipment settings were selected to achieve the best size separation at an acceptable throughput rate. These are the baseline operating parameters used for Test #1 and Test #2.

An added benefit of the pre-test was the opportunity for close observation by WHC and RL management of the system in operation. This was not possible during Test #1 and Test #2 because these tests were conducted in a surface contamination area where the closest observation point was over 50 m from the system.

A more detailed description of the pre-test including operation, measurements, and sampling is provided by McGuire (1993). In general, the objectives of the pre-test were met. Operators gained experience operating the soil-washing system, operating parameters were established, system repairs were made, and the system was readied for the tests with contaminated soils.

#### 6.0 TEST #1

This test was conducted in the north process pond between June 23 and June 29, 1993. The purpose was to establish the performance of the system. Initial plans were to process 40 tons of soil; however, less material was processed due to unexpected test complications and results explained later in this section. Table 6-1 summarizes the processing activities for Test #1.

Date	Processed	Material	Processing Time
06/23/93	10 tons	Soils contaminated with green and white particles	Approximately 30 min for backhoe to dump and 76 min processing
06/24 - 25/93 (combined)	7.0 tons	Soils contaminated with green and white particles	Approximately 20 min for backhoe to dump and 169 min processing
06/29/93	0.5 ton	Soils contaminated with green and white particles	Approximately 70 min processing

Table 6-1. Summary of Test #1 Activities.

Two things need to be pointed out about Table 6-1: (1) the material processed was not the type of material that was proposed for the test; and (2) the processing times shown in Table 6-1 are broken down to show the amount of time spent dumping by the backhoe and the amount of time actually processing. This was necessary for Test #1 because the process was not continuous.

Figure 6-1 shows the system configuration and the material balance for Test #1. The operating parameters and flow measurements for Test #1 are shown in Table 6-2.

A 0.425-mm screen size was selected for the secondary screen, the final screening step, to separate contaminated and clean material. Based on data in Tables 1-1, 1-2, and 1-3, this cut point was selected to meet the test goal to reduce the amount of contaminated material by 90% (by weight). The size of the primary screen was dictated by the design capabilities of the trommel (i.e., feed material of 25 mm or less) and the flows were initially set to conform to the designed operating levels of the trommel and by experience gained during the pre-test shakedown. Adjustments were made during the test.

150 mm Fresh Water Feed Grizzik Legend 17.5 90 0 **Dry Tons** Percent 6.3 1,500 2.1 500 0.4 95.2 Solids Solids 25 mm 0.02 5 H<sub>2</sub>O Sprays Tons Total Vibrating > 150 mm gals. Water Screen Clean Flow Stream Slurry < 25 mm 17.1 89.1 495 2.1 9.5 90 Fresh Water 250 1.1 0 0 7.5 79.8 93.8 22,500 Hopper 450 1.9 Trommel 150 mm - 25 mm Clean < 2 mm 0.1 1.8 5.4 1,295 4.3 4.1 0.425 mm 100.3 24,045 **Vibrating Screen** Slurry Pump 80 3.3 0.7 170 < 0.425 mm 0.8 200 Slurry 2 mm - 0.425 mm Clean Slurry 25 mm - 2 mm Pump Clean 2.2 2.2 99.6 23,875 Fractionation H<sub>2</sub>O Tank Treated H<sub>2</sub>O **Treatment** Sludge 0.425 mm LSA Boxes

Figure 6-1. System Configuration/Material Balance for Test #1.

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Table 6-2. Equipment Operating Parameters and Flow Measurements for Test #1.

Component	Pai	rameter	June 23 Processing	June 24-25 Processing	June 29 Processing
Grizzly	Opening B	etween Bars	150 mm	150 mm	150 mm
	   Estimated	Feed Rate	20.0 tons/hr	22.5 tons/hr	22.5 tons/hr
Primary	Screen Opening Size Screening Area Slope		25 mm	25 mm	25 mm
Screen			750 by 2,400 mm	750 by 2,400 mm	750 by 2,400 mm
			0 deg	0 deg	0 deg
	Rinse	Pressure	2.8 kg/cm <sup>2</sup>	2.8 kg/cm <sup>2</sup>	2.8 kg/cm <sup>2</sup>
	Nozzles	Flowrate	38 L/min	38 L/min	38 L/min
		≈ L/ton	200 L/ton (50 gal/ton)	220 L/ton (60 gal/ton)	220 L/ton (60 gal/ton)
	Estimated	Feed Rate	19.4 tons/hr	21.9 tons/hr	21.9 tons/hr
Trommel	Screen Op	ening Size	2 mm	2 mm	2 mm
	Overall D	imensions	1.4 m dia. by 6.4 m	1.4 m día. by 6.4 m	1.4 m dia. by 6.4 m
	Rotationa	l Speed	5 rpm	5 rpm	5 rpm
	Stope		3 deg	3 deg	0 deg
	Retention (wash		3 min	3 min	20 min
	Initial		4.2 kg/cm <sup>2</sup>	4.2 kg/cm <sup>2</sup>	4.2 kg/cm <sup>2</sup>
	Rinse Nozzles	flowrate	600 L/min	600 L/min	600 L/min
		≈ L/ton	11,500 L/ton (3,050 gal/ton)	29,600 L/ton (7,800 gal/ton)	84,000 L/ton (22,200 gal/ton)
	Wash	Pressure	2.8 kg/cm <sup>2</sup>	2.8 kg/cm <sup>2</sup>	2.8 kg/cm <sup>2</sup>
	Water Nozzle	Flowrate	75 L/min	55 L/min	75 L/min
		≈ L/ton	3,600 L/ton (900 gal/ton)	7,750 L/ton (2,000 gal/ton)	21,000 L/ton (5,500 gal/ton)
	Final	Pressure	2.8 kg/cm <sup>2</sup>	2.8 kg/cm <sup>2</sup>	2.8 kg/cm <sup>2</sup>
	Rinse Nozzles	Flowrate	305 L/min	220 L/min	305 L/min
		≃ L/ton	14,500 L/ton (3,800 gal/ton)	31,000 L/ton (8,200 gal/ton)	85,400 L/ton (22,600 gal/ton)
	Estimated	i Feed Rate	3.4 tons/hr	1.2 tons/hr	0.6 tons/hr
Secondary	Screen Op	pening Size	0.425 mm	0.425 mm	0.425 mm
Screen	Screening		0.56 by 2.1 m	0.56 by 2.1 m	0.56 by 2.1 m
	Slope		0 deg	0 deg -	0 deg
	Speed Set	cting (%)	100	100	100
	Feed Stu	rry Density	7.3% dry solids	3.0% dry solids	0.8% dry solids
	Estimated	i Feed Rate	2.0 tons/hr	0.5 ton/hr	0.2 ton/hr
	Estimated Flowrate	i Slurry	390 L/min	350 L/min	375 L/min

Processing occurred on June 23, 24, 25, and 29, 1993. The feed soils that were processed each day were all very similar. As a result, the analytical results for sampling done on the various days are combined in this report. Minor differences in soil characteristics and contaminant composition exist; however, the primary differences each day are in the problems with the system and adjustments that were made.

Prior to the beginning of processing for each day, plastic liners were laid down for each process stream to ensure that processed material was not mixed with any of the existing material or with previously processed material.

Soils for processing were excavated from the southwest corner of the north process pond near the inlet end of the ponds (see Figure 1-2). Phase I RI characterization data (DOE-RL 1993c) show that this is the most contaminated portion of the pond. Soils were excavated within 1.0 m of the surface in an attempt to avoid the higher concentrations of uranium, which were characterized by a greenish appearance (green material). Based on Dennison et al. (1989) and the RI Phase I report (DOE-RL 1993c), this material was believed to be confined to a thin layer about 1.5 m beneath the ground surface.

However, during excavation of the feed material, it was discovered that green material was distributed throughout the soils in this particular area. Associated with the green particles are white-colored particles. The white particles are assumed to be from the whitish layer visible directly above the green layer where cuts have been made through undisturbed portions of the material. Rarely is one seen without the other being present. The green material always exhibited higher levels of activity than the white material and appears to be the major contributor of uranium contamination in the pond. In this report, green material refers to the green and white particles, unless specifically noted.

A field decision was made on June 23 to process the green material to determine what system modifications, if any, would be needed to meet test performance levels.

Soils were not processed continuously, as in the pre-test run, to ensure minimal dust exposure. The procedure was as follows. Soils to be processed were wetted down thoroughly prior to excavation. Soils were fed to the grizzly and separated by the 25-mm vibrating screen until the primary hopper was full. After the hopper was full, the conveyor system to the trommel was turned on and the trommel started.

This operating approach (noncontinuous operation and heavy wetting of the soils) resulted in several processing problems including less control in dumping material from the backhoe bucket, overloading of the primary screen resulting in insufficient washing of the oversize material, and clogging of the primary conveyor.

In addition, problems with the system occurred such as the discovery of blank plates inserted between the valves and the tank on the fractionation tanks, discharge chutes too flat to flow freely, and the collapse of the middle section of one of the discharge chutes. These were all untested parts of the system that could not be refined during the pre-test.

The end result of the first day of processing was that radioactivity levels measured in the field using a Geiger Mueller (GM) detector probe (Eberline, Albuquerque, New Mexico, Model E-140B) (exceeded test performance levels (Table 2-1) in each of the process piles. The green material basically passed through the system without breaking down to any significant degree.

On the second day of the test, June 24, a new location near the inlet end of the ponds (approximately 10 m from the June 23 site) and nearer to the ground surface was selected from which to excavate soils in an attempt to avoid the green material. Again, green particles were found distributed throughout the excavated soils.

No changes were made in the operating parameters of the system. The same noncontinuous operating approach was used on June 24. However, the feed soils were not wetted down as heavily and the backhoe operator had better success controlling the feed rate to the system. This resulted in the oversize material from the primary screen receiving a more thorough rinse, and more fine soils being sent to the trommel. This caused the trommel slurry discharge line to be plugged before the trommel was ever started. Additional problems included a blown fuse in the secondary screen and a sheared pin on the trommel metering wheel.

The net result was that not very much processing occurred and the hopper under the primary screen was still two-thirds full. The limited processing showed the same results as June 23; contamination in all process piles.

On June 25, processing began to empty out the hopper. No additional material was fed to the system by the backhoe. The system was working smoothly until the fresh water supply pump began to fail. Fresh water pressure to the system dropped significantly and to prevent the system from running out of water while full of soils, the feed to the trommel had to be shut off numerous times. This resulted in different flowrates of the wash nozzles and the final rinse nozzles in the trommel, and affected the water-to-solids ratios for those sections. Eventually, the lack of sufficient water forced the processing to be discontinued before the hopper could be emptied.

Only about 0.5 ton remained in the hopper, which needed to be emptied, and it was determined by the project engineers that some system changes would be beneficial to see what effect they might have on the green material. No additional feed material was fed to the primary screen and hopper.

One change made to the system was to decrease the slope of the trommel from 3 to 0 deg to increase the retention (wash) time. It was hoped that the increased retention time for the oversize material in the trommel would be enough to allow the green material in that size range to be broken down.

On June 29, the processing went smoothly until the fresh water supply pump lost pressure again. However, since this occurred at the end of the processing, it did not have any substantial impacts.

Field measurements with hand-held instruments by the Health Physics personnel were taken on each of the piles from this run and some success was seen in the 25- to 2-mm pile, the oversize from the trommel. However, there was still some contamination in the pile and further work needs to be done.

This completed the processing for Test #1. In spite of the problems and concerns associated with Test #1, an estimated 17.5 tons of material was processed. HEIS numbers of soil and effluent samples taken during Test #1 are shown in Table 4-1.

The following is a description and summary of data analyses obtained as part of Test #1. Complete data analyses results are included in Appendix B.1 and the PNL sediment characterization report (Serne et al. 1993).

## 6.1 FEED SOILS AND FRESH WATER

## 6.1.1 Particle Size Distribution

Samples (Table 4-1) were sent to offsite analytical laboratories for chemical and radiochemical analyses and to onsite laboratories for sieve analysis and chemical and radiochemical analysis of soils in each size fraction after sieving.

The particle size distribution of the feed soils processed in Test #1 is shown in Table 6-3 and Figure 6-2a. Figure 6-2b shows the percent of the total processed material reporting to each process pile. The soils were located near the pond inlet and within 0.5 m of the ground surface. Therefore, they contain more fine particles than anticipated based on the RI Phase I studies and previous characterization of soils conducted by Serne et al. (1992). However, as shown in Figure 6-la, a 90% reduction by weight could still be achieved if soils are successfully separated with particles >0.212 mm meeting established performance levels.

# 6.1.2 Analytical Results

Field measurements using a GM probe showed that feed soils contained up to 35,000 dpm above background (500 dpm). These were the hottest soils found in the north pond using the hand-held GM probes.

The average concentration and standard deviation for offsite chemical and radiochemical contaminants in feed soils <25 mm are shown in Table 6-4. These data show that prior to processing, only uranium concentrations were greater than the performance levels for contaminants specified in the test plan (see Table 2-1). The radionuclides other than uranium are of low enough concentrations that their actual detection could be questioned. Some are decay products in the uranium chain and some were detected in the Phase I RI characterization work, but all are of low enough concentrations that they are not of concern. This is true of all of the gamma spectrometer radionuclide analyses presented in this report. PCBs were not analyzed for in Test #1 due to miscommunication with the analytical laboratories.

-----Also shown in Table 6-4 are the average concentration and standard deviation for chemical and radiochemical contaminants in the feed water.

Table 6-3.	Wet-Sieved Size Distri	ibution o	f Feed Soils
in Test #1	(Percent by Weight).	(Serne e	t al. 1993)

Size Fraction	June 23 Processing	June 24-25 Processing	Test #1 Average
>25 mm	60.5%	51.2%	55.9%
25 to 2 mm	14.3%	25.5%	19.9%
2 to 0.425 mm	12.3%	11.7%	12.0%
0.425 to 0.212 mm	5.81%	5.32%	5.57%
0.212 to 0.150 mm	1.26%	1.16%	1.21%
0.150 to 0.075 mm	2.30%	2.00%	2.15%
<0.075 mm	3.49%	3.06%	3.28%

Green- and white-colored soils were separated (based on appearance) in the laboratory from unused portions of Test #1 feed soil samples sent to an onsite laboratory. Table 6-5 shows that the 9.5- to 1-mm white-colored soils were made up primarily of aluminum and silicate and were less radioactive than the green particles. The same sizes of green material contained lower concentrations of aluminum than the white material and higher concentrations of calcium, copper, zirconium, and uranium. A more detailed analyses of the green material is given in Table 6-5.

# 6.2 PROCESSED SOILS AND EFFLUENT

### 6.2.1 Separation Efficiency

Samples collected from each process pile were sent to an onsite laboratory for analytical screening by size fraction. Sieve analyses (Table 6-6) indicate that <2% of the particles were smaller than the desired cut in the >150-mm, 150- to 25-mm, and 25- to 2-mm process piles. About 18% of the soils retained on the 0.425-mm sieve were smaller than 0.425 mm. Of these, 13.6% were in the size range from 0.425 to 0.212 mm. One likely explanation for this high percentage of 0.425- to 0.212-mm material is that green material that was slightly larger than 0.425 mm in size after processing in the field was broken down enough during the wet-sieving analysis to pass through a 0.425-mm sieve.

Defining separation efficiency as the percent of material that actually passes through a screen compared to the amount available to pass through it, the following separation efficiencies for the various screens were calculated.

The 25-mm primary screen operated in excess of 95% efficiency. Despite a fairly high efficiency, fines that were not rinsed off this material did cause contamination in this pile.

Figure 6-2a. Average Wet-Sieved Size Distribution of Feed Soils in Test #1 (Percent by Weight) (Serne et al. 1993).

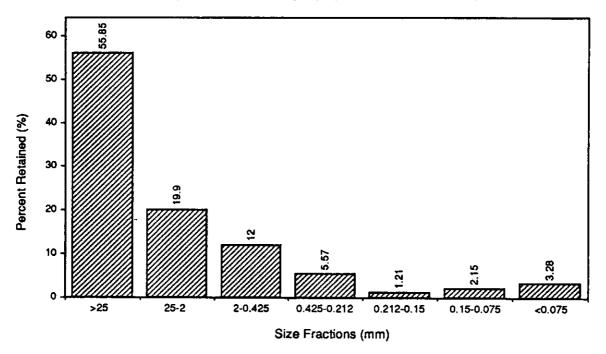
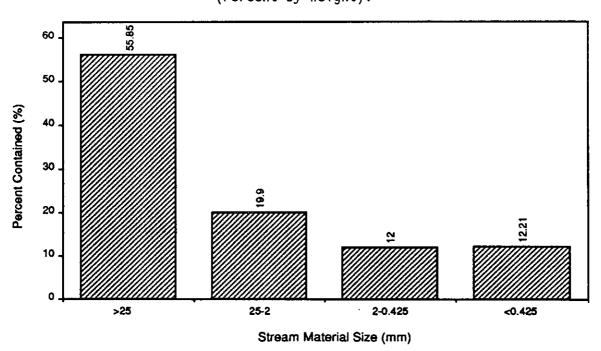


Figure 6-2b. Percent of Soils in Each Process Pile, Test #1 (Percent by Weight).



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Table 6-4. Chemical and Radiochemical Analyses of Feed Soils <25 mm and Feed Water for Test #1 (Appendix B.1).

Constituent	Feed	Soils	Feed	Water
Constituent	A∨g	ŝ	Avg	s
Cobalt-60 Cesium-137 Lead-212 Lead-214 Radium-224 <sup>a</sup> Radium-226 <sup>a</sup> Ruthenium-106 <sup>a</sup> Antimony-125 <sup>a</sup> Uranium (total)	(pCi/g) 0.0 0.2 1.4 0.5 0.6 1.3 0.0 0.0	(pCi/g) 0.0 0.1 0.4 0.1 0.3 0.5 0.2 0.1	(pci/L) 6.42 2.44 0 0 0 6.31 0.0 0.60	(pCi/L) 3.31 1.84 0 0 7.57 0.0 0.41
Silver Aluminum Arsenic Barium Beryllium Calcium Calcium Cobalta Chromium Copper Iron Mercury Potassium Magnesium Manganese Sodium Nickel Lead Antimony Tin Vanadium Zinc	(mg/kg)  21.0  22,571  2.2  1,062.9  0.5  11,086  0.4  6.9  224.3  2,763  16,857  2.3  1,046  6,386  253  2,043  278  47.9  5.9  21.3  37.1  86.7	(mg/kg) 20.2 3,923 0.7 522 0.5 26,702 0.4 132 3,123 1,355 0.6 250 766 10.3 592 289 17.1 4.3 12.6 3.3 28.2	(mg/L)  0 0.15 0 0.026 0 18 0 0 0 0.007 0.42 0 0.92 4.2 0.012 2.8 0 0.005 0 0.005 0 0.001	(mg/L) 0 0.076 0 0 1.41 0 0 0.003 0.031 0 0.43 0.309 0.001 0.28 0 0.003 0 0.003
(Water only) Chloroform <sup>a</sup> Methyl ethyl ketone <sup>a</sup> Tetrachloroethylene Tetrahydrofuran <sup>a</sup> Trichloroethylene	NA NA NA NA NA	NA NA NA NA NA	0.02 U U U	0.0 0.0 0.0 0.0

S = standard deviation; U = undetected; NA = not analyzed.

NOTE: Material >25 mm is not able to be handled by the laboratory. Material between 25 and 2 mm was crushed to 2 mm or less and then analyzed.

 $^{\rm a}{\rm Constituents}$  detected in the laboratory, but not identified in Table 2-1.

Table 6-5. Composition of Green and White Sediment in the 300-FF-1 North Pond (Weight Percent).

(Serne et al. 1993)

Constituents <sup>a</sup>	Green (2 to 1 mm)	Green (9.5 to 2 mm)	White (2 to 1 mm)	White (9.5 to 2 mm)
Na <sub>2</sub>	0.31	1.21	1.12	0.71
Mg0	3.04	4.19	0.70	0.12
A1 <sub>2</sub> 0 <sub>3</sub>	31.21	24.80	50.59	56.94
SiO <sub>2</sub>	7.71	20.43	12.00	5.41
K <sub>2</sub> 0	0.16	0.33	0.18	0.06
CaO	7.50	9.00	2.49	1.28
TiO <sub>2</sub>	0.05	0.14	0.05	0.02
Cr <sub>2</sub> O <sub>3</sub>	0.16	0.25	0.02	0.00
MnO <sub>2</sub>	0.06	0.06	0.01	0.00
Fe <sub>2</sub> 0 <sub>3</sub>	0.57	2.33	0.33	0.12
NiO	0.28	0.36	0.02	0.00
CuO	7.68	4.99	0.16	0.03
Zn0	0.03	0.05	0.01	0.00
\$r0	0.03	0.04	0.02	0.00
Pb0	0.03	0.04	0.01	0.00
Zr0 <sub>2</sub>	1.72	2.62	0.06	0.01
Ag <sub>2</sub> 0	0.02	0.03	0.00	0.00
SnO <sub>2</sub>	0.05	0.05	0.01	0.00
Ba0	0.03	0.05	0.02	0.00
UO <sub>2</sub>	1.97	1.89	0.18	0.08
Ce <sub>2</sub> 0 <sub>3</sub>	0.0	0.02	0.00	0.00
ь	37.42	25.92	32.02	33.22

<sup>&</sup>lt;sup>a</sup>The percent concentration of constituents in the sediment are given as oxides such that columns add to 100%. However, the constituents were not in the form of oxides.

<sup>&</sup>lt;sup>b</sup>Loss on ignition to 900°C of carbonate and bound waters.

Fraction (mm)	>150 mm	150 to 25 mm	25 to 2 mm	2 to 0.425 mm	<0.425 mm
>50.8	96.7	87.56	0	0	0
50.8 to 25.4	2.85	11.26	0	0	0
25.4 to 12.7	0	0.51	31.9	0	0
12.7 to 9.5	0	0.03	22.5	0	0
9.5 to 2.0	0.03	0.02	44.5	1.48	0.38
2.0 to 1.0	0.02	0.01	0.61	16.72	0.75
1.0 to 0.425	0.14	0.13	0.07	63.61	6.24
0.425 to	0.08	0.18	0.05	13.62	75.68
0.212	0.02	0.04	0.02	0.69	7.75
0.212 to 0.15	0.05	0.08	0.02	0.59	5.68
0.15 to 0.075	0.11	0.18	0.33	3.29	3.52
<0.075					

Table 6-6. Sieve Analyses for Soil Fractions Processed in Test #1 (Percent by Weight). (Serne et al. 1993)

Bold indicates size fraction that should be in the pile.

The trommel efficiency for Test #1 was very high at 99%. This is most likely a result of the high percentage of fines fed to the trommel during this test. As discussed, the fines content was higher than expected from characterization data.

The final screening unit in the system, the 0.425-mm secondary screen, operated at about 82% efficiency for this test. As with the trommel, the percentage of fines fed to this unit were high and the efficiency would be expected to be higher also.

# 6.2.2 Analytical Results

Prior to sampling of the process piles, the piles were surveyed with a hand-held GM instrument. Based on these field measurements, activity levels indicated radioactive contamination in all of the process piles. Table 6-7 gives a summary of the field measurements taken on processed soils. The levels measured in the feed soils are also shown for comparison purposes.

Soil and effluent samples (Table 4-1) were collected and sent to an offsite laboratory for analyses to assess which contaminants were in each of the process streams and to determine what water treatment, if any, would be required for effluent to meet purgewater acceptance standards. A summary of laboratory results is shown in Table 6-8. Additional data are included in Appendix B.1.

Size Fraction	Radioactivity, (dpm/100 cm <sup>2</sup> above background) <sup>a</sup>				
Feed Soils	2,000 to 35,000				
>150 mm	2,000 to 40,000				
150 to 25 mm	3,000 to 6,000				
25 to 2 mm	1,500 to 25,000				
2 to 0.425 mm	6,500 to 20,000				
<0.425 mm (soils)	3,000 to 6,000				

Table 6-7. Summary of GM Probe Field Radioactivity Measurements.

Data in Table 6-8 show that all the constituents in all the process streams were below the test performance limits except uranium. This was also true of the feed soils prior to processing (see Table 6-4). In addition, unfiltered laboratory analyses of process effluent show significant uranium concentrations (Table 6-8).

Analysis confirmed that VOCs are not contaminants that need to be addressed in the north pond area. VOCs found were near purgewater limits.

Offsite analytical laboratories did not provide data for filtered samples.

TCLP analyses (Appendix B.1) showed that all constituents analyzed for were significantly below regulatory limits (40 CFR Part 261.24).

Soil and effluent samples (Table 4-1) were also sent to an onsite laboratory for analytical screening by size fraction. This was done to assess the effectiveness of this system to physically separate and concentrate the contaminants in the fines.

After wet-sieving and determining the size fraction of soils in each of the piles, soils from the same size fractions were composited for XRF measurements and counting gamma activity levels. The results (Table 6-9) show that contaminants were primarily partitioned to the fine soil particles in each of the fractions, and contaminants were below performance levels specified in the test plan in the soil fractions >0.212 mm. Therefore, laboratory analysis of processed material showed that at a cutpoint of 0.425 mm, >87% by weight met the test performance levels, and at a cutpoint of 0.212 mm, >93% by weight of the soils met test performance levels.

<sup>&</sup>lt;sup>a</sup>Background about 500 dpm.

Table 6-8. Test #1 Analyses for Each of the Process Streams and Unfiltered Effluent (Appendix B.1).

Constituent	25 to 2 mm (avg)	2 to 0.425 mm (avg)	<0.425 mm (avg)	Unfiltered Effluent (avg)
	(pCi/g)	(pCi/g)	(pCi/g)	(pCi/L)
Cobalt-60	0.02	0.03	0.01	3.36
Cesium-137	0.06	0.10	0.20	7.69
	(μg/L)	(μg/L)	(μg/L)	(μg/L)
Uranium (total)	791	650	329	39,886
	(mg/kg)	(mg/kg)	(mg/kg)	(mg/L)
Silver	4.39	11.1	1.3	0.53
Aluminum	11,694	16,000	8,214	562
Arsenic	0.92	1.44	1.4	0.02
Beryllium	. 0.11	0.04	0.1	0.01
Cadmium	0.07	. 0.08	0.0	0.0
Chromium	62.5	122	39.1	5.77
Curium	1,318	2,025	330	52.2
Iron	17,275	17,333	14,571	155
Mercury	0.54	1_18	0.2	0.09
Manganese	225	241	184	3.52
Nickel	104	176	32.7	4.99
Lead	17.6	32.83	15.6	1.36
Antimony	0.45	0.93	0.7	0.0
Zinc	51.2	64.25	39.6	1.74
(Water only)				,
Chloroform	NA NA	NA	NA	0.01
Methyl ethyl ketone <sup>a</sup>	NA NA	NA	NA	0.05
Tetrachloroethylene	NA	NA	NA	0.002
Tetrahydrofuran <sup>a</sup>	NA NA	NA	NA	U
Trichloroethylene	l na l	NA I	NA	0.007

U = undetected; NA = not analyzed.

Schematics showing the distribution of uranium-238, uranium-235, and cobalt-60 by particle size are given in Figures 6-3a, 6-4a, and 6-5a, respectively. Calculated concentrations of uranium-238, uranium-235, and cobalt-60 in each of the process piles are shown in Figures 6-3b, 6-4b, and 6-5b. Values shown were calculated considering the activity levels in each fraction of soils (Table 6-9) and the distribution of soils for each process pile (Table 6-6).

<sup>&</sup>lt;sup>a</sup>Constituents analyzed in the laboratory for information, but not identified in Table 2-1.

Table 6-9. Test #1 Size Distribution of Contaminants in Processed Soils After Wet-Sieving. (Serne et al. 1993)

Size (mm) Contaminant	>50.8	50.8 to 25.4	25.4 to 12.7	12.7 to 9.5	9.5 to 2	2 to 1	1 to 0.425	0.425 to 0.212	0.212 to 0.15	0.15 to 0.075	<0.075
Gamma Spec (pCi/g)							· · · · · · · · · · · · · · · · · · ·				
Cobalt-60 Cesium-137 Uranium-235 Uranium-238	0.06 0.05 0.26 1.92	0.1 0.05 0.10 0.58	0.25 0.25 0.30 2.3	1.5 1.1 0.8 4.6	2.3 2.3 19.5 149	3.9 3.8 37 284	4.5 2.5 16.5 147.5	3.2 2.4 15.0 119.5	1.6 2.3 24.5 232	4.5 5.0 46.5 461	6.0 6.0 149.5 1,083
XRF (mg/kg) <sup>a</sup> Aluminum <sup>b</sup> Silicon Phosphprus Sulfur Potassium Calcium Titanium Vanadium Chromium Manganese	NA NA NA NA NA NA NA NA	NA NA NA NA NA NA NA	NA NA NA NA NA NA NA NA	NA NA NA NA NA NA NA NA	10.42 18.5 0.233 0.033 0.79 4.96 1.08 323 152 1,217 7.16	8.26 21.1 0.335 0.070 1.02 4.35 0.75 183 240 845 5.06	7.60 27.6 0.182 0.045 1.38 3.60 0.73 159 130 738 4.40	7.36 27.8 0.182 0.037 1.46 3.07 0.59 108 163 651	7.83 25.0 0.248 0.041 1.29 3.87 0.77 163 259 884	8.52 20.2 0.349 0.046 1.09 4.70 0.68 120 410 852 4.79	9.65 14.9 0.438 0.075 0.91 4.32 0.48 21 677 729
Iron Nickel Copper Zinc Arsenic Selenium Rubidium Strontium Zirconium Silver Cadmium	NA	NA	NA NA NA NA NA NA NA	NA NA NA NA NA NA NA NA	302 3,379 133 5.1 1.9 39 327 1,326 25 8.9	473 5,943 128 4.8 1.9 79 339 2,104 38 9.3	190 2,010 88 4.8 1.8 59 375 754 14 8.5	218 2,166 86 4.6 1.7 63 382 820 22 9.0	5.26 359 3,460 116 6.8 1.9 67 375 1,308 32 8.9	589 5,933 141 6.4 1.9 92 368 2,143 58 9.5	866 8,145 219 8.1 1.9 196 431 3,290 91 9.0
Tin Barium Mercury Lead Uranium U (pCi/g) <sup>C</sup>	NA NA NA NA NA	NA NA NA NA NA	NA NA NA NA NA	NA NA NA NA NA	33 573 7.6 38.2 1,179 413	64 897 8.6 67.1 2,291	26 950 5.3 39.2 983	30 975 5.3 46.2 858 300	61 1,088 6.8 65.0 1,425	87 1,405 8.8 103.8 2,493	190 3,513 10.3 155.5 7,078

NA = not analyzed.

<sup>&</sup>lt;sup>a</sup>Metals are averages for one run only; data for the second run was similar and is included in the PNL report (Serne et al. 1993) b<sub>1</sub>% is equivalent to 10,000 mg/kg.

<sup>&</sup>lt;sup>c</sup>Conversion factor for total uranium (mg/kg) times 0.35 = pCi/g for uranium-235 and uranium-238 only.

Figure 6-3a. Test #1, Wet-Sieved Size Distribution of Processed Soils, Uranium-238 Gamma Spectrometry. (Serne et al. 1993)

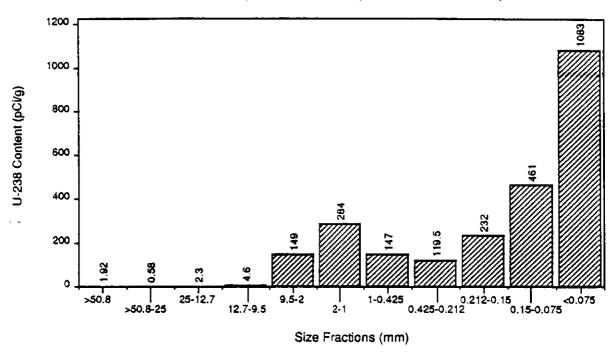


Figure 6-3b. Test #1, Contaminant Concentrations in Each Process Pile, Uranium-238 Gamma Spectrometry.

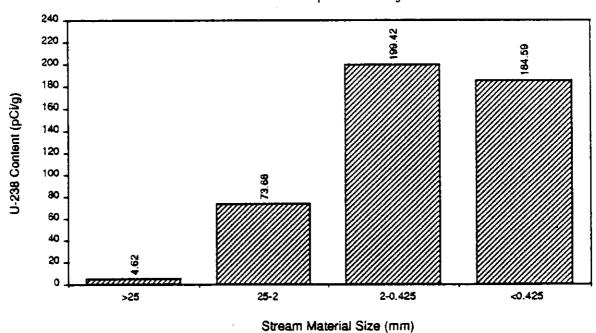


Figure 6-4a. Test #1, Wet-Sieved Size Distribution of Processed Soils, Uranium-235 Gamma Spectrometry. (Serne et al. 1993)

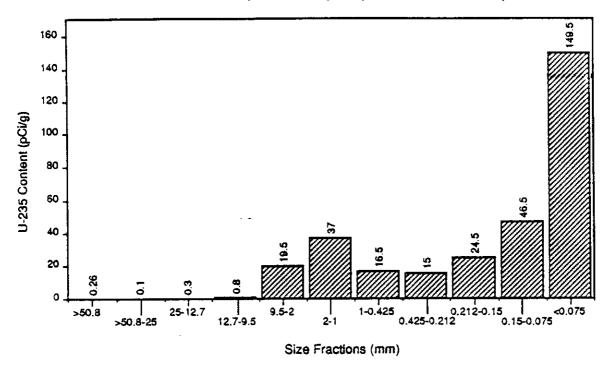
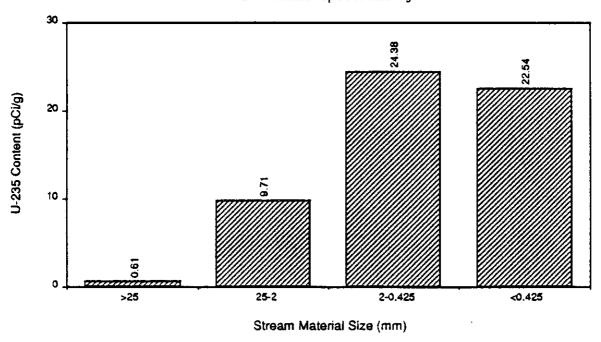


Figure 6-4b. Test #1, Contaminant Concentrations in Each Process Pile, Uranium-235 Gamma Spectrometry.



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Figure 6-5a. Test #1, Wet-Sieved Size Distribution of Processed Soils, Cobalt-60 Gamma Spectrometry. (Serne et al. 1993)

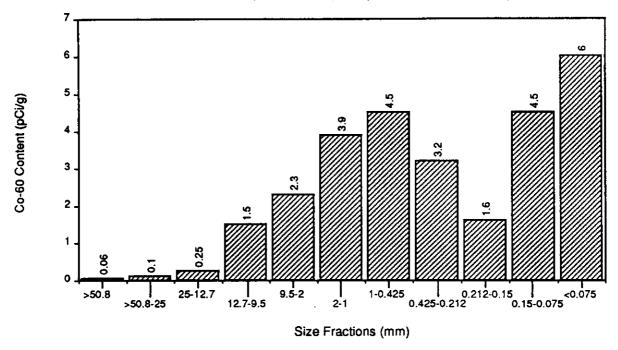
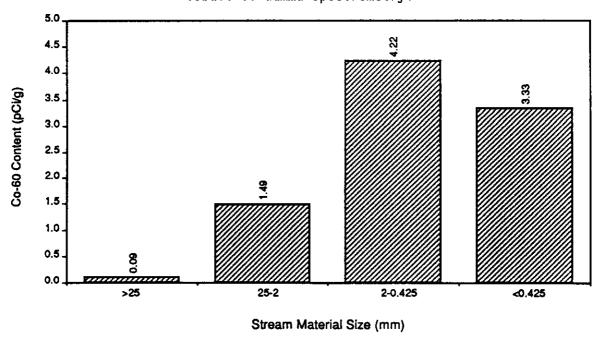


Figure 6-5b. Test #1, Contaminant Concentrations in Each Process Pile, Cobalt-60 Gamma Spectrometry.



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Although test performance levels were met in the coarse soil fraction, uranium concentrations were still as high as 284 pCi/g in material up to 2 mm in diameter and as high as 149 pCi/g in the 9.5- to 2-mm fraction of material. This is most likely the result of the green material not breaking down completely.

Process effluent samples were filtered using a  $0.45-\mu m$  filter and analyzed by an onsite laboratory. These results are shown in Table 6-10. Results are shown for the two main processing periods in Test #1 and are comparable. The values for uranium-238 in filtered effluent (24.2 and 34.4 mg/L) indicate a potential solubility problem that could affect the treatment of water for recycling.

Most contaminants were removed from the water after filtering, but uranium concentrations were still as high as 34 mg/L (purgewater acceptance standards are 0.59 mg/L for total uranium). This indicated that in spite of previous laboratory tests where uranium was not found in the water (Gerber et al. 1991), in this field test some of the uranium could not be filtered out of the process effluent. Therefore, precipitation or ion exchange water may be required.

### 6.3 JUNE 29 PROCESSING RESULTS

A final run for Test #1 was made on June 29, 1993, in which about 0.5 ton of soil was processed to clean out the hopper and trommel. Prior to processing, the trommel angle was lowered to 0 deg to increase the retention time in the trommel. In this run, there was progress made in breaking up the green material. A few flakes of green material remained in the 25- to 2-mm process stream, but it was greatly reduced from previous runs. The 2- to 0.425-mm soils still contained radioactivity in the range shown in Table 6-7. Samples from this run were collected, and particle size analyses were performed by an onsite laboratory. No other analyses were performed for this run.

Increasing trommel retention time resulted in better breakdown of particles in the trommel, as shown by <0.10% of the particles <2 mm in the 25- to 2-mm pile (Table 6-11), as compared 1.1% (Table 6-6). Also seen was an increase in the amount of fines in the 2- to 0.425-mm pile, where over 25% of the particles were smaller than 0.425 mm.

The green material was not completely broken down. In the 25- to 2-mm fraction, it was possible to visually identify and physically separate the green material that did not break down in the trommel from the individual pieces of gravel. When this was done in the field, the resulting gravels showed radioactivity levels below background levels (500 dpm) and activity levels for the green material by itself were in the ranges shown in Table 6-7.

Addition of water sprays to flush the 0.425-mm screen or decreasing the screen angle may be needed to break down green particles between 2 and 0.425 mm in size. About 7% of the <0.425-mm material going to the fractionation tanks was slightly larger than the desired size fraction.

Table 6-10. Filtered Screening Analyses of Processed Effluent Samples Collected for Test #1. (Serne et al. 1993).

Sample	June 23 Processing	June 24-25 Processing
Constituent Aluminum Boron Barium Calcium Chromium Copper Iron Potassium Magnesium Manganese Sodium Silicon Strontium Zirconium	(mg/L) 0.27 3 0.03 7.8 0.075 0.014 0.44 2.5 1.37 0.007 90 3.2 0.035 0.016	(mg/L) 0.325 3.0 0.03 7.5 0.098 0.015 0.43 1.9 0.99 0.008 114 3.2 0.032 0.012
Uranium-238 Uranium-235	24.2 0.184	34.4 0.297
F' Cl' NO <sub>3</sub>	0.79 5.4 3.9	3.2 3.6 4.4
SO <sub>4</sub> <sup>2-</sup> HCO <sub>3</sub>	24.l 175 (est)	32.3 210 (est)
Total organic compounds	2.85	3.95
Cations Calcium Potassium Magnesium Sodium UO2	(meq/L) 0.39 0.064 0.115 3.869 0.179	(meq/L) 0.375 0.049 0.082 4.935 0.255
Anions F C1 NO <sub>3</sub> SO <sub>4</sub> 2-	0.042 0.152 0.063	0.168 0.102 0.071
pH	0.502 8.07	0.673 8.19

Except as noted, analyses are ICP for metals and ion chromatography (IC) for anions. A 0.45- $\mu$ m filter was used.

Table 6-11. Test #1, June 29 Run, Wet-Sieved Analyses for Processed Soil Fractions (Percent by Weight). (Serne et al. 1993)

Fraction (mm)	25 to 2 mm	2 to 0.425 mm
25 to 13	92.45	0.00
13 to 9.5	5.76	0.00
9.5 to 2	1.69	0.75
2 to 1	0.05	12.33
1 to 0.425	0.01	62.50
0.425 to 0.212	0.01	22.80
0.212 to 0.150	0.00	1.11
0.150 to 0.075	0.00	0.52
<0.075	0.03	1.31

Bold indicates size fraction that should be in the pile.

### 6.4 ATTRITION SCRUBBING

Attrition scrubbing laboratory tests were conducted to determine the viability of using this process to further break down the green particles. Tests were conducted using a laboratory-scale attrition scrubber that simulates a commercial unit (Freeman et al. 1993). It has countercurrent impellers that rotate at a selected speed and time to determine energy input requirements. Based on 100 Area tests, additional fines are created in the attrition scrubbing process.

Table 6-12 compares particle size distribution for three tests conducted using soil samples collected from the 2 to 0.425-mm processed material. These are dry-screened, wet-screened, and attrition-scrubbed followed by wet screening. Table 6-12 shows significantly more fine soils after attrition scrubbing and less coarse material than for the wet- or dry-sieved material, indicating that particles were broken down using the scrubber.

Table 6-13 and Figures 6-6a, 6-7a, and 6-8a show that following scrubbing, contaminant concentrations were much lower in each of the wetsieved size fractions above 0.212 mm. Calculated concentrations of uranium-238, uranium-235, and cobalt-60 representative of each process pile are shown in Figures 6-6b, 6-7b, and 6-8b. Values shown were calculated considering the activity levels in each fraction of soils before and after attrition scrubbing (Tables 6-13) and the size distribution of soils for each process pile (Table 6-6).

The results of the attrition scrubbing test conducted in the laboratory indicate that the addition of a commercial attrition scrubber to the soil washing system would provide the sufficient energy to treat the 2- to 0.425-mm material such that it would meet the test objectives for soils containing the green material. Modifications to the trommel and the secondary screen in Test #2 provided additional information regarding treatment of soils containing the green material.

Table 6-12. Test #1 Size Distribution of Dry-Sieved, Wet-Sieved, and Attrition-Scrubbed/Wet-Sieved Soil Samples from the 2- to 0.425-mm Process Pile (Percent by Weight). (Serne et al. 1993)

Fraction (mm)	Wet Sieved	Dry Sieved	Attrition/Wet Sieved
>50.8 50.8 to 25.4 25.4 to 12.7	0.00 0.00 0.00	0.00 0.00 0.00	0.00 0.00 0.00
12.5 to 9.5 9.5 to 2 2 to 1	0.00 2.53 <b>20.27</b>	0.00 0.65 <b>10.87</b>	0.00 0.41 9.91 62.0
1 to 0.425 0.425 to 0.212 0.212 to 0.15	<b>62.24</b> 11.63 0.52	66.06 20.38 0.70	13.08 0.49 0.43 13.68
0.15 to 0.075 <0.075	0.43 2.37	0.53 0.83	

Bold indicates size fraction that should be in the pile.

Table 6-13. Size Distribution of Radiochemical Isotopes After Attrition Scrubbing, Test #1 (Serne et al 1993).

Fraction (mm)	Uranium-238 (pCi/g)	Uranium-235 (pCi/g)	Cobalt-60 (pCi/g)	Cesium-137 (pCi/g)
9.5 to 2	33.7	4.1	5.37	5.05
2 to 1	28.1	2.8	0.97	0.70
1 to 0.425	50.8	6.3	0.90	0.46
0.425 to 0.212	35.4	3.8	1.54	1.68
0.212 to 0.15	75.2	10.4	6.68	3.92
0.15 to 0.075	190	14.0	19.9	14.9
<0.075	777	103	8.82	7.47

In areas of the pond where the green layer is intact and undisturbed, it may be appropriate to selectively extract this material and send it directly to disposal. Since it is already concentrated in a distinct layer, volume reduction of this material is less likely by processing it in a full-scale system.

Figure 6-6a. Test #1 Distribution of Uranium-238 by Particle Size, Before and After Attrition Scrubbing. (Serne et al. 1993).

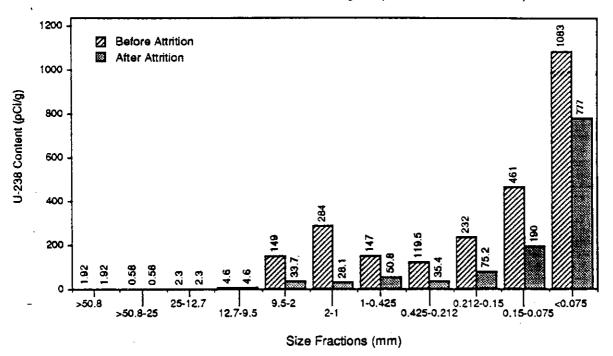
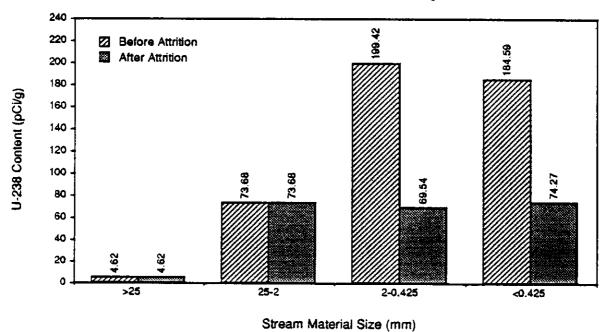


Figure 6-6b. Test #1 Uranium-238 Levels in Each Process Pile Size Fraction, Before and After Attrition Scrubbing.



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Figure 6-7a. Test #1 Distribution of Uranium-235 by Particle Size. Before and After Attrition scrubbing. (Serne et al. 1993).

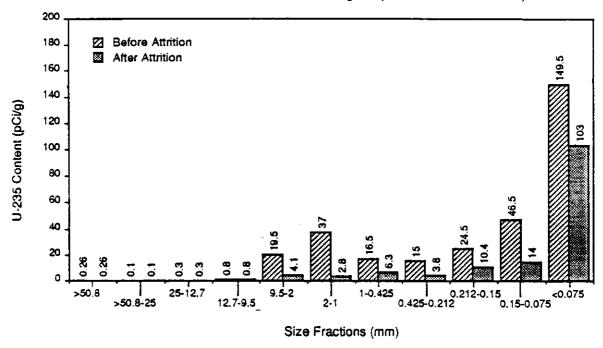
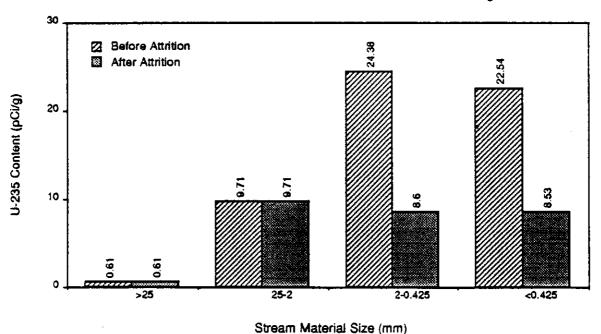


Figure 6-7b. Test #1 Uranium-235 Levels That Would Be in Each Process Pile Size Fraction, Before and After Attrition Scrubbing.



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Figure 6-8a. Test #1 Distribution of Cobalt-60 by Particle Size, Before and After Attrition Scrubbing. (Serne et al. 1993)

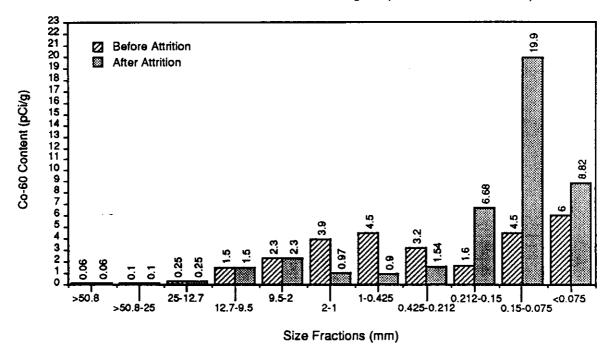
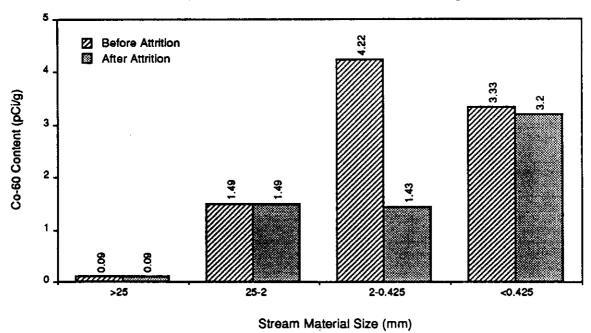


Figure 6-8b. Test #1 Cobalt-60 Levels That Would Be in Each Process Pile Size Fraction, Before and After Attrition Scrubbing.



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#### 6.5 DATA DISCREPANCIES

Some differences between offsite laboratory results and onsite PNL gamma spectrometry and XRF results should be mentioned here. Almost without exception, offsite laboratory analysis of metals and radionuclides in the feed soils and in the processed streams showed higher concentrations than gamma spectrometry or XRF analyses conducted onsite for the same constituents. In both analytical laboratories, instruments were calibrated daily to a known standard.

One explanation for the differences may be that processed soils were wet sieved in the PNL laboratories and more of the uranium contaminants solubilized into the water used for wet sieving. Another potential explanation may be that in spite of efforts to obtain representative samples and duplicate samples for the laboratories, there was a spatial variability in the samples. A third possible explanation is that the samples sent to offsite laboratories may be biased because the full-size range of material may not fit into the sample bottles. As a result, oversize material that had been excluded was not accounted for. This is particularity true for the feed soils.

Another difference noticed was between activity levels for uranium-238 calculated from XRF measurements and uranium-238 analyses using gamma spectrometry. The value derived through XRF analysis is 2.2 times higher than that from gamma spectrometry. Because XRF analyses are closer to offsite laboratory results and because uranium is primarily an alpha emitter with gamma emissions and gamma measurements are less sensitive, XRF is likely the more accurate of the two. Investigations into these discrepancies are further addressed by Serne et al. (1993).

Another noted discrepancy in the data was that the concentration of uranium isotopes in feed soils was higher than the concentration in the processed soil fractions. The reason for this was that much of the uranium remained in the effluent. A rough mass balance illustrates this.

The concentration of uranium (Table 6-8) was 791 pCi/g in the 25- to 2-mm fraction, 650 pCi/g in the 2- to 0.425-mm fraction, and 329 pCi/g for soils <0.425 mm. A weighted average of these comes out to 625 pCi/g based on the distribution in Figure 6-2b. The concentration of uranium in the <25-mm feed soils was 1,802 pCi/g (Table 6-4). The difference between feed soils and processed soils is 1,177 pCi/g, rounded to 1,200 pCi/g. Since approximately 4.3 tons of <2-mm soil was processed in Test #1 (Figure 6-1), this gives a total radioactivity level of 5.26E09 pCi that is not accounted for and that should have accumulated in the process effluent.

Approximately 91,000 L of effluent was processed in Test #1. After processing, unfiltered effluent contained approximately 40,000 pCi/L of uranium activity (Table 6-8). Multiplied, this is 3.6E09 pCi of uranium, which is within the same order of magnitude as the difference in soil activity levels before and after processing.

## 6.6 RECOMMENDATIONS FOR TEST #2

Based on the activities of Test #1 and evaluation of the results of sampling done during the test, the following items were considered before the start of Test #2.

- The original scope of this test as defined in the test plan was to treat soils that were not contaminated with the green material. These soils represent the majority of the soils in the 300-FF-1 Operable Unit and must be processed during Test #2.
- 2. The system needs to be modified so it can be fed with smaller equipment. This will provide better control of the material going onto the primary screen allowing for higher screen efficiency and better rinsing of the oversize material.
- The system needs to be modified such that it can be operated continuously. This will be accomplished by the modification for the use of smaller feed equipment and adequate dust control measures.
- 4. The operating parameters for the trommel need to be modified to better treat soils containing the green material. As with Test #1, the slope of the trommel should remain at 0 deg for soils with the green material. The speed should be increased from 5 to 7 rpm. These modifications are proposed to promote the breakdown of the green particles.
- 5. The secondary screen and its operating parameters need to be modified in an attempt to effectively treat soils containing the green material. The system modifications include installation of sprays over the secondary screen. The slope of the secondary screen should be changed to increase the retention time of oversize material on the screen. The speed of the secondary screen should be slowed down to also increase the retention time. These changes are proposed to increase the efficiency of the screen and to enhance the breakdown of the green particles.

#### 7.0 TEST #2

Test #2 was conducted September 8 and 9, 1993. The purpose of Test #2 was to process soils free of the green material and to assess system modifications recommended in Section 6.6. Soils processed on September 8 were collected from three different areas of the north pond (see Figure 1-2). Soils processed on September 9 were collected from piles on the southwest portion of the north pond, near the location for Test #1. A summary of Test #2 activities is shown in Table 7-1.

Date	Tons Processed	Material	Approximate Processing Time (min)
09/08/93	15	Contaminated soils free of any visible green particles	135
09/09/93	5	Soils contaminated with green particles	60

Table 7-1. Summary of Test #2 Activities.

Prior to conducting Test #2, field radiological measurements were made using a GM probe to identify those locations in the ponds without the green material. Green material was found in each of the soil piles along the west side of the north process pond, with radioactivity levels ranging from 150 to 1,200 dpm above background (500 dpm). No green material was observed on the north-central end and along the east side of the north process pond. Radioactivity of these soils was measured at near-background levels (500 dpm) and were chosen for the September 8 feed. A front-end loader was used to stockpile these soils prior to processing.

Field measurements of soils processed on September 8 showed that radioactivity levels were near background and well below test performance levels. Therefore, the goal of processing the soils was not to meet test performance levels, but to determine if, or by how much, radioactivity and metal concentrations could be reduced using the modified EPA system. RI Phase I investigations (DOE-RL 1993c) indicate that the soils processed are representative of about 75% of the contaminated soils in the north and south process ponds.

The system was modified for Test #2 so a small front-end loader could be used to feed it. Modifications involved mounting the 150-mm grizzly on a shorter, smaller hopper and adding a conveyor to move soils from this hopper to the 25-mm screen (Figure 7-1). With these modifications, less water was required for dust control and the system operated continuously.

Legend **Dry Tons** Percent Solids Solids Feed Tons Total 15 90 Water gals. 1.7 400 Flow Stream Fresh Water 150 mm Grizzly 0.2 95 8.3 2,000 0.01 3 25 mm Vibrating H<sub>2</sub>O Sprays + 6" Screen 本本 Clean Slurry < 25 mm 14.8 89.7 1.7 397 85 Fresh Water 500 2.1 90.6 2.9 45.9 11,000 Hopper 0.3 80 T<sub>rommel</sub> ▼ 25 mm 150 mm - 25 mm Clean < 2 mm 0.1 1.3 7.6 1,817 0.6 1.1 0.425 mm 53.1 12,722 Vibrating Screen Slurry Pump 2.4 77.4 < 0.425 mm 0.7 | 175 Slurry 2 mm - 0.425 mm Clean Slurry 25 mm - 2 mm Pump Clean 0.2 0.4 52.2 12,515 Fractionation H<sub>2</sub>O Treated Tank H<sub>2</sub>O Treatment Sludge - 0.425 mm **LSA Boxes** H9304006.5c

Figure 7-1. System Configuration/Material Balance for Test #2.

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As was to be expected with untested components in the system, several problems were encountered that had to be worked out. The head pulley on the conveyor was adjusted to tighten the belt. The new operator was unfamiliar with the system and had trouble feeding the material without jamming the conveyor, and the chain drive on the conveyor came off. After these problems were resolved, the system ran smoothly.

Although the system was modified to operate continuously, travel and feed time for the front-end loader and limitations on the feed rate of the 25-mm shaker screen contributed to lower feed rates. It was not possible to improve the feed rate in a timely manner. However, except for limiting the amount of material processed, this did not impact the test results.

The system configuration and a mass balance for September 8 processing are shown in Figure 7-1. Operating parameters and flow measurements are shown in Table 7-2. HEIS numbers of soil and effluent samples taken on September 8 are shown in Table 4-2. Sections 7.1 and 7.2 are results from processing on September 8 only.

On September 9, additional testing was performed on soils containing the green material. Several of the operating parameters were changed in an effort to enhance the breakdown of the green material. However, the changes resulted in limited success, and no samples or analyses except for field measurements were obtained.

#### 7.1 FEED SOILS AND FRESH WATER

## 7.1.1 Particle Size Distribution

The particle size distribution of feed soils used in Test #2 is shown in Table 7-3 and Figure 7-2a. The corresponding percent of soils expected in each process pile is shown in Figure 7-2b. More than 96% of the soil particles were >0.425 mm. This was more coarse material than in Test #1 where about 88% of the soil particles were >0.425 mm (see Figure 6-2b).

## 7.1.2 Analytical Results

Laboratory analyses showing the average concentration and standard deviation for chemical and radiochemical contaminants for feed soils and water are shown in Table 7-4. As expected based on RI Phase I data (DOE-RL 1993c), chemical and radiochemical constituents in feed soils for Test #2 were below test performance levels prior to processing. TCLP analyses (Appendix 8.2) were also below regulatory levels of concern.

Clean water fed to the system was analyzed for comparison with process effluent.

Table 7-2. Equipment Operating Parameters and Flow Measurements for Test #2.

			<del>,                                     </del>	
Component	Pa	rameter	September 8 Processing	September 9 Processing
Grizzly Opening Betwe		etween Bars	150 mm	150 mm
	Estimated Feed Rate		6.7 tons/hr	7.5 tons/hr
Primary	Screen Opening Size		25 mm	25 mm
Screen	Screening	Area	750 by 2,400 mm	750 by 2,400 mm
	Slope		0.0 deg	1.5 deg
	Rinse	Pressure	2.8 kg/cm <sup>2</sup> (40 lb/in <sup>2</sup> )	Moved to secondary screen
	Nozzles	Flowrate	50 L/min (13 gal/min)	N/A
		≈ L/ton	560 L/ton (150 gal/ton)	N/A
	Estimated	Feed Rate	6.6 tons/hr	7.4 tons/hr
Trommel	Screen Op	ening Size	2 mm	2 mm
	Overall D	imensions	1.4 m dia. by 6.4 m	1.4 m dia. by 6.4 m
	Rotationa	ıl Speed	5.0 rpm	7.0 rpm
	Slope		3.0 deg	0.0 deg
	Retention (wash) Time		3 min	20 min
	Initial	Pressure	4.2 kg/cm <sup>2</sup> (60 lb/in <sup>2</sup> )	4.2 kg/cm <sup>2</sup> (60 lb/in <sup>2</sup> )
Wa: Wa: Wa	Rinse Nozzles	Flowrate	600 L/min (160 gal/min)	600 L/min (160 gal/min)
		≈ gal/ton	27,000 L/ton (7,100 gal/ton)	36,000 L/ton (9,500 gal/ton)
	Wash Water Nozzle	Pressure	2.8 kg/cm <sup>2</sup> (40 lb/in <sup>2</sup> )	2.8 kg/cm <sup>2</sup> (40 lb/in <sup>2</sup> )
		Flowrate	60 L/min (15 gal/min)	40 L/min (10 gal/min)
		≃ gal/ton	3,400 L/ton (900 gal/ton)	3,000 L/ton (800 gal/ton)
	Final	Pressure	2.8 kg/cm <sup>2</sup> (40 lb/in <sup>2</sup> )	2.8 kg/cm <sup>2</sup> (40 lb/in <sup>2</sup> )
	Rinse Nozzles	flowrate	250 L/min (65 gal/min)	160 L/min (40 gal/min)
		≈ gal/ton	14,000 L/ton (3,700 gal/ton)	12,000 L/ton (3,200 gal/ton)
	Estimated Feed Rate		1.3 tons/hr	1.4 tons/hr
Secondary	Screen Opening Size		0.425 mm	0.425 mm
Screen	Screening Area		0.56 by 2.1 m	0.56 by 2.1 m
	Slope		0.0 deg	-0.5 deg
	Rinse	Pressure	N/A	2.8 kg/cm <sup>2</sup> (40 lb/in <sup>2</sup> )
	Nozzles	Flowrate	N/A	50 L/min (13 gal/min)
	1	≈ gal/ton	N/A	18,000 L/ton (4,700 gal/ton)
	Speed Setting (%)		100	40
	Feed Slurry Density		1.1% dry solids	1.6% dry solids
	Estimated Feed Rate		0.3 ton/hr	0.3 ton/hr
	Estimated Slurry Flowrate		410 L/min	280 L/min

Table 7-3. Test #2, Wet-Sieved Size Distribution of Feed Soils. (Serne et al. 1993).

Size Fraction (mm)	% by Wt
>50.8	63.2
50.8 to 25	16.8
25 to 2	15.7
2 to 0.425	2.9
0.425 to 0.212	0.45
0.212 to 0.15	0.10
0.15 to 0.075	0.15
<0.075	0.85

### 7.2 PROCESSED SOILS AND EFFLUENT

# 7.2.1 Separation Efficiency

Samples collected from each of the process piles were sieved onsite. Sieve analyses for each of the process piles in Test #2 (Table 7-5) show that the three screening units in the system performed well within normal operating parameters for this equipment.

Defining separation efficiency as the percent of material that actually passes through a screen compared to the amount available to pass through it, the following separation efficiencies for the various screens were calculated.

The 25-mm primary screen operated at almost 99% efficiency. The trommel efficiency for Test #2 was about 90%, slightly lower than it was for Test #1. The difference was due to the much higher percentage of fines in Test #1 as compared to Test #2 (56% and 22%, respectively).

The 0.425-mm secondary screen operated at 85% efficiency for Test #2. This is slightly higher than for Test #1. The increased efficiency is attributed to addition of water spray to help improve the separation made by this screen. This screen experienced a certain amount of blinding off that reduced the unit's efficiency. Full-scale operations will require either a different process for separating soil particles <0.425 mm (i.e., hydrocyclones or countercurrent columns) or additional vibrating screens to facilitate a schedule for the shutdown for cleaning without interrupting the processing.

Based on Tables 7-5 and 7-3, after processing in the field, approximately 98% of the soils were in the 150- to 25-mm, 25- to 2-mm, and 2- to 0.425-mm process piles. Only about 2% of the soil particles were in the <0.425-mm stream sent to the fractionation tanks.

Figure 7-2a. Average Wet-Sieved Size Distribution of Feed Soils in Test #2 (Percent by Weight). (Serne et al. 1993)

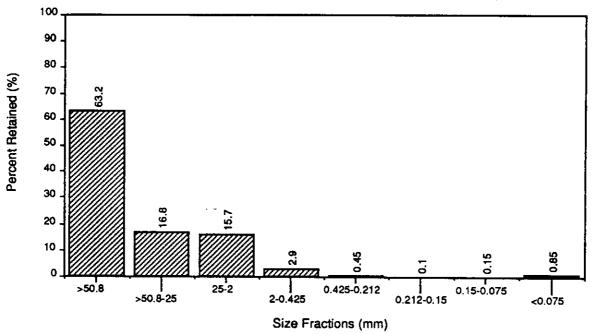
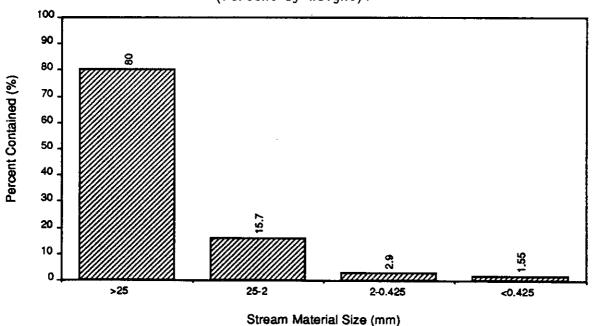


Figure 7-2b. Percent of Soils in Each Process Pile, Test #2 (Percent by Weight).



GEN/M112593-A

Table 7-4. Test #2, September 8, Chemical and Radiochemical Analyses of Feed Soils <25  $\,\mathrm{mm}^{\mathrm{a}}$  and Feed Water (Appendix B.2).

	Feed	Soils	Water		
Sample	Avg	S	Avg	s	
Contaminant Cobalt-60 Cesium-137 Lead-12 <sup>D</sup> Lead-214 Radium-224 Radium-226 Radium-106 Antimony-125	(pCi/g) 0.116 0.062 0.591 0.475 0.594 0.440 0.040 U	(pCi/g) 0.102 0.020 0.058 0.027 0.058 0.065 0.120 0.030	(pCi/L) 2.809 U 3.075 U NA NA NA NA U U	(pCi/L) 2.144 1.112 NA NA NA U U	
Uranium (total)	5.506	4.162	(μg/L) 0.958	(μg/L) 0.391	
Metals Silver Aluminum Barium Beryllium Calcium Cadmium Cobalt Chromium Copper Iron Mercury Potassiumb Magnesium Manganese Sodium Nickel Lead Antimony Tin Vanadium Zinc	(mg/kg) 3.6 11,320 0.33 7,880 0.00 12.6 19.8 238 32,600 0.17 1,294 6,340 498 446 28.8 5.68 4.82 0.00 88.2 70.6	(mg/kg) 0.92 2,282 0.10 1,038 0.00 1.02 3.66 80.6 1,625 0.15 368 779 73.1 17.4 4.79 1.32 2.46 0.00 1.72 4.76	(mg/L) 0.002 0.00 0.031 0.00 28.3 0.00 0.00 0.00 0.03 0.79 0.00 2.20 6.45 0.028 5.80 0.00 0.012 0.00 0.00 0.012 0.00 0.0013 0.010	(mg/L) 0.002 0.00 0.005 0.00 5.76 0.00 0.00 0.003 0.031 0.671 0.00 0.51 1.46 0.025 2.18 0.00 0.015 0.00 0.015	
Organics 1,1,1-trichloroethane 1,1,2-trichloroethane 1,1-dichloroethane 1,2-dichloroethane 1,4-dichloroethane 1,4-dichloroethane 1-butanol 4-methyl-2-pentanone Acetone Benzene Carbon disulfide Carbon tetrachloride Chloroform Ethyl cyanide Methyl ethyl ketone Methylene chloride Tetrachloroethane Tetrahydrofuran Toluene Vinyl chloride Xylenes (total)	NA A A A A A A A A A A A A A A A A A A	NA N	(mg/L) 0.008U U U U U U U U U 0.0014U U 0.005U U U 0.0094U U 0.0001U U	(mg/L) 0.0012U U U U U U U 0.0029U U 0.015U U 0.0123U U 0.0003U U	

S = standard deviation; U = undetected; NA = not analyzed.

 $<sup>^{\</sup>rm a}$  Material >25 mm is not able to be handled by the laboratory. Material between 25 and 2 mm was crushed to 2 mm or less and then analyzed.

 $<sup>^{\</sup>mathrm{b}}\mathrm{Constituents}$  detected in the laboratory, but not identified in Table 2-1.

Fraction (mm)	150 to 25 mm	25 to 2 mm	2 to 0.425 mm	<0.425 mm
>50.8	95.42	0.00	0.00	0.00
50.8 to 25.4	4.26	0.00	0.00	0.00
25.4 to 12.7	0.00	14.46	0.00	0.00
12.7 to 9.5	0.00	18.78	0.00	0.00
9.5 to 2	0.02	63.79	1.21	0.03
2 to 1	0.01	2.92	27.32	1.28
1 to 0.425	0.05	0.02	62.86	2.65
0.425 to 0.212	0.03	0.01	5.86	51.78
0.212 to 0.15	0.01	0.00	0.08	9.58
0.15 to 0.075	0.02	0.02	0.09	11.07
<0.075	0.17	0.01	2.58	23.61

Table 7-5. Sieve Analyses for Soil Fractions Processed in Test #2 (Percent by Weight). (Serne et al 1993).

Bold indicates size fraction that should be in the pile.

# 7.2.2 Analytical Results

During processing and after processing was completed, soil and effluent samples were collected and sent offsite for analyses to assess which contaminants were in each of the process streams and to determine what water treatment, if any, would be required for effluent to meet purgewater acceptance standards. A summary of laboratory results is shown in Table 7-6. Additional data are included in Appendix B.2.

Offsite analyses (Table 7-6) show that all the constituents in all the soil streams were below the performance limits for the test, and the highest concentrations of uranium and chromium were in the fine soil particles. The average activity of uranium in soils processed was 1.4 pCi/g in the 25- to 2-mm process pile, 12.1 pCi/g in the 2- to 0.425-mm pile, and 93.6 pCi/g in soil particles <0.425 mm. This confirmed that the system tested effectively separated soils such that the concentration of uranium was significantly reduced in the more coarse soil fractions. A similar reduction in concentrations was seen for chromium.

Process effluent from Test #2 was filtered in the field using a 0.45- $\mu m$  filter. Analyses showed that only 178  $\mu g/L$  of the uranium was found in the filtered effluent (Table 7-6). As noted by Serne et al. (1993), this may have been due to a short contact time as compared with Test #1 (where effluent was not filtered in the field), or to lower concentrations of uranium in the soils and little or no green material in the soils processed. Regardless of the reason, these data indicate that flocculation of particles and filtering may be sufficient to treat process effluent to meet purgewater acceptance standards such that it can be recycled in a soil treatment system.

Table 7-6. Test #2 Laboratory Analyses for Each of the Process Piles (Appendix B.2).

Sample	25 to 2 mm (avg)	2 to 0.425 mm (avg)	<0.425 mm (avg)	Filtered Water (avg)
<u>Contaminant</u>	(pCi/g)	(pCi/g)	(pCi/g)	(pCi/L)
Cobalt-60 Cesium-137 Lead-212 Lead-214 Radium-224 Radium-226 Ruthenium-106 Antimony-125	0.106 0.118 0.568 0.506 0.572 0.491 U	0.260 0.256 0.671 0.438 0.675 0.417 U	0.242 0.273 1.049 0.681 1.051 0.632 U	U U - - - U 4.2
Uranium (total)	1.432	12.05	93.63	(μg/L) 177.8
	(mg/kg)	(mg/kg)	(mg/kg)	(mg/L)
Silver Aluminum Barium Beryllium Calcium Cadmium Cobalt Chromium Copper Iron Mercury Potassium Magnesium Manganese Sodium Nickel Lead Antimony Tin Vanadium Zinc	0.91 4,292 70.0 0.22 5,450 0.00 9.08 4.18 158 24,583 0.00 309 3,492 267 328 9.19 1.93 1.70 0.00 63.9 51.3	4.00 7,567 93.1 0.35 7,083 0.00 11.8 18.8 644 33,750 0.22 569 5,533 406 478 31.3 4.93 2.25 0.00 98.5 106	4.73 7,867 220 0.04 5,067 0.00 7.80 41.3 580 24,333 0.25 683 4,167 287 367 38.3 13.0 0.00 6.83 70.7 75.7	0.0014 0.06 0.04 0.0004 23.7 0.00 0.00 0.0022 0.029 0.064 0.00 2.13 4.77 0.0134 7.83 0.00 0.0006 0.000 0.000 0.000

U = undetected.

Bold indicates constituent was detected in only one sample.

Analysis for VOCs was performed on the fresh water stream and the process water stream in Test #1 and Test #2. VOCs for Test #2 were undetected except for laboratory additions including 1,1,1-trichloroethane, methyl ethyl ketone, and tetrahydrofuran.

Aroclor-1248 was the only PCB detected. It was detected below test performance levels (2,200 ppb) in all soil samples that were taken. The highest concentrations were found in three slurry soil samples with the highest

being 970 ppb. It was found in five of eight process effluent samples. Using zero for the nondetects, the average concentration found in the effluent was 0.35 ppb with a high of 1.3 ppb. In comparison, the purgewater acceptance standard for mixed PCBs is 1 ppb.

Soil particles of the same size fraction were composited from each of the process streams (e.g., the 2- to 0.425-mm fraction of materials in each process streams). The composited soils were analyzed in onsite laboratories for metals and radionuclides. As was the case with offsite analyses of process streams (Table 7-6), the results (Table 7-7) show that the highest concentrations of uranium and chromium were in the fine soil particles. In the sieved soils (Table 7-7), the concentration of uranium-238 in soil particles <0.425-mm was 26.9 pCi/g compared to 6.8 pCi/g in the 2- to 0.425-mm size fraction. The concentration of uranium-238 in particles <0.075 mm was 54 pCi/g compared to 35 pCi/g for particles between 0.15 and 0.075 mm and 23.3 pCi/g for particles between 0.212 and 0.15 mm.

The distribution of uranium-238, uranium-235, and cobalt-60 in each of the sieved size fractions is shown in Figures 7-3a, 7-4a, and 7-5a, respectively. Estimated concentrations of uranium-238, uranium-235, and cobalt-60 in each process pile are shown in Figures 7-3b, 7-4b, and 7-5b. Values shown were calculated considering the measured radioactivity levels in each fraction of soils (Table 7-7) and the distribution of soils for each process pile (Table 7-5). As in Test #1, uranium-238 was the primary contaminant.

A weighted average of the size distribution of soils in each process stream (Figure 7-2b) with uranium-238 analytical data (Figure 7-3b) shows that by separating soil in the field at a cutpoint of 0.425-mm uranium-238 concentrations were reduced by a factor of 45 and the fraction of soils was reduced by 98% (by weight).

#### 7.3 SEPTEMBER 9 TESTING

In addition to tests on September 8, 1993, soils containing green material were processed on September 9, 1993 to see if slight equipment modifications recommended (Section 6.0) would result in a better, more successful treatment process. Changes were made to the trommel angle and speed to increase retention time and energy input. Sprays were added to the 0.425-mm screen, and speed of the screen vibration was reduced to enhance particle separation. Other equipment parameters are specified in Table 7-2. This test was made using green material from one of the piles on the west side of the trench. The trommel speed was increased to 7 rpm to provide more energy to separate soils. The radioactivity of the field soils was measured at 6,000 to 13,000 dpm with an average of 9,000 dpm. Approximately 5 tons of soil were processed. After processing, no green particles >3 mm in diameter were detected in the trommel oversize material. This could be for one of two reasons: (1) feed material did not contain larger particles of the green material, which seems unlikely; or (2) the increased trommel speed provided enough additional energy to break down the larger green particles more than in Test #1. Increasing the speed of the trommel to 9 or 10 rpm would likely provide the required energy to remove green particles from the trommel oversize stream (>2 mm).

Table 7-7. Test #2 Size Distribution of Contaminants in Processed Soils After Wet-Sieving. (Serne et al. 1993)

Size (mm) Contaminant	>50.8	50.8 to 25.4	25.4 to 12.7	12.7 to 9.5	9.5 to 2	2 to 1	1 to 0.425	0.425 to 0.212	0.212 to 0.15	0.15 to 0.075	<0.075
Gamma Spec (pCi/g)											
Cobalt-60 Cesium-137 Uranium-235 Uranium-238	0.06 0.05 0.04 0.17	0.04 0.12 0.07 0.45	0.27 0.09 0.05 0.72	0.27 0.38 0.14 0.67	0.3 0.3 0.2 0.9	0.4 0.4 0.6 2.9	0,3 0.5 1.0 5.8	0.5 0.5 2.3 15.2	0.8 0.8 3.2 23.3	1.4 5.7 4.9 35.0	2.5 2.6 1.0 54.0
XRF (mg/kg) <sup>a</sup> Aluminum b Silicon phosphorus Sulfur b Potassium b Titanium b Titanium b Titanium b Manganese Iron Nickel Copper Zinc Arsenic Selenium Rubidium Strontium Silver Cadmium Tin Barium Mercury Lead Uranium	NA A A A A A A A A A A A A A A A A A A	NA N	NA N		6.40 26.0 0.08 0.05 1.36 4.92 1.34 436 18.7 1,634 120 125 3.5 1.3 41.0 322 188 12 13 14 794 5.0 8.0 9.0	7.08 25.8 0.09 0.04 1.12 4.90 1.37 462 39.3 1,393 8.68 36 300 125 4.1 1.3 31.0 311 201 13 14 16 644 5.0 9.4	6.44 24.0 0.10 0.038 1.06 4.5 1.32 448 33.5 1,360 8.48 46 716 129 4.8 1.3 34 328 230 13 17 15 614 5.0 6.8 21.6	5.91 26.6 0.07 0.036 1.34 3.4 0.96 308 85 1,044 6.13 61 997 129 3.8 1.2 52 370 516 15 15 15 21 670 4.8 17.2 82.4	6.4 26.2 0.07 0.032 1.34 3.24 0.95 311 107 1,093 6.73 66 1,036 146 5.5 1.3 54 345 556 16 15 28 682 5.0 20.3 86	6.81 25.6 0.076 0.035 1.32 3.48 1.04 346 117 1,258 8.00 102 1,425 167 6 1.2 55 347 698 21 12 22 673 5.0 26 97	9.18 23.4 0.064 0.047 1.87 2.31 0.70 203 193 1,200 5.89 182 2,310 185 10.3 1.1 108 267 971 48 13 20 890 4.7 38 186
U (pCi/g) <sup>C</sup>	NA NA	NA NA	NA NA	NA NA	3.2	3.3	7.6	28.9	30.1	34.0	65.1

NA = Not analyzed.

<sup>&</sup>lt;sup>a</sup>Metals are averages for one run only; data for the second run was similar and is included in the PNL report (Serne et al. 1993).

 $<sup>^{</sup>b}$ 1% is equivalent to 10,000 mg/kg.  $^{c}$ Conversion factor for total uranium (mg/kg) times 0.35 = pCi/g for  $^{235}$ U and  $^{238}$ U only.

Figure 7-3a. Test #2, Wet-Sieved Size Distribution of Processed Soils, Uranium-238 Gamma Spectrometry. (Serne et al. 1993)

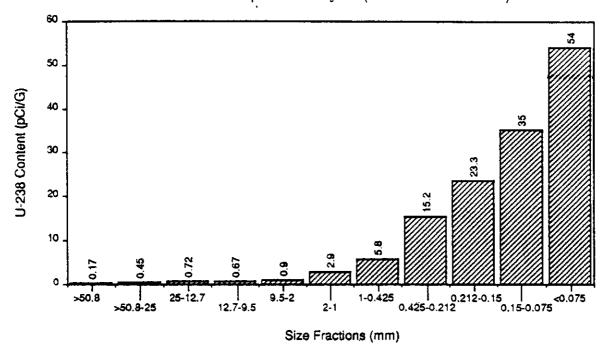
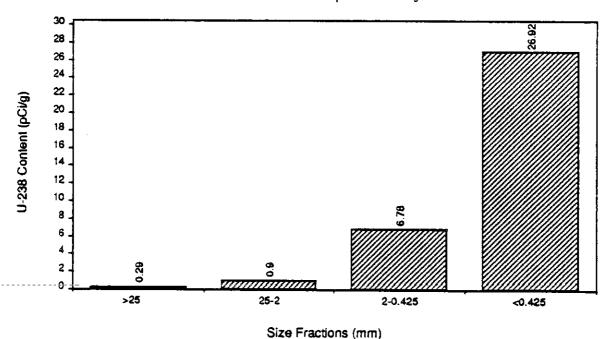


Figure 7-3b. Test #2, Contaminant Concentrations in Each Process Pile, Uranium-238 Gamma Spectrometry.



GEN/M3.9

Figure 7-4a. Test #2, Wet-Sieved Size Distribution of Processed Soils, Uranium-235 Gamma Spectrometry. (Serne et al. 1993).

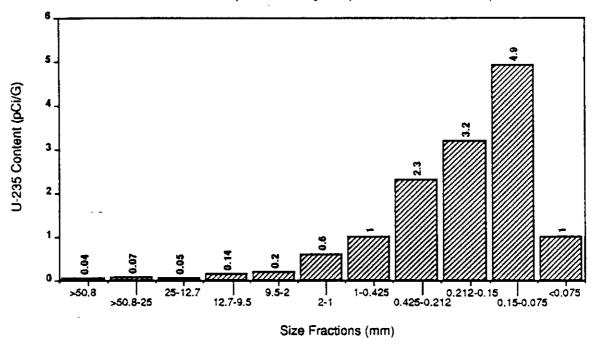
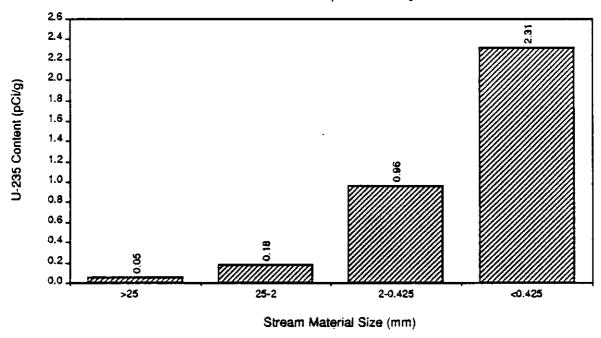


Figure 7-4b. Test #2, Contaminant Concentrations in Each Process Pile, Uranium-235 Gamma Spectrometry.



GEN\M3.10

Figure 7-5a. Test #2, Wet-Sieved Size Distribution of Processed Soils, Cobalt-60 Gamma Spectrometry. (Serne et al. 1993)

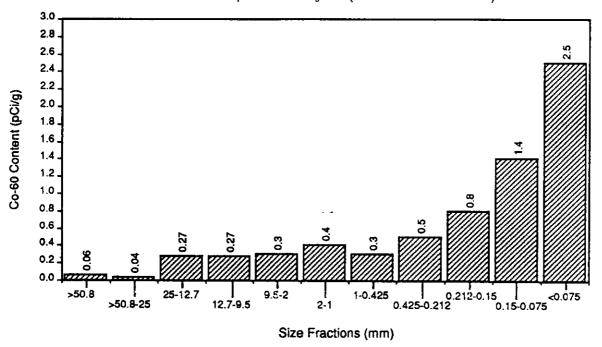
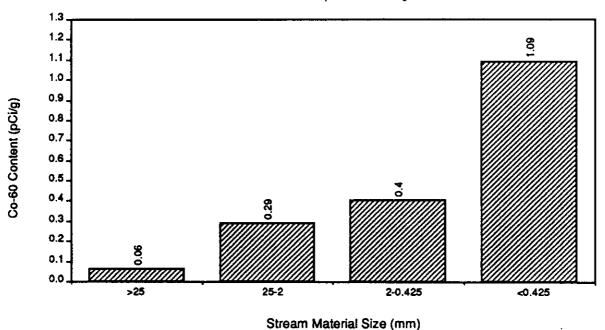


Figure 7-5b. Test #2, Contaminant Concentrations in Each Process Pile, Cobalt-60 Gamma Spectrometry.



GEN\M112593-L

The 2- to 0.425-mm material was unchanged. It still visibly contained particles of the green material, and activity levels of approximately 400 cpm were measured in the field. The 0.425-mm screen was sprayed with water using the spray bar off the primary screen in a further attempt to break down the green particles. The added sprays washed the soils more effectively as they traveled across the screen, but didn't seem to reduce or break down the green material. It was, therefore, determined that an attrition scrubber is likely required. Results from Test #1 showed that an attrition scrubber would break down the green material so that the fraction of fine particles (<0.75 mm) increased and the remaining larger material exhibited significantly lower activity.

Only field measurements were made; no samples were taken to send to the laboratory because radioactivity was found in soil fractions intended to be clean, and sufficient samples of soils with the green material were taken in Test #1.

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#### 8.0 WATER TREATMENT

## 8.1 APPROACH

Preoperational testing of the water treatment unit was performed during the month of September to ensure that all equipment was operating appropriately. Minor modifications/repairs were made based on this test. During the week of September 20, 1993, the clarification portion of the system was transported to the north process pond and prepared to treat the process effluent in the fractionation tanks from Test #1 and Test #2.

Water treatment tests began the first week of November. The tests were conducted using a skid-mounted clarifier obtained from the EPA and renovated for the test. Renovations included replacing pumps, adding pressure gages and water flow gages, and-plumbing.

In spite of previous laboratory indications to the contrary, in Test #1 uranium activity (likely due to the green material) was measured in the process effluent (Tables 6-8 and 6-10). Therefore, based on laboratory stir tests, a commercial flocculant was selected to enhance particle settling rates, and ferric chloride was added to precipitate uranium from the effluent. Effluent was to be treated to remove suspended solids and reduce the concentration of constituents in the effluent to purgewater acceptance levels (Appendix A). In addition to the clarifier, a skid-mounted ion exchange unit was made available, if needed. A schematic of the clarifier and ion exchange system is shown in Figure 8-1.

During the physical separations test, process effluent was redistributed between three fractionation tanks. Most of the effluent was initially pumped into tank #1; therefore, the greatest fraction of sediment is in this tank. When more volume was needed in tank #1, effluent was pumped to tanks #2 and #3. Process effluent was redistributed between the three tanks as needed. Although about 151,000 L of effluent from Test #1 (Figure 6-1) and Test #2 (Figure 7-1) were put in the fractionation tanks, when the water treatment test started, there was approximately 121,000 L of effluent distributed between the three tanks. The difference was due to evaporation during the period between Test #1 and Test #2.

In a full-scale system, process effluent would be treated in-line and recycled. This would reduce the volume of water used in the system. Final treatment or disposal of process water would not generally occur until soil processing is completed.

Samples shown in Table 8-1 were collected before (influent) and after treatment (effluent). One set of samples was collected about midmorning and another at midafternoon. Samples were only collected for offsite analyses on those days when the field supervisor determined that the system was operating adequately.

Samples were sent to offsite laboratories for EPA Level III chemical analyses and Level V radiochemical analyses (EPA 1990). Samples sent to onsite laboratories received EPA level II analyses using inductively coupled plasma/mass spectrometry (ICP/MS).

Solds
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Tank
Soil Washing Waste Water Treatment System
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Figure 8-1. Schematic of the Water Treatment System.

LABORATORY ANALYSIS

and Analyses

DATE	SAMPLE TYPE**	TURBIDITY NTUs	TSS mg/l	HEIS #	SAMPLE TYPE**	Mg mg/L	Al mg/L	Cr mg/L	Cu mg/L	Sr mg/L	Zr mg/L	Ba mg/L	238 <sub>U</sub> mg/L
11/02/93	No Samples			воэвка‡	Influent	4.77	1.34	0.0061	0.345	NR	NR	0.087	5.97
				воэвя5‡	Effluent	4.43	0.155	0.0041	0.160	NR	NR	0.063	4.18
				воэвw2‡	Trip Blank	N/A							
11/04/93	Influent	1.9		B09BR6‡	Influent	4.68	0.0422	0.0041	0.013	NR	NR	0.061	ANP
	Effluent	19.6		во9вп7‡	Effluent	4.62	0.291	0.0077	0.252	NR	NR	0.070	1.49
	Sludge	976	822	воэвка‡	Influent	3.02	0.104	0.0041	0.0131	NR	NR	0.034	2.67
	Influent	17.5	10	воэвкэ‡	Effluent	3.82	0.103	0.0041	0.0389	NR	NR	0.053	1.73
	Effluent	10.6	24	BO9BSO‡	Effluent Dup	3.74	0.078	0.0041	0.0341	NR	NR	0.053	1.37
	Sludge	970-1000	980	809BW5‡	Trip Blank	N/A							
	Influent	4.96	17	BO9BW8‡	Trip Blank	N/A							
	Effluent	6.2	9	B09BW6	Influent-PNL	5.21	DNR	.00108	.0137	.0934	.00191	.0771	1.9
				B09BW7	Effluent-PNL	5.24	.288	.022	.284	.0949	.0195	.0834	4.18
				B09BW9	Influent-PNL	3.33	.0822	.00196	.0102	.051	.00367	.0385	2.84
				воэвхо	Effluent-PNL	4.49	.093	.00344	.0505	.0793	.003	.0662	1.42
				B09BX1	Effluent Dup- PNL	4,53	.0482	.00247	.0363	.0774	.0164	.0659	1.10
11/05/93	No Samples			B09BX2	Sludge-PNL	13.3	15.5	.0821	.308	.124	1.26	.419	114
11/16/93	influent	6.22	4.0	B09BX3	Influent Filtered-PNL	3.84	0.0007	0.0015	0.0055	0.081	0.0003	0.12	0.033
	Influent	11.4	7.0	B09BX4	Influent-PNL	3.86	0.111	0.0057	0.030	0.077	0.0032	0,106	1.66
	Effluent-filtered Influent	0.32 14.3	9.0	B09BX5	Effluent Filtered-PNL	3.86	0.011	0.0012	0.0086	0.076	0.0002	0.126	0.063
	Effluent	20.3	12.0				 			-			

\*\* Referring to Figure 1-3: Influent is Stream #9
Effluent is Stream #10

Sludge is Stream #11

# Additional data provided in Appendix B.3

FIELD ANALYSIS

Analysis is Not Applicable for Trip Blanks Not Requested Analysis Not Possible N/A

NR

ANP DNR Did Not Receive A sample screening trailer was set up in the field to obtain quick analyses to assess system performance. Chromium concentrations were measured in the screening trailer using a Hach kit (a tradename of Hach Company). Turbidity measurements were also made to determine suspended solids concentrations.

#### 8.2 RESULTS

Water treatment operations started on November 2, 1993. The first day of operation consisted primarily of filling the clarification system and establishing constant flow conditions. Process effluent from tank #2 was pumped into the treatment system (about 30,300 L). After treatment, effluent was returned to tank #2. Initial testing began by processing the wastewater at 132 L/min. At this flow rate, ferric chloride was added to the wastewater at a rate of 35 mg/L of water. This was added to the waste stream in the flash mix tank. Next, a cationic polymer was added to the stream leaving the mix tank at a rate of 2 mg/L of water. Judging from the turbidity of the effluent and visual observation inside the tank, few solids remained in tank #2 after one treatment cycle. The water treatment flow rates were 189 L/min when filling the clarifier, and 151 L/min during steady-state processing.

The water treatment system did not operate on November 3, 1993 because repairs were required on the flocculator mixer, which had not worked well the first day of the test. Water treatment operations restarted on November 4. During the morning, process effluent was fed from tank #2. By about 1:00 p.m., tank #2 was empty, so water was fed from tank #1. That afternoon, the ferric chloride feed pump was found to be out of order, so operators began adding ferric chloride by bucket. Water treatment was stopped on November 5 because the concentrated ferric chloride solution attached to the stainless steel pump seal and ruined the ferric chloride feed pump.

Field measurements from the first 2 days of sampling indicated that the flocculation process was working. However, problems with the ferric chloride feed pump prevented optimization of the flocculation process. In addition, it was determined that an in-line filter was needed after the clarifier to remove suspended solids. These problems resulted in 2 wk of downtime.

Water treatment operations restarted November 16. A  $10-\mu$  filter was installed after the clarifier. Ferric chloride was added by a Masterflex peristaltic pump, which did not have any corrosion problems and worked much better for this application. The pump delivered ferric chloride solution to the system at a rate of 10.5 L/hr. Most of the day, pumping pressure was used to open flow channels in the frozen pipes and treatment system. Water was pumped from tank #1 to the treatment system and treated water was returned to tank #1. Only 3 hr of steady-state flow were achieved. Ferric chloride and polymer were added, but suspended particles did not flocculate.

Over the 3 days when treatment occurred, approximately half of the effluent in the fractionation tanks was processed in a single cycle through the clarifier skid.

Several bench-scale tests were performed during the operation of the system in an attempt to optimize the process chemistry. The results of these tests indicated that controlling the amount of ferric chloride is crucial. If more than twice the concentration is added, no settling will occur. The volume of cationic polymer added is not as crucial, however. Large overdoses of polymer only slow the rate of flocculent formation and settling.

At this time, the outside temperature was dropping below 0°C during the nighttime hours. Several attempts were made to continue operations, but the effectiveness of the ferric chloride diminishes significantly at these lower temperatures. It was determined by field operators and engineers that modifications were required for the ferric chloride and flocculents to work effectively in the cold weather. As a result of processing problems caused by the freezing temperatures and to protect the environment from potential leaks caused by freezing of the system, operations were terminated just before Thanksgiving. Effluent was pumped from the water treatment system into the fractionation tanks, and the fractionation tanks were winterized by wrapping the valves with electrical heat tape. Tests are not expected to resume until spring at the earliest.

Analytical results of the tests completed in November 1993 (Table 8-1 and Appendix B.3) indicate that the bulk of uranium was removed from the effluent during the treatment process. Validation reports for the offsite water treatment analyses are in progress and will be included in future revisions of this document.

Based on the tests and analyses on November 16, 1993, optimization of the flocculation process is expected to be successful in treating the effluent in the fractionation tanks when tests results of future treatment will be reported in future revisions of this document.

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## 9.0 RESIDUALS MANAGEMENT

Treatability tests were conducted in a surface contamination area. Therefore, after processing was completed, in accordance with the test plan, soils in each of the process piles were flattened and blended into the surrounding landscape to be remediated in accordance with the record of decision (ROD) for the 300-FF-1 Operable Unit.

Fine soils (<0.425 mm) in the process slurry were gravity-fed to the fractionation tanks. Approximately 32,000 gal of process effluent and associated fines from Test #1 and Test #2 were in the three 75,000-L fractionation tanks at the time water treatment tests started.

The intent of water treatment tests was to cycle effluent through the treatment system back to the fractionation tanks until enough solids were removed from the fractionation tanks and effluent was treated to meet purgewater acceptance standards (Appendix A). However, because water treatment tests were interrupted due to cold weather, only one cycle was completed for about half of the water. When water treatment tests resume, it is anticipated that cycling of the effluent from the tanks through the water treatment system will continue.

Solids separated from the effluent in the water treatment process were pumped to a B-25, LSA box located near the fractionation tanks. To date, approximately 2 yd<sup>3</sup> of fine soils have been removed from the tanks and placed in the B-25 LSA box. Additional boxes are available for when tests resume. The LSA boxes are expected to remain in the bottom of the north process pond according to the waste control plant until final remediation begins, when they will be disposed of with the other 300-FF-1 Operable Unit wastes in accordance with an ROD when it is completed.

Treated effluent was contained in the fractionation tanks. Disposition of the effluent at the conclusion of water treatment tests will be in accordance with the waste control plan. At this time, it is expected that the effluent will be evaporated. The Washington Department of Health was notified of this intent.

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#### 10.0 DATA MANAGEMENT

All data collected during this study was managed in accordance with WHC environmental investigation instructions (EII) (WHC 1988) and the 300-FF-1 Data Management Plan (DOE-RL 1990, Attachment 4).

Samples were assigned a HEIS computer code number, and information associated with the samples will be entered into the HEIS database. Copies of data obtained were forwarded to the Environmental Data Management Center to be placed in the administrative record and/or project records, as applicable.

A field logbook was maintained recording test times, personnel participating, pre-job safety and tailgate meetings, and occurrences during tests. The logbook, currently in use to record water treatment field activities, will be issued and entered into the administrative record on completion.

Samples were managed in accordance with WHC chain-of-custody procedures (WHC 1988, EII 5.1).



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## 11.0 QUALITY ASSURANCE/QUALITY CONTROL

Analytical samples and other investigation activities were subject to in-process quality control (QC) measures and performed in accordance with manuals and procedures specified in the *Remedial Investigation/Feasibility Study Work Plan for the 300-FF-1 Operable Unit* (DOE-RL 1990) in both the field and laboratory. QA samples for tests included duplicates and trip blanks shown in Tables 4-1 and 4-2 and in Appendix B.

Analytical methods, analytical levels, detection limits, precision and accuracy requirements for data receiving Level III and Level V analysis at an offsite laboratory and presented in Appendix B are specified in Table 11-1.

All of the samples receiving Level III chemical analysis and Level V radiochemical analysis were validated using WHC Level B RCRA data validation procedures as required in Section 5.0 of the test plan (DOE-RL 1993b). The two data validation reports, one for Test #1 and one for Test #2, are included as part of Appendix B.1 and B.2 of this report.

### 11.1 DATA QUALIFIERS AND FLAGS

Certain qualifiers and flags have been added to the data by the laboratory or as the result of the data validation. The following qualifiers and flags accompany data in this report.

## • Qualifiers added by the laboratory

- U Indicates that this constituent was analyzed for but undetected.
- L Indicates that the value is less than the contract required detection limit (CRDL) and above the maximum detection limit (MDL).
- B Laboratory blanks exceeded acceptable criteria.
- XYZ Indicates that matrix interference was encountered causing higher detection limits and false results in the gamma scan analysis.

## Flags added as a result of data validation

- Q Data can be used qualitatively, but regulatory decisions should not be made on a single flagged data point.
- H Indicates holding time missed. Data can be used qualitatively, but regulatory decisions should not be made on a single flagged data point.

Table 11-1. Analytical Methods, Detection Limits, Precision and Accuracy.

Category of Analysis	Analyte of Interest	Analytical Level	Analytical Method <sup>a</sup>	MDC (soil) <sup>b</sup> (ppb)	Precision (soil)	Accuracy (soil)	MDC (water) <sup>b</sup> (ppb)	Precision (water)	Accuracy (water)
Radionuclides	Cesium-137	٧	Gamma spectroscopy	0.1 pCi/g	±25	75-125	20 pCi/L	±25	75-125
	Cobalt-60	٧	Gamma spectroscopy	0.1 pCi/g	±25	75-125	20 pCi/L	±25	75-125
	Uranium-totał Uranium-isotopic	V V	Fluorimetry Fluorimetry	0.01 pCi/g 1 pCi/g	±25 ±25	75-125 75-125	0.5 μg/L 0.1 pCi/L	±25 ±25	75 - 125 75 - 125
Metals <sup>C</sup>	Aluminum Antimony Arsenic	111 111 111	6010 6010 7060	20,000 20,000 500	±25 ±25 ±25	75-125 75-125 75-125	200 200 5	±25 ±25 ±25	75-125 75-125 75-125
	Beryllium Cadmium	111 111	6010 6010	300 1,000	±25 ±25	75-125 75-125	3 10	±25 ±25	75 - 125 75 - 125
	Chromium Copper Iron Lead Manganese	111 111 111 111	6010 6010 6010 7421 6010	2,000 2,000 2,000 500 1,000	±25 ±25 ±25 ±25 ±25	75-125 75-125 75-125 75-125 75-125	20 20 20 5 10	±25 ±25 ±25 ±25 ±25	75-125 75-125 75-125 75-125 75-125
	Mercury Nickel Silver Zinc		7470 6010 6010 6010	400 3,000 2,000 1,000	±25 ±25 ±25 ±25	75-125 75-125 75-125 75-125	0.2 30 20 10	±25 ±25 ±25 ±25	75 - 125 75 - 125 75 - 125 75 - 125
Volatile Organic Compounds (VOC) <sup>C</sup>	1,2-Dichloroethene Methylene chloride Tetrachloroethene Trichloroethene	111 111 111 111	8240 8240 8240 8240	N/A N/A N/A N/A	N/A N/A N/A N/A	N/A N/A N/A N/A	1 5 0.5 1	±25 ±25 ±25 ±25	75-125 75-125 75-125 75-125
Pesticides/PBC <sup>C</sup>	Aroclor-1016 through 1260	111	8080	100	±25	75-125	1	±25	75-125

NOTE: This table is compiled from <u>Quality Assurance Project Plan for RCRA Groundwater Monitoring Activities</u> (WHC 1992) and the statements of work for the laboratories.

<sup>&</sup>lt;sup>a</sup>All analytical methods shall be WHC-approved methods.

bMDC refers to minimum detection concentration. Precision is expressed as relative percent difference (RPD) and accuracy is espressed as percent recovery (%R).

<sup>&</sup>lt;sup>C</sup>Methods specified are from <u>Test Methods for Evaluating Solid Waste</u> (EPA 1990).

The XYZ qualifier attached by the laboratory was the result of matrix interference being encountered. This resulted in the laboratory being unable to meet the CRDL and also caused the total error for the analysis to increase. This increase in the error and the low level of the measurements raises the question as to whether or not the analytes were actually detected.

Q flags were given to data for two reasons. These reasons are discussed in the data validation report and include: the relative percent difference between matrix duplicates exceeds 25% and blanks exceeding two times the MDL (this results in a Q flag on all samples of that matrix taken the same day as the blank).

There were no data received from the laboratory with a B qualifier. No data were rejected during the data validation process. Details of what data were flagged and why are given in the data validation reports in Appendix B.2. Flagged data are presented in the tables in this report and were used to calculate averages, but at no time was a single piece of flagged data used to make a recommendation and, in most cases, trends in contaminant concentrations seen in flagged data were confirmed by onsite laboratory analysis.

## 11.2 SUMMARY OF PARCC PARAMETERS

#### 11.2.1 Precision

The data validation reports evaluated the precision in field duplicates. In Test #1, this evaluation resulted in a  $\underline{total}$  of 30 individual constituents among eight different samples being flagged with a Q flag. In Test #2, a  $\underline{total}$  of 22 individual constituents among four different samples were given a Q flag. This meets test criteria.

#### 11.2.2 Accuracy

Accuracy is addressed in Part E of the data validation reports. As discussed above and in the data validation reports, other than the gamma scan data in Test #1 that has an XYZ qualifier, no data were found to have matrix spike, matrix spike duplicate, or surrogate samples met laboratory acceptance criteria as detailed in Table 11-1.

#### 11.2.3 Representativeness

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- 11.2.3.1 Sampling Methods. Representativeness was achieved by using standardized sampling procedures for collection of samples as detailed in the WHC EIIs (WHC 1988, Section 5.2) and by following the sample plan detailed in the test plan (DOE-RL 1993b).
- 11.2.3.2 Analytical Methods, Reporting Units, and Detection Limits. Representativeness of analysis, reporting, and detection limits was achieved by the use of standard analytical methods (Level II and III) and the use of recognized analytical techniques (Level II and V) for determination of radionuclide constituents.

Results were reported in units that are appropriate for comparison purposes with historical and current analytical data.

Detection limits were met with the exception of those variances discussed in the data validation reports.

## 11.2.4 Completeness

As discussed in the data validation reports, completeness is calculated by the number of unflagged data divided by the total number of data expressed as a percentage.

For Test #1 soils, there are 1,256 unflagged data and 1,302 total data giving a calculated completeness of 96%. For Test #1 water, there are 421 unflagged data and 578 total data giving a completeness of 73%. For Test #2 soils, there are 918 unflagged data and 1,122 total data giving a calculated completeness of 82%. For Test #2 water, there are 639 unflagged data and 683 total data giving a completeness of 93%.

Therefore, completeness for the overall test for soils is 90% and for water is 84%. These meet the 80% criteria used in the data validation report. Water treatment data are not included at this time.

## 11.2.5 Comparability

Comparability of data sets was facilitated by the proper reporting of results in correct units and by the analysis of duplicate samples. Results for duplicate samples were acceptable with the exception of the results identified in the data validation reports and Section 11.2.1.

## 11.3 SURVEILLANCES

Environmental QA surveillances of field activities, including sampling, verified that activities examined were performed acceptably in accordance with governing documents.

Offsite laboratory activities are subject to Environmental QA surveillances and appropriate laboratory corrective actions if required.

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## 12.0 COMPARISON OF TEST RESULTS WITH PERFORMANCE STANDARDS

Table 12-1 summarizes test results and test performance levels for primary contaminants of concern discussed in Section 1.2.1. Table 12-1 shows that test performance levels were met in both Test #1 and Test #2 for the 2- to 0.425-mm size process pile, and the total fraction of soil particles >0.425 mm. Although contaminant levels in the 2- to 0.425-mm fraction of soils are higher than in the total soil, in practice, soils from each process stream are combined when returned to the site as clean soils. Therefore, contaminant levels in the "Total Soil Fraction >0.425 mm" is the better measure to compare with test performance levels and other performance standards.

Table 12-2 shows acceptable soil concentrations of uranium-238, uranium-235, cobalt-60, and chromium to meet MTCA residential standards, RESRAD, and 1E-06 cancer risk levels. These levels are included for comparison with target performance levels and test results in accordance with the test plan; these are not soil cleanup levels.

MTCA residential levels apply to chromium only. This level was met in Test #1 and Test #2 soils <9.5 mm.

RESRAD values (Gilbert et al. 1989) are included because these are based on DOE Order 5400.5, which requires soil radioactivity levels <20  $\mu$ R/hr above background levels. Values derived were for a maximum dose of <25 mrem/hr. RESRAD levels were met in Test #1 and Test #2.

Incremental cancer risk (ICR) levels are given for three pathways: ingestion, inhalation, and external exposure. Values for an ICR of 1E-06 were determined using methods and assumptions (DOE-RL 1993c). Except for chromium (which exceeded external exposure levels for chromium VI) in Test #2, the total soils >0.425 met 1E-06 levels for all constituents and pathways. Chromium in the 300-FF-1 Operable Unit is expected to be chromium III, for which there is no known cancer risk. In Test #1, total soils >0.425 mm met 1E-06 levels for the ingestion pathway for all constituents, but exceeded levels for the inhalation and external exposure pathways. ICR values given are based on conservative assumptions and may overestimate risk levels by as much as an order of magnitude (DOE-RL 1993c).

Water-based standards such as drinking water or groundwater standards are not included in Table 12-2. These levels were significantly lower than the test results for uranium-238, uranium-235, cobalt-60, and chromium, and may not be applicable for soil treatment applications.

As stated previously, cleanup levels for soils in the 300-FF-1 Operable Unit have not been established. These will be discussed in the Phase III FS. The milestone to submit a draft of the Phase III FS to EPA and Ecology is August 15, 1994.

Table 12-1. Summary of Test Results and Test Performance Levels for Uranium-238, Uranium-235, Cobalt-60, and Chromium.

	Tes	t #1	Tes	t #2	Test Performance Levels	
Constituent	2 to 0.425 mm <sup>a</sup>	Total soils >0.425 mm <sup>b</sup>	2 to 0.425 mm <sup>c</sup>	Total soils >0.425 mm <sup>d</sup>		
238 <sub>U (pCi/g)</sub>	69.5	27.5	6.8	0.59	370	
<sup>235</sup> U (pCi/g)	8.6	3.6	1.0	0.10	170	
60 <sub>Co (pCi/g)</sub>	1.4	0.6	0.4	0.11	7.1	
Chromium (mg/kg)	178	157	36.4	19.3	1,600	

NA = not applicable.

<sup>a</sup>Values for radionuclides are those measured after attrition scrubbing Table 6-13. Chromium values are for wet-sieving only (Table 6-9).

 $^{b}$ Weighted average values of radionuclides after attrition scrubbing (Figure 6-2b, Table 6-12, and Table 6-13). The concentration of chromium in particles >9.5 mm (not measured) is assumed to be the same as in particles between 9.5 and 2 mm.

<sup>C</sup>Values are derived from Table 7-7.

 $^{\hbox{d}}\mbox{Weighted}$  average values are derived from Tables 7-5, 7-7, and Figure 7-2b. The concentration of chromium in particles >9.5 mm (not measured) is assumed to be the same as in particles between 9.5 and 2 mm.

Table 12-2. Comparison Levels for Uranium-238, Uranium-235, Cobalt-60, and Chromium.

B	MTCA,	DECRAP	1E-6 Cancer Risk <sup>a</sup>				
Constituent	residential standards	RESRAD	Ingestion	Inhalation	External Exposure		
238 <sub>U (pCi/g)</sub>	NA	426	240	3.8	13		
<sup>235</sup> U (pCi/g)	NA	142	430	8	2		
60 <sub>Co</sub> (pCi/g)	NA	7.0	460	1,300	0.055		
Chromium (mg/kg)	80,000 <sup>b</sup>	NA	NA <sup>C</sup>	NAC	NA <sup>C</sup>		

 $<sup>^{\</sup>rm a}$  Equations and assumptions for these calculations are provided (DOE-RL 1993c, Section 6.2).  $^{\rm b}$ MTCA. Method B (Ecology 1993).

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<sup>&</sup>lt;sup>C</sup>Chromium III is not a known carcinogen.

### 13.0 DEVIATIONS FROM THE TEST PLAN

Many of the deviations from the test plan were discussed with RL, EPA, and Ecology, and verbal approval was given to proceed prior to implementing changes. These changes and other field changes agreed to by the field team leader and project engineer are identified in this section.

Deviations to the test plan included the following:

- MTCA, Method C, industrial minimum (test) performance levels in Table 3-1 of the test plan (DOE-RL 1993b) were revised per updates by Ecology (1993). The revised levels are generally higher than those in the test plan.
- In Tests #1 and #2, about half the material discussed in the test plan was processed. This was due to two factors. First, the system used was designed and built under a very tight schedule and only available equipment could be used; consequently, there were many breakdowns and delays resulting in the processing of less material. Second, in Test #1 it was obvious early on from field measurements that radioactivity was present in each of the processed piles of soil; consequently, nothing would have been gained by processing more material.
- Green material was processed in Test #1, while the test plan states that it would not be processed. Reasons for this were given in Section 6.0.
- The test plan schedule shows that Test #1 would be performed the first 2 wk of June and Test #2 the last 2 wk. Due to additional testing and analyses of the green material and significant modifications to equipment, Test #2 was not completed until September.
- Laboratory attrition scrubbing tests were not identified in the test plan. These were necessary because the trommel and screens did not adequately break down material in Test #1. Laboratory attrition tests were conducted in accordance with 100 Area Soil Washing Bench-Scale Test Procedures (Freeman et al. 1993).
- Sample numbers and times for the runs varied from the test plan. Fewer effluent samples were taken than anticipated because of shorter processing periods. Effluent samples were collected at approximately 1-hr intervals. Also, two sets of samples were collected during June rather than one; one set on June 23 and another June 25. Additional samples were also collected from the 0.425- to 2-mm and 2- to 25-mm process piles after a final short run on June 29. One set of soil and water samples was collected in September for Test #2.
- The 0.425-mm screen was used in Test #2 as opposed to the 0.212-mm screen, and feed soils were obtained from new locations in the north process pond to avoid the green material. Reasons for these changes are discussed in Section 6.0.

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### 14.0 COST

This section looks at the potential costs that might be expected for a full-scale operation. These estimates were based on knowledge gained during this test and address <u>only</u> the operating costs.

The following assumptions were made regarding full-scale operation:

- Processing rate is 100 tons/hr.
- Single shift of processing/day.
- Hours of processing/shift is 5 hr.
- Number of processing days/year is 250 days.
- All preventive maintenance occurs during an off shift.
- Fresh water to feed the plant and for dust control will be supplied by pipeline.
- Electrical power will be supplied by lines.
- Numerous samples will be taken during the shift for field screening to control the process.
- Two additional samples will be taken every process day (one for clean material, one for waste material). The clean samples will be composited for 1 wk to make one sample, which will be analyzed using EPA Level III and Level V analytical methods (EPA 1990). The same will be done with the waste sample.
- 20% of the samples receiving EPA Level III analysis will be validated (the number validated for 300-FF-1 characterization work).
- When feasible, work will be performed by onsite employees.

Five factors were looked at in developing these costs. They were labor, materials and consumables, utilities, analytical costs, and maintenance costs. Overhead costs are not included. In addition, a 20% contingency was added.

#### 14.1 LABOR

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Labor is composed of two groups: those directly involved with the operation of the plant and the support labor necessary for the day-to-day operation. Table 14-1 details the expected direct labor personnel requirements, and Table 14-2 details the anticipated requirements for support labor.

Personnel	FTEs	Annual Cost per FTE, \$	Total Annual Cost, \$
Plant Operators	2	65,000	130,000
Equipment Operators	3	65,000	195,000
Sampler/Lab. Tech.	3	65,000	195,000
Supervisor	1	65,000	65,000
Total	9		585,000

Table 14-1. Direct Labor Requirements.

FTE = full time employee.

Total

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Personnel	FTEs	Annual Cost per FTE, \$	Total Annual Cost, \$
Health Physics Tech.	2	65,000	130,000
Site Safety Officer	1	65,000	65,000
Maintenance	2	65,000	130,000
Fuel Truck Driver	0.5	65,000	33,000

Table 14-2. Support Labor Costs.

It is anticipated that full-scale operation will require two full-time plant operators. During the test, three people were required to oversee the operation; however, it is anticipated that the full-scale plant would be more automated and only require two operators.

5,5

358,000

Three equipment operators will be necessary to perform the material handling. Two people will be involved in feeding the plant (one dozer and one loader) and one loader operator will handle the processed streams coming out of the plant.

Three people will take samples of the process streams and do field screening tests (XRF and gamma scans) for process control.

There will be one full-time supervisor/engineer for the operation.

It is expected that two Health Physics technicians will be required during the operation. Two were necessary for the test and two should be adequate for the full-scale operation.

One site safety person will be sufficient for the operation. One person was adequate to cover the test.

Two maintenance people will be required to perform preventive maintenance on the plant and the equipment when they are shut down. These two maintenance FTEs will also cover any electrical work required. The fuel truck driver is included to fuel the equipment and to serve as a third maintenance person.

## 14.2 MATERIALS AND CONSUMABLES

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This section estimates the amount of materials and consumables that will be used by a full-scale operation. Table 14-3 details the items considered in this section.

Item	Total Annual Cost, \$
Water for makeup and dust control	7,000
Water treatment flocculents	62,000
Laundry	66,000
Safety equipment and supplies	5,000
Signs, ropes, fences, etc.	5,000
Dust control equipment and supplies	5,000
Tools	1,000
Garbage	5,000
Miscellaneous materials (steel, timber, etc.)	10,000
Total	161,000

Table 14-3. Materials and Consumables Costs.

It is estimated that a full-scale plant that recycles its water will require 265 L/min to feed the system. This is based on the amount of water lost to the various piles during the test and adjusted for a 100-ton/hr system. It is substantiated by the fact that during a visit to see the soilwashing plant at the King of Prussia Site in New Jersey, site personnel stated that their 25-ton/hr plant required approximately 76 L/min of feed water.

Based on the work done during the test, it is estimated that approximately 189 L/ton of material processed will be required for dust control. Some of this water goes on the material to be washed and some goes onto the roadway where the equipment is traveling. That amounts to 314 L/min for dust control.

Total water required to feed the plant would be 579 L/min. This amounts to 42.58 million L/yr and will cost about \$7,000 at city of Richland water costs.

The estimates used to establish the baseline operating parameters for the water treatment system processing the water from the test give a cost of approximately \$0.50/ton of material processed for flocculents to treat water.

Laundry will cost approximately \$6/person to dress out one time (\$2/lb, 3 lb/set of whites). There are 14.5 FTEs, but not all will dress out every day. Assuming that an average of 11 dress out four times per day for 250 days, that amounts to 11,000 sets/yr or \$66,000/yr for laundry.

An estimate of \$5,000/yr was made for safety equipment and supplies. This covers ear plugs, safety glasses, hard hats, face shields, plastic pants and coats, safety harnesses, instruments required by the site safety officer, first aid kits, eye wash units, showers, etc.

A total of \$5,000/yr was included for signs, ropes, and fences. This may be higher for the first year and less after that, but \$5,000/yr is estimated.

For dust control, a sprinkler system would be set up to pre-wet the excavation area and roadways prior to the beginning of work. A total of \$5,000 was included to cover this simple system, which would lay on top of the ground.

Garbage disposal costs for tape, paper, plastics, etc., are estimated to be \$5,000/yr.

For the operators to make adjustments to the equipment from time to time and to clean the equipment as required, a set of tools will be required. A total of \$1,000 is included.

As is the case with any operation, there are numerous miscellaneous items that are not covered elsewhere. Therefore, \$10,000 has been included here for those items.

#### 14.3 UTILITIES

This section addresses the costs related to the utilities that will be needed during full-scale operation. Table 14-4 details these costs.

It is estimated that a full-scale system based on the plant utilized for the test could require 260 kW in various motors. These would include conveyors, vibrating screens, pumps, trommels, autogenous grinders, attrition scrubbers, etc. The total estimated power required would be 260 kW/hr for 7 hr/day with a demand of approximately 260 kW for any 15-min period. A figure of \$0.035/kW-hr is used for the usage cost, plus \$5,000 additional for the demand cost for a total of \$21,000/yr.

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Item	Total Annual Cost, \$
Electricity	21,000
Diesel Fuel	31,000
Gasoline	2,000
Total	54,000

Table 14-4. Utility Costs.

Diesel consumption for two front-end loaders and a dozer is estimated to be 114 L/hr of operation based on tables from the Caterpillar (a trademark of Caterpillar, Inc.) Performance Handbook, 22 Edition. A cost of \$0.22/L for diesel was used. Gasoline is a minor cost for pickups, and a total cost for fuel of \$2,000/yr is estimated.

#### 14.4 ANALYTICAL COSTS

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Analytical costs associated with a full-scale operation are assessed. Table 14-5 details these costs.

Item		Total Annual Cost, \$
Analysis		130,000
Sampling equipment and supplies		15,000
Data validation		26,000
	Total	171,000

Table 14-5. Analytical Costs.

Analytical costs are based on the costs incurred under the contracts that were used for the test. The total cost for analysis with expedited turnaround time was approximately \$1,300/sample. The total cost for two samples per week comes to \$130,000/yr.

Sampling equipment and supplies will also include field screening equipment such as an XRF analyzer, hand-held gamma detectors, bottles, spoons, coolers, ice, etc. This cost will likely be high during the first year and much less the following years. An average cost of \$15,000/yr is estimated.

Data validation costs are difficult to predict dependent on what is required, but could cost as much per sample as the analysis itself. Using this as a conservative number and assuming that 20% of the data will require validation, a total cost of \$26,000/yr would be incurred.

#### 14.5 MAINTENANCE COSTS

Maintenance costs anticipated for a full-scale operation are provided in Table 14-6.

Item	Total Annual Cost, \$
Parts	100,000
Tools	1,000
Miscellaneous (lubricants, solvents, rags, etc.)	20,000
Total	121,000

Table 14-6. Maintenance Costs.

Parts for this cost analysis include conveyor belts, loader tires, replacement screens, belts, filters, hoses, pump impellers, and all other miscellaneous parts that will be required to operate and maintain the plant and associated equipment. This cost is strictly an estimate, since the test did not last long enough to establish any baseline numbers. A figure of \$100,000/yr will be used.

A figure of 1,000/yr is included for tools. This is in addition to the 1,000/yr for tools for the operators.

Another miscellaneous category includes lubricants and solvents. An estimate of \$20,000/yr is used.

## 14.6 COST SUMMARY

Combining individual costs, the entire cost for operating a full-scale plant was determined. Table 14-7 shows a summary of this.

As can be seen from the costs in Table 14-7, the anticipated operating cost for the full-scale soil-washing plant is \$13.92/ton of material processed. This is believed to be a conservatively high cost based on the assumptions made and added contingencies. It is also anticipated that this cost could be reduced by increasing the processing rate, increasing the number of days of operation, and/or increasing the number of shifts worked per day.

It should be noted that there are additional costs for a project that are not included in the operating costs. These include the capital costs involved with the purchase, mobilization, and construction of the plant; the cost for installation of electrical and water lines; costs associated with hauling and disposal of process wastes; and overhead costs for various organizations involved. These items will need to be assessed in comparing soil washing with other remedial alternatives.

Table 14-7. Full-Scale Operation Cost Summary.

Item	Total Annual Cost, \$	Total Cost/Ton Processed, \$
Labor-direct	585,000	4.68
Labor-support	358,000	2.86
Materials and consumables	161,000	1.29
Utilities	54,000	0.43
Analytical	171,000	1.37
Maintenance	121,000	0.97
Subtota1	1,450,000	11.60
Contingency (20%)	290,000	2.32
Total	1,740,000	13.92

One of the benefits of performing the vendor test, in addition to the tests reported, is to obtain better cost and scale-up information from a commercially proven system. As noted previously, the system used for tests in this report was made up of equipment components that were available at the time and were not necessarily designed to work together.

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The overall objective of the test was to evaluate the use of physical separations systems as a means of concentrating chemical and radiochemical contaminants into fine soil fractions, thereby minimizing waste volumes. The minimum test performance levels are shown in Table 2-1. The goal for the test was to achieve a 90% (by weight) reduction in contaminated soils (WHC 1991).

The RI report, analyses by Serne et al. (1992), and this treatability test showed that the primary risk driver in the 300-FF-1 Operable Unit is uranium-238 and uranium-235. Analytical data presented in Section 3.0 show that all other contaminants in soils sampled were below test performance levels prior to processing. These performance levels were established as goals for the test, they are not soil cleanup standards. While final cleanup standards for 300-FF-1 soils have yet to be determined, these will be critical to assessing the effectiveness of remedial alternatives.

In general, the physical separation system tested met the test goals, thereby demonstrating the potential to reduce the amount of contaminated soils in the 300-FF-1 Operable Unit without the use of chemical processes. Therefore, physical separation of excavated soils prior to disposal is an alternative that should be carried in the Phase III FS.

In Test #2, offsite analytical results of soil piles after processing showed that soils representative of the largest fraction of the 300-FF-1 Operable Unit waste sites (not containing green material) were separated so that the concentration of uranium was significantly lower in the coarse fraction of soils (12 pCi/g for >0.425-mm particles and 93.63 pCi/g for <0.425-mm particles). Onsite laboratory analyses showed similar results. These levels are significantly lower than test performance levels of 370 pCi/g for uranium-238 and 170 pCi/g for uranium-235, and lower than comparison levels discussed in Section 3.5. The cutpoint of 0.425 mm, resulted in a 98.6% reduction by weight in the amount of contaminated feed material.

While uranium-238 and uranium-235 radioactivity levels were of primary concern, Test #2 laboratory analyses using XRF (Table 7-7) showed that the concentration of copper and uranium elements in the soils was reduced proportionally. Therefore, copper or uranium are potential indicator analytes for future tests or during site remediation.

While physical separation processes were effective for these soils, it is recommended that careful consideration be given in the Phase III FS as to the benefit versus cost of processing soils within the 300-FF-1 Operable Unit that are near background levels and below test performance levels prior to processing.

Test #1 showed that soils containing the green material can likely be processed with the addition of an attrition scrubber to the system tested. This finding exceeded the scope of the test plan, which originally excluded processing of soils containing the green material due to laboratory indications that physical separation processes may not be effective for this material (Dennison et al. 1989).

After processing, radioactivity was measured in the field in each of the process piles. Analytical tests confirmed that, as expected, the green material was the primary source of the radioactivity and that uranium-238 was the primary radioactive isotope. However, after wet-sieving in the laboratory, green material was broken down so that gamma spectrometry analyses showed that soils met performance levels for 94% by weight of the feed soils (>0.15 mm).

Laboratory tests also showed that attrition scrubbing further separated particles containing the green material such that soil particles >0.075 mm met test performance levels. The highest concentrations of uranium-238 and uranium-235 in soil fractions >0.425 mm were <50 and <5 pCi/g, respectively. In the laboratory attrition tests, as much as 10% to 12% more fines were generated in the material scrubbed (Table 6-12). This is equivalent to 4% to 5% more fines in the feed soils. The overall reduction in the amount of contaminated soils would be approximately 85% by weight (Section 3.2.2).

Field-scale attrition scrubber tests are recommended to verify laboratory tests can be duplicated in the field and further verify the effectiveness of using attrition scrubbing to treat soils containing the green material. An attrition scrubber has been purchased and is expected to be incorporated as part of the vendors test.

Physical separation processes are not recommended for treating concentrated soil fines such as the intact green layer or fly ash. Excavation and direct disposal may be the preferred alternative for this material.

Cost estimates (Section 4.0) for a full-scale physical separations system to operate at 100 ton/hr were estimated at approximately \$14/ton of material. This figure is for operating costs only. It does not include disposal, overhead, or capital costs for equipment and mobilization. Capital costs among vendors range from roughly \$1,000,000 to over \$5,000,000. As of December 1993, Hanford disposal costs during remediation were unknown. However, physical separation and volume reduction is expected to be economically competitive with direct disposal.

The water treatment test and vendor test are tentatively scheduled to be completed in the spring of 1994. Per the January 1994 unit managers meeting minutes, test results will be documented in WHC support documents to be reviewed by DOE-RL, Ecology, and EPA. Information from these tests, and information contained within this report will be used in the Phase III FS, scheduled to be completed by August 15, 1994. A detailed schedule for additional water treatment and vendor tests was not included because the schedule is dependent on vendor contract modifications, approval of the vendor's system, cold weather conditions, and priority allocation of resources.

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# APPENDIX A

# PURGEWATER ACCEPTANCE STANDARDS

Table A-1. Purgewater Acceptance Standards.

Analyte	Units	Concentration
Metals (inorganics)	ppb	
Aluminum Antimony Arsenic Beryllium Cadmium Chromium Copper Iron Lead Manganese Mercury Nickel Silver Uranium Zinc		N/A 16,000 480 53 11 110 120 3,000 32 500 0.1 1,600 10 590 1100
<u>Organics</u>	ppb	
1,2-dichloroethylene Methylene chloride Tetrachloroethylene Trichloroethylene		70 N/A 8,400 50
PCB	ppb	N/A
Radiochemical Contaminants	pCi/L	
Cesium-137 Cobalt-60 Uranium		2,000 1,000 400

NOTE: Values are from WHC Environmental Compliance Manual, Section 8, "Water Quality" (WHC 1991).

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# APPENDIX B

## ANALYTICAL DATA

## **B.1 ANALYTICAL DATA FOR TEST #1**

### DOE/RL-93-96, Rev. 0

## DATA QUALIFIERS FOR ANALYTICAL DATA

- U Indicates that this constituent was analyzed for but undetected.
- Indicates the value is less than the Contract Required Detection Limit (CRDL) and above the Method Detection Limit (MDL).
- Q Data can be used qualitatively, but regulatory decisions should not be made on a single flagged data point.
- H Indicates holding time missed. Data can be used qualitatively, but regulatory decisions should not be made on a single flagged data point.
- XYZ indicates matrix interference was encountered causing higher detection limits and false results in the gamma scan analysis.

	TE	ST #1 SOIL RAW FEED	WASHING RES	ULTS							
		JUNE 1993 PROCESSING									
	B07C09 soil mg/kg	B07C10 soil mg/kg	B07C11 soil mg/kg	B07C67 soil mg/kg	B07C38 soil mg/kg	807C39 soil mg/kg	B07C40 soil mg/kg				
Ag	67	29	9.6_	9.4	8.7	18	5.1				
At	31000	22000	19000	18000	24000	22000	22000				
As	3.8	2	1.7	1.7	1.9	1.5	2.7				
Ва	270	700	1300 Q	570 Q	1600	1200	1800				
Be	0.75	0.93	U	U	U	1.5	υ				
Ca	17000	12000	9600	8000	10000	11000	10000				
Cd	1.7	υ	0.52L	U	0.51L	U	U				
Co	6.1	6.4	6.9	7.2	7.3	7.1	7.2				
Cr	520	280	160 Q	100 Q	150	220	140				
Cu	10000	3500	910 ଦ	1200 Q	930	2500	300				
Fe	14000	16000	18000	17000	18000	18000	17000				
Нд	3.1	2.9	1.9	1.2	2.5	2.6	2.2				
<b>x</b>	540	980	1200	1300	1300	900	1100				
Mg	8000	6600	5700	5400	6300	6300	6400				
Mn	250	260	260	270	250	240	240				
Na	1000	1600	2100	1900	2800	2100	2800				
Ní	940	380	110	130	99	240	45				
Pb	83	40	36_	29	60	49	38				
Sb	12L	7.4L	10LQ	6.9LQ	U	5.2L	υ				
Sn	41	25	20 Q	UQ	20	18	25				
v	34	35	37	45	38	36	35				
Zn	150	95	75	56	77	85	69				
	pCi/g										
Co-60	0.0715 XYZ	0.0671 XYZ	0.0298 XYZ	0 XYZ	0 XYZ	0.0408 XYZ	0.062 XYZ				
Cs+137	0.129 XYZ	0.144 XYZ	0.14 QXYZ	0.18 QXYZ	0.264 XYZ	0.272 XYZ	0.181 XYZ				
Pb-212	1.84 XYZ	1.32 XYZ	0.89 QXYZ	1.38 QXYZ	0.817 XYZ	1.53 XYZ	1.81 XYZ				
Pb-214	0.38 XYZ	0.604 XYZ	0.528 XYZ	0.57 XYZ	0.586 XYZ	0.547 XYZ	0.509 XYZ				
Ra-224	0.347 XYZ	0.591 XYZ	0.48 QXYZ	1.4 QXYZ	0.42 XYZ	0.615 XYZ	0.522 XYZ				
Ra-226	1.87 XYZ	1.34 XYZ	0.904 XYZ	0.535 XYZ	0.83 XYZ	1.55 XYZ	1.84 XYZ				
Ru-106	0.0687 XYZ	O XYZ	0 XYZ	0 XYZ	0.182 XYZ	0.25 XYZ	0.08 XYZ				
Sb-125	0 XYZ	0.0178 XYZ	0.0087 XYZ	0 XYZ	0 XYZ	0.1 XYZ	0.157 XYZ				
	pCi/g										
U-Nat	3360	2220	2650 Q	663 Q	1280	775	1670				

U-Analyzed for but undetected Q=Can be used qualitatively

L=Less than CRDL and above MDL XYZ=Matrix interference encountered

		WASHING RESULTS R (UNFILTERED)								
	FRESH WATER (UNFILTERED)  JUNE 1993 PROCESSING									
	B07c70 water mg/L	807C71 water mg/L	B07C72 water mg/L							
Ag	U	U	U							
AL	0.19 L	0.12 L	0.13 L							
As	U	<u>u</u>	U							
Ва	0.026	0.026	0.026							
Be	U	U	U							
Ca	20	17	17							
Cd	U	U	U							
Co	U	U	U							
Cr	U	U	U							
Cu	0.0068 L	0.0063 L	0.0073 L							
Fe	0.46	0.4	0.39							
Нg	U	U	U							
К	1.2	0.75 L	0.81 L							
Mg	4.6	3.9	4							
Mn	0.013	0_011	0.011							
Na	3.2	2.6	2.6							
Ni	U	υ	U							
РЬ	0.002 L	0.0072	0.0069							
Sb	U	U	U							
Sn	U	U	Ų							
ν	0.0047 L	U	U							
Zn	0.0058 L	0.0045 L	0.0055 L							
	pCi/L	pCi/L	pCi/L							
Co-60	7.6	9.76	1.91							
Cs-137	2.01	0.433	4.87							
Pb-212										
Pb-214										
Ra-224										
Ra-226										
Ru-106	11	12.3	0							
Sb- 125	0	0	0							
	ug/L	ug/L	ug/L							
U-Nat	0.28	1.18	0.339							

U=Analyzed for but undetected

L=Less than CRDL and above MDL

	TEST #1 SOIL WASHING RESULTS 25 mm TO 2mm (June 1993 Processing) (sheet 1 of 2)															
,	B07C14 soil mg/kg	B07C15 soil mg/kg	807C16 soil mg/kg	B07C17 soil mg/kg	B07C18 soil mg/kg	B07C19 soil mg/kg	B07C20 soil mg/kg	B07C21 soil mg/kg	807C22 soil mg/kg	B07C23 soil mg/kg	BO7C24 soil mg/kg	B07C25 soil mg/kg	B07C43 soil mg/kg	B07C44 soil mg/kg	B07C45 soil mg/kg	BO7C46 soi mg/kç
Ag	5.4	8.1	5.1	5.5	2.5	4.8	4.3	11	0.99 L	1.7	0.58 L	4.7	13	3.1	υ	17
Al	21000	31000	8500	5800	3700	11000	6900	13000	3900	4900 L	4400	12000	15000	22000	4000	20000
As	1.5	0.9	0.64	0.2 L	0.58	0.65	1	0.81	0.98	0.59	0.64	0.96	3.5	1.1	U	2.5
Ba	100	160	110	79	60	200	110	170	170	100	80	90	180	70	61	200
Ве	Ų	0.52	J	0.2	0.15 L	o ·	U	U	U	U	0.14 L	U	0.79	0.32	U	1
Ca	5900	8700	6700	3600	4100	6600	6200	7600	4100	5000	1500	6100	8500	4100	1000	11000
Cd	U	U	U	U	U	υ	υ	0.73 L	U	υ	0.35 L	U	U	U	0.39 L	0.65
Со	7.7	9.8	8.7	2.3	5.9	9.8	8.5	6.6	5.7	8.2	4.5	8.1	10	2.9	2.7	8.1
Cr	59	100	58	58	23	36	50	140	20	20	17	62	150	32	5.2	170
Cu	1300	2100	1200	1200	320	650	1100	2600	280	370	130	1300	3300	770	61	4400
Fe	20000	23000	21000	8500	13000	25000	26000	17000	16000	22000	7500	20000	26000	7400	5000	19000
Hg	0.37 L	1.6	0.08 L	1.5	0.39 L	0.1 L	0.3 L	0.1 L	U	0.37 L	0.41	2.2	0.89	0.42	1.7	2.6
K	360	410	630	210	340	440	660	360	480	440	1500	460	410	200	650	620
Mg	3700	4500	4500	1800	2200	4500	4200	4000	2500	3800	3900	4000	7500	1800	2100	6100
Mn	210	290	240	95	320	340	410	200	170	250	87	260	310	74	71	280
Na	750	1000	780	370	430	840	860	780	410	680	240	710	850	650	720	1300
Ni	92	180	100	100	34	57	80	230	31	35	14	95	250	52	12	300
Pb	7	7.2	15	4.5	11	12	13	22	19	13	8	12	60	20	16	42
Sb	5.5 L	U	U	U	U	U	U	U	U	U	U	υ	U	8.3 L	U	l
Sn	U	15	U	U	6.7 L	U	U	6.6	5.9 L	U	U	υ	5.7	10	0	6.8
v	59	76	54	27	34	55	48	45	48	71	18	50	61	20	20	49
Zn	52	85	62	33	33	58	49	74	41	46	16	56	93	27	6.7	8

	TEST #1 SOIL WASHING RESULTS (25 mm to 2 mm (June 1993 Processing) (Sheet 2 of 2)															
	B07C14	B07C15	B07C16	B07C17	B07C18	B07C19	B07C20	B07C21	B07C22	B07C23	B07C24	B07C25	B07C43	B07C44	B07C45	B07C46
	pCi/g	· pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g
60 <sub>Co</sub>	0.0245 XYZ	0.013 XYZ	0.029 XYZ	0.031 XYZ	0.032 XYZ	0.003 XYZ	0.035 XYZ	o xyz	0 XYZ	0.009 XYZ	0 XYZ	0.003 XYZ	0.009 XYZ	0.025 XYZ	0.044 XYZ	0.064 XYZ
137 <sub>Cs</sub>	0.0724 XYZ	0.03 XYZ	0.036 XYZ	0.034 XYZ	0.049 XYZ	0.039 XYZ	0.057 XYZ	0.082 XYZ	0.103 XYZ	0.056 XYZ	0.043 XYZ	0.034 XYZ	0.084 XYZ	0.106 XYZ	0.124 XYZ	0.059 XYZ
212 <sub>Pb</sub>	0.811 XYZ	0.649 XYZ	0,886 XYZ	0.69 XYZ	0.824 XYZ	0.83 XYZ	0.687 XYZ	0.704 XYZ	0.896 XYZ	0.66 XYZ	0.622 XYZ	0.688 XYZ	1.34 XYZ	1.54 XYZ	1.42 XYZ	1.9 XYZ XYZXYZ
214 <sub>Pb</sub>	0.463 XYZ	0.497 XYZ	0.403 XYZ	0.375 XYZ	0.363 XYZ	0.521 XYZ	0.498 XYZ	0.399 XYZ	0.526 XYZ	0.43 XYZ	0.383 XYZ	0.465 XYZ	0. <b>439</b> XYZ	0.455 XYZ	0.443 XYZ	0.445 XYZ
224 <sub>Ra</sub>	0. <b>449</b> XYZ	0,498 XYZ	0.358 XYZ	0.475 XYZ	0.426 XYZ	0.42 XYZ	0.55 XYZ	0.344 XYZ	0.576 XYZ	0.392 XYZ	0.357 XYZ	0.408 XYZ	0.459 XYZ	0.455 XYZ	1.45 XYZ	1.94 XYZ
226 <sub>Ra</sub>	0.823 XYZ	0.659 XYZ		0.7 XYZ	0.836 XYZ	0.843 XYZ	0.698 XYZ	0.715 · XYZ	0.91 XYZ	0.67 XYZ	0.632 XYZ	0.699 XYZ	1.36 XYZ	1.57 XYZ	0.39 XYZ	0.46 XYZ
106 <sub>Ru</sub>	0 XYZ	0 XYZ	0.08 XYZ	0.164 XYZ	0 XYZ	0 XYZ	0.167 XYZ	0.071 XYZ	0.225 XYZ	0.061 XYZ	0 XYZ	0 XYZ	0 XYZ	o xyz	0 XYZ	0 XYZ
125 <sub>Sb</sub>	0 XYZ	0 XYZ	o xyz -	0 XYZ	0.027 XYZ	0 XYZ	0.054 XYZ	0 XYZ	0 XYZ	0 XYZ	0 XYZ	0.042 XYZ	0.028 XYZ	o xyz	0 XYZ	0.027 XYZ
	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g
U (total)	527	64.2	1820	1420	3870	272	61.3	111	185	272	131	1200	509	540	188	1480

U=Analyzed for but undetected Q=Data can be used qualitatievely XYZ=Matrix interference encountered L=Less than CRDL and above MDL H=Holding time missed

				TES		IL WASH TO 0.4	ING RESUL 25mm	TS			· · · · · · · · · · · · · · · · · · ·	
	JUNE 1993 PROCESSING											
	B07C26 soil mg/kg	B07C27 soil mg/kg	B07C2B soil mg/kg	B07C29 soil mg/kg	B07C30 soil mg/kg	BO7C3 1 soil mg/kg	B07C32 soil mg/kg	B07C68 sail mg/kg	B07C55 soil mg/kg	B07C56 sail mg/kg	B07C57 soil mg/kg	B07C58 soll mg/kg
Ag	10	12	9.2	12	9.7	11	10	11	11	14	12	12
Al	17000	18000	13000	15000	14000	16000	14000	17000	17000	17000	16000	18000
As	1.4	1.6	0.94	0.87	1.5	2 Q	1.7	0.B1 Q	1.8	1.4	1.8	1.5
Ва	300	340	360	460	280	370	380	330	470	470	570	480
Ве	U	U	U	υ	U	U	U	U	U	0.82	U	U
Ca	7000	7900	6200	8100	8500	8100	7100	8600	8400	10000	8300	9200
Cd	0.47 L	U	U	U	υ	U	υ	υ	0.48 L	0.54 L	0.43 L	U
Со	6.6	5.9	5.9	7.6	6.1	6	6.9	7	5.9	7	6	5.5
Cr	120	120	97	140	99	110	110	110	130	160	130	140
Cu	1400	1400	1300	2200	1500	1600	1700	1700	2800	3200	2800	2700
Fe	18000	17000	17000	19000	18000	18000	18000	18000	16000	17000	15000	17000
Hg	1.1	0.97	0.83	0.79	0.96	0.96	1.4	1	1.1	1.8	1.4	1.8
ĸ	720	790	660	690	760	850	690	870	700	750	780	800
Mg	5300	5000	4900	5500	5400	5300	5100	5500	5300	5900	5400	6100
Mn	260	240	210	240	310	240	230	270	220	240	200	230
Na	2000	1400	1000	1 200	1200	1200	1100	1500	1200	1400	1300	1600
Ni	150	150	130	200	150	150	170	160	210	230	200	210
Рь	28	31	29	30	27	29	29	32	35	44	38	42
Sb	U	5.1 L	U	5.6 L	Ü	4.7 L	U	U	U	6.1 L	C	٥
Sn	8.5 L	17	U	19	12	υq	14	9.4 LQ	24	21	21	19
v	45	42	42	46	47	45	46	55	47	51	42	52
Zn	61	61	59	68	58	61	63	58	66	77	65	74
	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g
Co-60	0.0359 XYZ	0.0038 XYZ	0.0167 XYZ	0.0068 XYZ	0.0311 XYZ	0.05 XYZ	0.0092 XYZ	0.0277 XYZ	0.0593 XYZ	0.0409 XYZ	0.0482 XYZ	0.0704 XYZ
Cs-137	0.107 XYZ	0.102 XYZ	0.0861 XYZ	0.102 XYZ	0.117 XYZ	0.0791 XYZ	0.138 XYZ	0.0919 XYZ	0.0939 XYZ	0,101 XYZ	0.133 XYZ	0.0977 XYZ
Pb-212	0.858 XYZ	0.867 XYZ	0.843 XYZ	0.766 XYZ	0.806 XYZ	0.908 XYZ	0.703 XYZ	0.838 XYZ	1.5 XYZ	1.75 XYZ	1.22 XYZ	1.45 XYZ
Pb-214	0.494 XYZ	0.389 XYZ	0.328 XYZ	0.37 XYZ	0.407 XYZ	0.428 XYZ	0.395 XYZ	0.397 XYZ	0.4 XYZ	0.513 XYZ	0.426 XYZ	0.352 XYZ
Ra-224	0.341 XYZ	0.385 XYZ	0.394 XYZ	0.32 XYZ	0.539 XYZ	0.415 XYZ	0.254 XYZ	0.854 XYZ	1.53 XYZ	1.78 XYZ	1.24 XYZ	1.47 XYZ
Ra-226	0.872 XYZ	0.881 XYZ	0.857 XYZ	0.778 XYZ	0.82 XYZ	0.923 QXYZ	0.715 XYZ	0.329 QXYZ	0.202 XYZ	0.441 XYZ	0.46 XYZ	0.486 XYZ
Ru-106	o xyz	0 XYZ	0.0438 XYZ	0 XYZ	0 XYZ	-0 XYZ	0 XYZ	0.232 XYZ	0 XYZ	0 XYZ	0 XYZ	0.354 XYZ
Sb-125	0.0529 XYZ	0.001 XYZ	0 XYZ	0.0268 XYZ	o xyz	o xyz	0 XYZ	o xyz	0 XYZ	0.0521 XYZ	0.113 XYZ	0.0554 XYZ
	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g
U-Nat	403	144	809	593	564	516 Q	362	384 Q	1100	614	848	1460

U=Analyzed for but undetected Q=Data can be used qualitatively L=Less than CRDL and above MDL XYZ=Matrix interference encountered

		TEC.	T #1 9011 UAS	SHING RESULTS		1,	
				WATER (UNFILTE	RED)		
			JUNE	1993 PROCESSI	1G		
	B07C75	в07с76	B07C77	B07C85	в07с79	во7с80	B07C81
	water mg/L	water mg/L	water mg/L	water mg/L	water mg/L	water mg/L	water mg/L
Ag	0.05	1	0.53	0.98	0.64	0.3	0.18
AL	37	850	550	770	1000	480	250
As	0.003 L	0.024	0.028	0.026	0.023	0.022	0.011
Ва	2.1	67 Q	43	60 Q	120	59	27
Be	0.0013 L	0.019	0.011	0.018	0.018	0.0082	0.0042
Ca	19	400	170	400	350	170	100
Cd	U	0.011	U	0.0091 L	υ	ŭ	U
Со	0.0071 L	0.095	0.14	0.092	0.27	0,13	0.066
Cr	0.38	9.2	5.5	8.6	9.5	4.6	2.6
Cu	3.5	100	50	98	60	29	25
Fe	13	230	160	220	270	130	63
Нд	0.0045	0.13	0.078	0.14	0.12	0.096	0.049
K	3.5	34	24	33	37	18	9.2
Mg	10	190	120	170	210	100	59
Mn	0.27	5.3	3.7	4.9	6	2.9	1.6
Na	31	120	110	120	170	96	66
Ni .	0.32	10	5	9.6	5.3	2.7	2
Pb ·	0.093	2.6	1.1	2.1	2.1	0.98	0.55
Sb	U	U	U	U	U	U	Ų
Sn	0.061 L	1	0.68	0.89	1.3	0.67	0.38
٧	0.0089 L	0.36	0.22	0.36	0.4	0.19	0.097
Zn ,	0.11	2.6	1.7	2.4	3	1.5	0.89
	piC/L	pCi/L	pCi/L	pCi/L	pCi/L	pCi/L	pCi/L
Co-60	0	2.19	11,9 XYZ	0.877	0 XYZ	18.6 XYZ	0 XYZ
Cs-137	1.32	0.0867	9.56 XYZ	5.47	4.86 XYZ	7.43 XYZ	25.1 XYZ
Pb-212							
Pb-214							
Ra-224							
Ra-226							
Ru-106	23.3	47.9	0 XYZ	0	0 XYZ	80.8 XYZ	0 XYZ
Sb-125	0	0	42.3 XYZ	0	27.7 XYZ	0 XYZ	30.2 XYZ
	ug/L	ug/L	ug/L	ug/L	ug/L	ug/L	ug/L
U-Nat	10200	24800	58000	30600	93700	38500	23400

U=Analyzed for but undetected

L=Less than CRDL and above MDL Q=Data can be used qualitatively XYZ=Matrix interference encountered

			ST #1 SOIL WA INUS 0.425mm	SHING RESULTS SLURRY SOILS			
			JUNE	1993 PROCESSI	NG		
	B07C91 soil mg/kg	B07C92 soil mg/kg	807C93 soil mg/kg	B07C95 soil mg/kg	B07C96 soil mg/kg	B07C97 soil mg/kg	B07CB1 soil mg/kg
Ag	2.1	1.5 L	1.1 L	2.2	1.5 L	2.8	1.9 L
Αl	7600	7800	7100	8900	10000	9900 Q	6900 Q
As	1.3	1.2	1.2	2.2	1.1	1.7 Q	1 Q
Ba	220	200	190	310	380	390 Q	300 Q
8e	0.24 L	0.23 L	0.18 L	0.1 L	0.22 L	0.2 L	0.21 L
Ca	3900	4000	3800	5 <u>100</u>	5000	5400 Q	4100 Q
Cd	U	U	U	u	u <sub>.</sub>	U	U
Co	3.6	4.6	4.9	6	4.7	5.3	5
Cr	34	30	28	45	44	53 Q	40 Q
Cu	320	240	150	420	420	500 <u></u>	260 Q
Fe	12000	13000	15000	19000	14000	15000	14000
Hg	0.3 L	0.2 L	0.35 L	0.49	0.3 L	0.48	0.54
K	670	750_	730	800	810	790	650
Mg	3100	3100	3300	3800	3700	3700	3200_
Mn	160	180	200	220	180	180	170
Na	540	650	650	710	890	900 q	620 Q
Ní	34	27	22	40	30	47 Q	29 Q
Pb	13	13	11	16	15	24 Q	17 Q
Sb	U	U	4.4 L	U	U	4.5 L	U
Sn	U	6 L	U	U	6.1 L	U	U
v	37	38	48	61	42	45	39
Zn	35	36	37	44	42	44	39
	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g
Co-60	0 XYZ	0 XYZ	0 XYZ	0 XYZ	0.0091 XYZ	0.0074 XYZ	0.0077 XYZ
Cs-137	0.152 XYZ	0.118 XYZ	0.138 XYZ	0.174 XYZ	0.279 XYZ	0.303 XYZ	0.224 XYZ
Pb-212	0.596 XYZ	0.604 XYZ	0.834 XYZ	0.828 XYZ	0.724 XYZ	0.821 XYZ	0.917 XYZ
Pb-214	0.511 XYZ	0.403 XYZ	0.556 XYZ	0.424 XYZ	0.518 XYZ	0.478 XYZ	0.619 XYZ
Ra-224	0.608 XYZ	0.616 XYZ	0.85 XYZ	0.84 XYZ	0.734 XYZ	0.832 XYZ	0.55 XYZ
Ra-226	0.461 XYZ	0.459 XYZ	0.534 XYZ	0.448 XYZ	0.458 XYZ	0.509 XYZ	0.929 XYZ
Ru-106	0.0369 XYZ	0.209 XYZ	0.0328 XYZ	0.0307 XYZ	0 XYZ	0.446 XYZ	0.0867 XYZ
Sb-125	0.0251 XYZ	0.0062 XYZ	0.0726 XYZ	0.0429 XYZ	0.0428 XYZ	O XYZ	0 XYZ
	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g
U-Nat	217	214	158	173	358	355 Q	827Q

U=Analyzed for but undetected Q=Data can be used qualitatively U=Less than CRDL and above MDL XYZ=Matrix interference encountered

DOE/RL-93-96, Rev. 0

				TEST #1	SOIL WAS	HING RES	ULTS					
		RESH WA	TER (UNF	ILTERED)	· · · · · · · · · · · · · · · · · · ·	MINUS 0.425mm SLURRY WATER (UNFILTERED)						
		JUNE 19	993 PROC	ESSING				JUNE 1	993 PROC	ESSING		
	B07C70 water mg/L	B07C71 water mg/L	B07C72 water mg/L	B07C73 trp bik mg/L	807C74 trp blk mg/L	B07C75 water mg/L	B07C76 water mg/L	B07C77 water mg/L	B07C85 water mg/L	B07C79 water mg/L	807C80 water mg/L	B07C81 water mg/L
Chloroform	0.05	0.02 QH	0.02 Q	U	U	0.01	0.01	0.01 H	0.01	0.0029 H	0.0044 H	0.0064 H
Methyl Ethyl Ketone	U	UH	υ	U	U	0.07	U	0.05 H	U	0.18 H	0.03 H	0.02 H
Tetrachloroethylene	U	UH	U	U	υ	0.001	0.0013	0.001B H	0.0016	0.0023 H	0.0025 H	0.0038 ਮ
Tetrahydrofuran	U	UH	υ	U	υ	U	U	UН	U	0.08 H	UН	UH
Trichloroethylene	U	UH	υ	υ	U	0.0034	0.0054	0.006 <b>4</b> H	0.0067	0.0077 H	0.0097 H	0.01 H
1,2-Dichloroethane, d4	0.05	0. <b>04</b> H	0.05	0.05	0.06	0.05	0.06	0.05 H	0.06	0.04 H	0.04 H	0.05 H
Toluene, d8	0.05	0.05 н	0.05	0.05	0.05	0.05	0.05	0.05 H	0.05	0.05 H	0.05 H	0.05 H
4-BromoFluorobenzene	0.05	0.05 H	0.05	0.05	0.05	0.05	0.05	0.05 H	0.05	0.05 H	0.05 H	0.05 H

U=Analyzed for but undetected

Q=Data can be used qualitatively

H=Holding time missed

THA Inc.

instrument ID: 4500

REPORT

Work Order # A3-06-092

eived: 06/30/93

Results by Sample

PLE ID BOSMHO

FRACTION 01A TEST CODE TOV1 NAME TOLP Volatiles form 1 Date & Time Collected 06/24/93 \_\_\_\_\_ Category \_\_\_\_\_

#### TCLP VOLATILE ORGANICS

Lab File ID: 30712R05

analyzed (mL): 1.0 TCLP Extraction Date: 07/09/93

Date Received: 06/30/93 Date Leachate Extracted:
Date Analyzed: 07/12/93 Dilution Factor: Sample Matrix (soil/water): WATER\_ Leachate vol analyzed (mi): 1.0

CAS No.	COMPOUND	RESULT (mg/L)	PQL (mg/L)
71-43-2	Benzene	סא	0.025
56-23-5	Carbon Tetrachloride	ИО	0.025
108-90-7	"Chlorobenzene	нΩ	0.025
67-66-3	Chloroform	0.014	0.025
107-06-2	1,2-Dichloroethane	ИО	0.025
75-35-4	1,1-Dichloroethylene	ΝО	0.025
78-93-3	Methyl Ethyl Ketone	NO	0.05
127-18-4	Tetrachloroethylene	МО	0.025
79-01-6	Trichloroethylene	סא	0.025
75-01-4	Vinyl Chloride	NO	0.05

#### % RECOVERY SURROGATE COMPOUND

d8-Toluene 107

Bromofluorobenzene 106

1,2-Dichloroethane-d4 107

FORM I

1 . . .

THA Inc.

REPORT

Work Order # A3-06-092

Results by Sample

LE 10 808KL6

eived: 06/30/93

PRACTION <u>OZA</u> TEST CODE <u>TCV1</u> NAME <u>TCLP Volatiles form 1</u>

Date & Time Collected <u>06/24/93</u> Category

TCLP VOLATILE ORGANICS

Sample Matrix (soil/water): WATER
Leachare vol analyzed (mL): 1.0

Lab file ID: 30709R05
TCLP Extraction Date: 07/08/93

Date Received: 06/30/93

1 . .

TCLP Extraction Date: 07/08/93

Date Leachate Extracted:

Date Analyzed: 07/09/93 '.
Instrument ID: 4500

Dilution factor: 5.0

CAS No.	COMPOUND	RESULT (mg/l)	PQL (mg/L)
71-43-2	Benzene	ДК	0.025
56-23-5	Carbon Tetrachloride	OH	0.025
108-90-7	"Chlorobenzene	нр	0.025
67-66-3	Chloroform	0.006	0.025
107-06-2	1,2-Dichloroethane	ND	0.025
75-35-4	1,1-Dichloroethylene	סא	0.025
78-93-3	Hethyl Ethyl Ketone	סא	0.05
127-18-4	Tetrachloroethylene	NO	0.025
79-01-6	- Trichloroethylene	ND	0.025
75-01-4	Vinyl Chloride	ND	0.05

% RECOVERY SURROGATE COMPOUND

d8-Toluene 98

Bromofluorobenzene \_\_\_\_\_105

1,2-Dichloroethane-d4 106

FORM T

Results by Sample

eived: 06/30/93 PLE 10 808MNO

FRACTION <u>01C</u> TEST CODE <u>TCS1</u>
Date & Time Collected <u>06/24/93</u> TEST CODE TCS1 NAME TCLP Semi-Volatiles form 1 \_\_\_\_\_Category \_\_\_\_

#### TCLP SEMI-VOLATILE ORGANICS

Sample Matrix: WATER Leachate vol (ml): 100 Date Received: 06/30/93 Conc. Extract Vol.(mL): 2 Injection Volume (uL): 1

Instrument ID: SHERMA

1

Lab File ID: 30720\$16 TCLP Extraction Date: 07/07/93 Date Leachate Extracted: 07/08/93 Date Analyzed: 07/20/93

Dilution ractor:

CAS No.	COMPOUND	RESULT (mg/L)	PQL (mg/L)
1319-77-3	Cresol (Total)	нр	0.1
87-86-5	Pentachlorophenol	ИD	0.5
95-95-4	2,4,5-Trichlorophenol	ND	0.1
88-06-2	2,4,6-Trichlorophenol	ΝО	0.1
106-46-7	1,4-Dichlorobenzene	סא	0.1
121-14-2	2,4-Dinitrotoluene	ОИ	0.1
118-74-1	Hexachiorobenzene	ОИ	0.1
87-68-3	Hexachlorobutadiene	סא	0.1
67-72-1	Hexachloroethane	ИD	0.1
98-95-3	Witrobenzene	ИО	0.1
110-86-1	Pyridine	מא	0.2

% RECOVERY SURROGATE COMPOUND

2-fluorophenol Phenol-d5 2,4,6-Tribromophenol 95 Nitrobenzene-d5 2-fluorobiphenyl 84 Terphenyl-d14

FORM [

THA Inc.

REPORT Results by Sample

Work Order # A3-06-092

eceived: 06/30/93 AMPLE ID BOSNLO

FRACTION 02B TEST CODE TCST NAME TCLP Semi-Volatiles Form 1 Date & Time Collected 06/24/93

Category \_\_\_\_

## TCLP SEMI-VOLATILE ORGANICS

Sample Matrix: WATER Leachate vol (mL): 100 Date Received: 06/30/93

Conc. Extract Vol.(mL): 2 Injection Volume (uL): 1

Instrument ID: SHERMA

1

Lab File ID: <u>30720\$20</u> TCLP Extraction Date: <u>07/08/93</u> Date Leachate Extracted: 07/08/93

Date Analyzed: 07/20/93 Dilution factor:

CAS NO.	COMPOUND	RESULT (mg/L)	PQL (mg/L)
1319-77-3	Cresol (Total)	ОИ	0.1
87-26-5	Pentachlorophenol	ND	0.5
95-95-4	2,4,5-Trichlorophenol	ИО	0.1
88-06-2	2,4,6-Trichlorophenol	ди	0.1
106-46-7	1,4-Dichlorobenzene	ИО	0.1
121-14-2	2,4-Dinitrotoluene	סא	0.1
118-74-1	<b>Rexachlorobenzene</b>	Ои	0.1
87-68-3	Hexachlorobutadiene	ND	0.1
67-72-1	Hexachlorgethane	N D	0.1
98-95-3	Nîtrobenzene	ND	0.1
110-86-1	Pyridine	NO	0.2

% RECOVERY SURROGATE COMPOUND

2-fluorophenol 87 Phenol-d5 2,4,6-Tribromophenol 80 100 Nitrobenzene-d5 2-fluorobiphenyl 94 98 Terphenyl-d14

:eived: 06/30/93

TMA Inc. Results by Sample REPORT

Work Order # A3-06-092

IPLE 10 808ML6

FRACTION 028 TEST CODE TCP1 HAME TCLP Pesticides Form 1
Date & Time Collected 06/24/93 Category

TCLP CHLORINATED PESTICIDES

Sample Matrix: WATER

Conc. Extract Vol.(mL): 10 Injection Volume (uL):: 1 Column ID: <u>D8-17</u>

Leachate vol (mL): 100 0 ate Received: 06/30/93

Lab File ID: AG12028

TCLP Extraction Date: 07/08/93
Date Leachate Extracted: 07/08/93
Date Analyzed: 07/13/93

Dilution Factor:

CAS No.	СОМРОИНО	RESULT (mg/L)	PQL (mg/L)
57-74-9	Chlordane	ND	0.005
72-20-8	Endrin	N D	0.001
76-44-8	Heptachlor	ДИ	0.0005
1024-57-3	Heptachlor Epoxide	ND	0.0005
58-89-9	Lindane	СИ	0.0005
72-43-5	Methoxychlor	ND	0.005
8001-35-2	Toxaphene	ИD	0.020

% RECOVERY SURROGATE COMPOUND

TCX 83

DCB 77

FORM I

B.1-16

BB 102 36

eived: 06/30/93

TMA Inc.

REPORT

PLE ID BOSKNO

Results by Sample

FRACTION <u>01C</u> TEST CODE <u>TCP1</u> NAME <u>TCLP Pesticides Form 1</u>
Date & Time Collected <u>06/24/93</u> Category \_\_\_\_\_

Category \_

#### TCLP CHLORINATED PESTICIDES

Sample Matrix: WATER Leachate vol (mt): 100

Date Received: 06/30/93

Conc. Extract Vol.(mt): 10 Injection Volume (uL): 1 Column ID: 08-17

Lab File ID: AG12025 TCLP Extraction Date: 07/07/93 Date Leachate Extracted: 07/08/93
Date Analyzed: 07/12/93 Dilution factor:

CAS NO.	COMPOUND	RESULT (mg/L)	PQL (mg/L)
57-74-9	Chlordane	ND	0.005
72-20-8	Endrin	NO	0001
76-44-8	Heptachlor	ИВ	0.0005
1024-57-3	Heptachlor Epoxide	סא	0.0005
58-89-9	Lindane	ND	0.0005
72-43-5	Hethoxychlor	NO	0.005
8001-35-2	Toxaphene	ND	0.020

#### % RECOVERY SURROGATE COMPOUND

1 CX

DCB

FORM I

B.1-17

000369

TMA Inc.
Results by Sample KEPORT

Work Order # A3-06-092

:ceived: 06/30/93

MPLE ID BOSMNO

FRACTION <u>01C</u> TEST CODE <u>TCH1</u>
Date & Time Collected <u>06/24/93</u>

TEST CODE TOHT NAME TOLP Herbicides Form 1

#### TOLP CHIORINATED HERBICIDES

Sample Matrix (soil/water): WATER

Lab File ID: AG12012

Leachate vol (mL): 100

TCLP Extraction Date: 07/07/93

Date Received: 06/30/93

Date Leachate Extracted: 07/09/93

Conc.Extract Vol.(mL): 5

Date Analyzed: 07/13/93

Injection Volume (uL): 1

Dilution Factor: \_\_\_\_\_5

Column ID: <u>D8-608</u>

CAS No.	COMPOUND	RESULT (mg/L)	PQL (mg/L)
94-75-7	2,4-D	ďУ	0.010
93-72-1	2,4,5-TP	ND	0.0010

% RECOVERY SURROGATE COMPOUND

DCAA 93

FORM I

B.1-18

980 JUZI 166

TMA Inc. REPORT Work Order # A3-06-092

Received: 06/30/93

SAMPLE 10 BOSNES\_\_\_\_

Results by Sample

FRACTION <u>OZB</u> TEST CODE <u>YCH1</u> NAME <u>TCLP Kerbicides Form 1</u>
Date & Time Collected <u>06/24/93</u> Category

## TCLP CHLORINATED HERBICIDES

Sample Matrix (soil/water): WATER\_\_\_\_

Lab File ID: AG12015

Leachate vol (mL): 100

TCLP Extraction Date: 07/08/93

Date Received: 06/30/93

Date Leachate Extracted: 07/09/93

Conc.Extract Vol.(mt): 5\_\_\_\_\_

Date Analyzed: 07/13/93

Injection Volume (uL): 1

Dilution Factor: \_\_\_\_\_5

Column ID: <u>DB-608</u>

CAS No.	COMPOUND	RESULT (mg/L)	POL (mg/L)
94-75-7	2,4-p	ND	0.010
93-72-1	2,4,5-TP	ND	0.0010

% RECOVERY SURROGATE COMPOUND

DCAA 105

THA Inc.

REPORT

eceived: 06/30/93

ARPLE ID BOSMNO

Results by Sample

FRACTION OIC TEST CODE TON1 NAME TOLP Metals Form 1 Date & Time Collected 06/24/93

TCLP METALS

Sample Hatrix: WATER

TCLP Extraction Date: 08/23/93

Date Received: 06/30/93

CAS No.	COMPOUND	RESULT (mg/L)	PQL (mg/L)	METHOD
7440-38-2	Arsenic	0.006	0.001	F
7440-39-3	Barium	3.49	0.001	P
7440-43-9	Cadmium	ИΩ	0.007	P
7440-47-3	Chromium	0.078	0.006	P
7439-92-1	Lead	0.017	0.001	F
7439-97-6	Hercury	0.0012	0.0002	cv
7782-49-2	Selenium	0.011	0.002	F
7440-22-4	Silver	0.005	0.003	Р

Analytical Methods Used:

P = 1CP A ⇒ Flame ÁA

CV = Cold Vapor AA

THA Inc.

REPORT

000489

deived: 06/30/93

Results by Sample

MPLE ID BOSNES

FRACTION 028 TEST CODE TOM1 NAME TOLP Metals FORM 1 Date & Time Collected 06/24/93 Category \_\_\_\_

#### TCLP METALS

Sample Matrix: WATER

TCLP Extraction Date: 07/08/93\_\_\_

Date Received: 06/30/93

CAS No.	COMPOUND	RESULT (mg/L)	PQL (mg/L)	HET HOD
7440-38-2	Arsenic	0.001	0.001	F
7440-39-3	Barium	0.567	0.001	P
7440-43-9	Cadmium	0.001	0.003	Р
7440-47-3	. Chromium	0.107	0.007	ρ
7439-92-1	Lead	0.008	0.001	F
7439-97-6	Hercury	0.0024	0.0002	cv
7782-49-2	Selenium	N D	0.002	F
7440-22-4	Silver	0.078	0.004	P

Analytical Methods Used:

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P = 1CP A = Flame AA F = Furnace AA

CV = Cold Vapto AA

From:

Geochemistry & Hydrochemistry

Phone:

376-3324

Date:

December 3, 1993

Subject: DATA VALIDATION OF 300-FF-1 SOIL WASHING COLLECTED JUNE 1993

To:

R. D. Belden

cc: J. C. Johnston

D. G. Horton

This report is to document the validation of 300-FF-1 Soil Washing data collected during JUNE 1993. The validation was based on WHC-CM-7-8 manual "Environmental Engineering and Geotechnology Function Procedures" (WHC 1992) and the "Annual Report for RCRA Groundwater Monitoring Projects at Hanford Site Facilities for 1992" Appendix B DOE/RL-93-09 (DOE-RL, 1993a).

The data were collected, analyzed and processed in a similar manner as the Resource Conservation and Recovery Act (RCRA) groundwater monitoring projects. The analytical laboratories utilized were Datachem Laboratory, Salt Lake City Utah and International Technology Analytical Services, Richland, Washington. Data validation was performed by Ms. P.B. Freeman, RCRA Sampling and Analysis Task Leader. A electronic copy of the data is provide in both paradox and lotus format. Hardcopies of data were provided prior to this report.

Data validation consisted of seven parts:

- a. 100% verification that requested data were received.
- b. 100% verification that holding times were meet.
- c. 100% evaluation of precision with field duplicates
- d. 100% evaluation of potential sample contamination with field blank data.
- e. 100% evaluation of laboratory MS/MSD and surrogate data through laboratory incident reports.
- f. 100% evaluation of laboratory blanks.
- g. 100% evaluation of data completeness.

The outcome of the validation:

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Part a: All data requested were not received. Sample numbers B07C86 and B07C87 were not received. These were for VOA analyses only as they were Trip blank # 3 and Trip blank # 4, respectfully.

Part b: All analytical holding times were not met. VOA analyses for the following samples numbers exceeded required holding times. These data have been flagged with "H" validation flag. The H-flagged data can be used

qualitatively, but no regulatory decisions should be made based on a single flagged analytical result. The sample numbers are B07C77, B07C79, B07C80, B07C81, B07C82, B07CB3, B07C71.

Part c: Evaluation of Duplicate data was performed using procedure 2.1 "Evaluation of RCRA Groundwater Field Duplicate and Blank Sample Data" (WHC 1992) and using Appendix B (DOE-RL 1993).

There were two water matrix and three soil matrix duplicate pairs evaluated. The water matrix paired sample numbers are B07C71 with B07C72 and B07C76 with B07C85, respectfully. The evaluation identifies constituents which exceeded a required 25% relative percentage difference (WHC 1992) and was above the limit of detection as defined in Appendix B (D0E-RL 1993).

The evaluation of B07C71 and B07C72 identified one constituent. The constituent is chloroform which was analyzed by method SW-846 8240.

The evaluation of B07C76 and B07C85 identified one constituent. The constituent is barium which was analyzed by method SW-846 6010.

The soil matrix paired sample numbers are B07C31 with B07C68 B07C97 with B07CB1 and B07C11 with B07C67, respectfully. The evaluation of B07C31 and B07C68 identified four constituents. The constituents are tin which was analyzed by method SW-846 6010; Arsenic which was analyzed by method SW-846 7060; uranium and radium-224 which were analyzed by International Technology Analytical Services inhouse methods.

The evaluation of B07C97 and B07CB1 identified ten constituents. The constituents are aluminum, barium, calcium, chromium, copper, nickel, sodium which were analyzed by method SW-846 6010; lead which is analyzed by method SW-846 7421; arsenic which is analyzed by method SW-846 7060 and uranium which was analyzed by International Technology Analytical Services inhouse method.

The evaluation of B07C11 and B07C67 identified nine constituents. The constituents are antimony, barium, chromium, copper, tin which were analyzed by method SW-846 6010; and uranium, cesium-137, lead-212, radium-224 which were analyzed by International Technology Analytical Services inhouse methods.

As a result of this evaluation all data associated with these sample numbers and constituents are flagged with a validation flag of Q. The Q-flagged data can be used qualitatively, but not regulatory decisions should be made based on a single flagged data point.

Part d: Evaluation of field blank data was performed using procedure 2.1 "Evaluation of RCRA Groundwater Field Duplicate and Blank Sample Data" (WHC 1992) and using Appendix B (DOE-RL 1993).

There were six water blanks collected during the June 1993 sampling. Results from two blanks were not received (see part a). The blanks exceeding two times the method detection limit (MDL) were flagged with a Q (WHC 1992). MDL are defined in Appendix B (DOE-RL 1993). The sample numbers for the water blanks are BO7C73, BO7C74, BO7CB2, BO7CB3, BO7C86 and BO7C87. Only samples BO7CB2 and BO7CB3 had one constituent exceed two times the MDL. The constituent was the same for each sample number and was methylene chloride which is analyzed by method SW-846 8240.

As a result of this evaluation the above constituents associated with the collect and analyze dates of these sample numbers and constituents are flagged with a validation flag of Q. The Q-flagged data can be used qualitatively, but not regulatory decisions should be made based on a single flagged data point.

Part e: There were three laboratory incident reports for this data. One incident report consisted of a sample analyzed by wrong uranium in-house method and was reanalyzed properly and reported without comment code. The other two reports described matrix interference which caused higher detection limits and false results in the gamma scan analysis. The effected samples for the gamma scan are flagged with a XYZ in the comment code. All the incident reports are attached for information. Otherwise, no data was found to have matrix spike, matrix spike duplicate or surrogate samples exceeding laboratory acceptance criteria.

Part f: There were no "B" qualifiers associated with these data, therefore no laboratory blanks exceeded laboratory acceptance criteria.

Part g: The data completeness is determined after data validation is completed and is calculated by the number of unflagged divided by the total number of validated data expressed as a percentage. The RCRA using a 80% acceptance guidance. The total number of soil data are 1302 constituents and water data are 578 constituents. The total unflagged soil data are 1256 constituents and water data are 421 constituents. The calculated completeness for soil and water data are 96.5% and 73%, respectfully. The soil data is within acceptable completeness criteria. The water data is below acceptable completeness criteria and may need to be evaluated further for its regulatory uses.

### References:

- DOE-RL, 1993, Annual Report for RCRA Groundwater monitoring Projects at Hanford Site Facilities for 1992, DOE/RL-93-09, U.S. Department of Energy, Richland Operations Office, Richland, Washington.
- WHC, 1992, Environmental Engineering and Geotechnology Function Procedures, WHC-CM-78, vol. 4, Westinghouse Hanford Company, Richland, Washington.

P. B. Freeman RCRA Sampling and Analysis Task Team Leader pbf

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# B.2 ANALYTICAL DATA FOR TEST #2

	TEST #2	SOIL WASHING RES	ULTS, RAW FEED		
	1		MBER 1993 PROCES	SING	
	B07DP9	B07DQ0	B07DQ1	B07DQ2	B07DQ3
	soil ma/kg	soil mg/kg	soil mg/kg	soil mg/kg	soil mg/kg
Λ-	mg/kg 3.2	4.6	2.8	2.6	4.8
Ag	12000	14000	13000	10000	7600
Al .	150	130	130	98	88
Ba	0.33	0.28 L	0.45	0.41	0.17 L
Be	7800	7100	8300	9600	6600
Ca	υ , , , , ,	U	U	U	U
Cd	13	13	14	12	11
Co	22	26	17	17	17
Cr	250	380	160	160	240
Cu	33000	33000	35000	32000	30000
Fe	0.45	0.14 Ł	υ υ	0.16 L	0.12 L
Hg K	1500	1700	1500	1100	670
· <del></del>	6600	7200	6900	6000	5000
Mg	590	510	550	460	380
Mn	480	440	440	440	430
Na	30	31	24	23	36
Ni		7.4	5	3.9	5,1
Pb	7	· · · · · · · · · · · · · · · · · · ·	5.5 L	5.8 L	, U
Sb	5.8 L ປ	7 L	9.5 L	5,8 C	0
\$n	86	87	91	89	88
<u>v</u>	73	77	. 72	68	63
Zn					
	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g
Co-60	0.0237 U	0.117	0.0496	0.079	0.31
Cs-137	0.0641	0.0905	0.0316	0.0529 U	0.0723
Pb-212	0.608	0.589	. 0.531	0.535	0.69
Pb-214	0.467	0.506	0.479	0.428	0.496
Ra-224	0.612	0.593	0.535	0.537	0.693
Ra-226	0.455	0.516	0.39	0.344	0.496
Ru-106	-0.0969 U	0.194	0.00646 U	-0.118 U	-0.118 U
Sb-125	0.0481	0.00982 U	0.0314 U	-0.00754U	-0.0375U
	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g
U-Nat	3.65	13.3	1.72	2.73	6.13
	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg
Aroclor-1016	U	U	U_	U	U
Araclor-1221	U	υ	U	U	U
Aroclor-1232	U	υ	U	U	U
Aroclor-1242	U	U	U	U	U
Arocior-1248	0.064 L	0.091 L	0.0089 L	0.012 L	0.12
Aroclor-1254	U	υ	U	U	U
Araciar-1260	U	U	U	U	U

U=Analyzed for but undetected Q=Data can be used qualitatively

L=Less than CRDL and above MDL

TEST #2 SOIL WASHING RESULTS FRESH WATER (UNFILTERED)						
	SEPTEMBER 1993 PROCESSING					
	B07DQ4 water mg/L	BO7DXB dup. mg/L	B07DQ5 water mg/L	B07DX9 dup. mg/L		
Ag	υū	0.005 LQ	υα	0.0047 LQ		
Al	υ	U	Ü	U		
8a	0.039 Q	0.03 Q	0.028	0.027		
Be	U	C	U	U		
Са	38 Q	27 Q	24	24		
Cd	O	U	٦	Ü		
Со	U	υ	v	٥		
Cr	υ	0.0062 L	כ	Ü		
Cu	0.078 Q	0.038 Q	0.0054 LQ	υα		
Fe	1.6	1.3	0,12	0.13		
Hg	د	د	Ū	U		
К	3 0	2.1 Q	1.6 Q	2.1 Q		
Mg	8.9 Q	6.2 Q	5.3	5.4		
Mn	0.067 Q	0.032 Q	0.0063 L	0.006 <b>9</b> L		
Na	9.5 Q	5.3 Q	4.3	4.1		
Ni	U	U	Ų	U		
Pb	0.037 Q	0.01 Q	0.00097 L	0.0016 L		
Sb	C	U	U	υ		
Sn	υ	U	U	U		
V	Ü	U	0.0053 L	U		
Zn	0.024 Q	0.012 Q	U	0.0045 L		
	pCi/L	pCi/L	pCi/L	pCi/L		
Co-60	0.146 U	5.25	1.29 ∪	4.55 U		
Cs-137	1.39 U	4.51 U	3,1 U	3.3 U		
Ru-106	-44.3 U	4.35 U	-32.3 U	-0.728 U		
Sb-125	5.77 U	-3.15 U	12.2 U	-15.3 U		
	ug/L	ug/L	ug/L	ug/L		
U-Nat	1.63 Q	0.693 Q	0.805	0.702		
	mg/L	mg/L	mg/L	mg/L		
Aroclar-1016	U	U	U	Ú		
Aroclor-1221	U	U	U	U		
Arociar-1232	U	U	U	U		
Aroclor-1242	U	U	υ	U		
Aroclor-1248	U	U	U	U		
Aroclor-1254	U	U	U	U		
Aracior-1260	U	U	U	U		

U=Analyzed for but undetected L=Less than CRDL and above MDL Q=Data can be used qualitatively

	··········			IES	T #2 SOI	IL WASHI	NG RESU	LTS		<del></del>		
					25	mm 10 2	mm					
1			5675144	22215			993 PRO		0070140	D07DW4	0070440	0070440
ľ	B07DV2 soil	B07DV3 soil	BO/DV4 soil	B07DV5 soil	B07DV6 soil	B07DV7 soil	soil	B07DV9 soil	B07DW0 soil	B07DW1 soil	B07DW2 soil	B07DW3 soil
	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg
Ag	1.2 L	1 L	0.73 L	1.1 L	0.84 L	0.96 L	0.67 L	0.86 L	1.1 L	0.95 L	0.76 L	0.78 L
Al	4900	5700	4200	5400	3900	5400	4000	3500	4100	3400	3100	3900
Ва	67	45	61	80	81	73	85	69	71	69	59	80
8e	0.29 L	0.22 L	0.13 L	0.3 L	0.13 L	0.31	0.2 L	0.23 L	0.25 L	0.23 L	0.13 L	0.19 L
Ca	5500	5800	4400	6500	5100	7000	5600	4900	5600	4900	5500	4600
Cd	U	υ	۲	υ	U	U	Ų	U	U	U	U	υ
Со	9.4	8.7	7.8	11	8,6	10	8.9	8.9	11	8.8	7.7	8.1
Cr	6.3	4.3	3.2	4.5	3.9	4.8	2.7	3.3	4.7	6	2.1	4.3
Cu	240	140	140	270	160	66	180	150	190	130	38	190
Fe	26000	24000	31000	22000	22000	26000	24000	23000	29000	25000	22000	21000
Hg	U	υ	υ	U	U	U	U	υ	υ	υ	υ	U
κ	440	260	350	270	230	350	280	240	290	360	260	380
Mg	3700	3200	2900	3700	3000	3900	3600	3400	4700	2500	3100	4200
Мп	290	260	220	340	240	270	310	250	340	290	210	180
Na	280	370	240	450	310	500	330	320	310	320	220	290
Ni	15	8.5	7.7	13	7.5	7	.12	10	12	6.8	4.1	6.7
Pb	2	2.4	2.1	2.8	1.1	1.8	1.9	1.6	1.8	2.3	1.7	1.6
Sb	υ	6.1 L	5.3 L	J.	4.6 L	U	U	U	4.4 L	U	υ	U
Sn	U	U	٥	Ü	U	U	U	υ	υ	U	υ	U
V	78	64	62	71	62	69	41	67	73	76	58	46
Żn	53	53	54	64	51	56	49	48	53	48	45	42
	pCi/g	pCl/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g
Co-60	0.129	0.155	0.125	0.133	0.034	0.0906	0.168	0.08	0.0947	0.0643	0.12	0.0793
Cs-137	0.121	0.124	0.116	0.196	0.0587	0.101	0.167	0.113	0.0863	0.115	0.112	0.105
Pb-212	0.576	0.523	0.463	0.48	0.526	0.493	0.604	0.741	0.536	0.627	0.686	0.563
Pb-214	0.451	0.5	0.39	0.47	0.484	0.431	0.509	0.632	0.494	0.6	0,609	0.502
Ra-224	0.579	0.526	0.466	0.483	0.529	0.495	0.607	0.745	0.54	0.632	0.691	0.567
Ra-226	0.509	0.484	0.371	0.38	0.373	0.448	0.678	0.592	0.452	0.601	0.549	0.449
	-0.075U	0.0320	-0.036U	-0.008U	-0.07 <b>6</b> U	0.1 U	-0.033U	-0.032U	-0.0844U	-0.0281U	-0.007U	-0.043U
Sb-125	-0.001U	-0.006U		-0.044U		-0.001U	0.09	-0.000U	0.0121U	0.0452U	-0.015U	0.003 U
	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g
U-Nat	2.01	1.37	1.33	2.02	0.912	1.53	2.13	0.857	1.23	1.07	1.32	1.4
	mg/kg	mg/kg	rng/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg
Aroclor-1016	Ų	U	U	U	U	U	U	U	U	U	U	U
Aroclar-1221	U	U	U	U	U	U	υ	U	U	U	U	U
Aroclor-1232	U	U	υ	U	U	U	υ	U	U	U	U	U
Aroclor-1242	U	U	U	U	U	U	U	U	U	U	U	U
Aroclor-1248	.0047 L	.0087L	.0039 L	.029 L	.0041 L	.0052 L	.0047 L	.0049 L	.0024 L	.0033 L	.0048 L	.0084 L
Aroclor-1254	Ü	U	U	U	U	U	U	U	U	U	U	υ
Aroclor-1260	U	U	U	U	U	U	U	U	U	U	U	U
			L				<u> </u>	<u>`</u>		1	<u> </u>	<u> </u>

U=Analyzed for but undetected

L=Less than CRDL and above MDL

Mg Ag Ag Ag Al Ba Ba 1 Ba 0. Ca 76 Cd Co Cd Cd Co Cd Cd Co Cd	soii ig/kg 3.9 400 120 0.49 600 U 15 20 630	B07DW5 soil mg/kg 3.3 7000 97 0.23 L 6300 U 11 16 520 33000 0.13 L 560 5200 400 400 26 2.9 U 94 74	B07DW6 soil mg/kg 4.4 8000 89 0.45 7600 U 12 21 720 34000 0.14 L 540 5600 400 500 33 4.9 U U 96	B07DW7 soil mg/kg 7.1 7600 88 0.51 7200 U 12 22 910 34000 U 630 5300 380 510 31 4.9 4.9 L U 100	BO7DW8 soil mg/kg 3.5 7200 91 0.26 L 6600 U 12 23 620 33000 0.32 L 560 6500 440 440 41 4.9 U 92	BO7DW9 soil mg/kg 3.8 8200 120 0.48 7600 U 12 22 620 35000 0.3 L 600 5400 410 440 37 4.8 U U 110	93 PROCESS BO7DXO soil mg/kg 4.1 8900 91 0.38 8500 U 12 18 700 35000 0.17 L 590 5300 410 770 31 5.4 6.5 L	BO7DX1 soil mg/kg 3.6 7200 86 0.23 L 7000 U 11 22 550 33000 0.12 L 550 6200 380 500 37 5 4.5 L	B07DX2 soil mg/kg 2.9 6800 85 0.22 L 6300 U 10 13 450 32000 0.28 L 500 5200 360 370 24 4.6 U U U	B07DX3 soil mg/kg 5.5 7100 83 0.3 6700 U 11 21 1100 33000 0.48 590 5300 370 370 36 6.1 5.8 L	BO7DX4 soil mg/kg 3.6 6800 79 0.22 L 6200 U 11 16 600 33000 0.16 L 500 5000 380 380 25 5.5 5.3 L U	B07DX5 soil mg/kg 2.3 7600 88 0.39 7400 U 12 11 310 34000 0.25 L 510 5500 390 540 4.3 U U
Mg Ag Ag Al Ba Al	soii g/kg 3.9 400 120 0.49 600 U 15 20 630 000 550 520 32 5.9 U U 110 81	soil mg/kg 3.3 7000 97 0.23 L 6300 U 11 16 520 33000 0.13 L 560 5200 400 400 26 2.9 U U 94 74	soil mg/kg 4.4 8000 89 0.45 7600 U 12 21 720 34000 0.14 L 540 5600 400 500 33 4.9 U U 96	soil mg/kg 7.1 7600 88 0.51 7200 U 12 22 910 34000 U 630 5300 380 510 31 4.9 4.9 L U 100	soil mg/kg 3.5 7200 91 0.26 L 6600 U 12 23 620 33000 0.32 L 560 6500 440 440 41 4.9 U U	soil mg/kg 3.8 8200 120 0.48 7600 U 12 22 620 35000 0.3 L 600 5400 410 440 37 4.8 U	soil mg/kg 4.1 8900 91 0.38 8500 U 12 18 700 35000 0.17 L 590 5300 410 770 31 5.4	soil mg/kg 3.6 7200 86 0.23 L 7000 U 11 22 550 33000 0.12 L 550 6200 380 500 37 5	soil mg/kg 2.9 6800 85 0.22 L 6300 U 10 13 450 32000 0.28 L 500 360 370 24 4.6 U	soil mg/kg 5.5 7100 83 0.3 6700 U 11 21 1100 33000 0.48 590 5300 370 370 36 6.1 5.8 L	soil mg/kg 3.6 6800 79 0.22 L 6200 U 11 16 600 33000 0.16 L 500 5000 380 25 5.5	soi mg/kg 2.3 7600 88 0.39 7400 12 11 310 34000 0.25 510 5500 390 540 24
Aq 3 Al 844 Ba 1 Ba 0. Ca 76 Cd Co 6 Cd 76 Cd 77 Co 60 Co 77	3.9 400 120 0.49 600 U 15 20 630 000 27 L 700 900 550 520 32 5.9 U U 110 81	3.3 7000 97 0.23 t 6300 U 11 16 520 33000 0.13 t 560 5200 400 26 2.9 U U 94 74	4.4 8000 89 0.45 7600 U 12 21 720 34000 0.14 L 540 5600 400 500 33 4.9 U	7.1 7600 88 0.51 7200 U 12 22 910 34000 U 630 5300 380 510 31 4.9 U U	3.5 7200 91 0.26 L 6600 U 12 23 620 33000 0.32 L 560 6500 440 440 41 4.9 U	3.8 8200 120 0.48 7600 U 12 22 620 35000 0.3 L 600 5400 410 440 37 4.8 U	4.1 8900 91 0.38 8500 U 12 18 700 35000 0.17 L 590 5300 410 770 31 5.4	3.6 7200 86 0.23 L 7000 U 11 22 550 33000 0.12 L 550 6200 380 500 37 5	2.9 6800 85 0.22 L 6300 U 10 13 450 32000 0.28 L 500 5200 360 370 24 4.6	5.5 7100 83 0.3 6700 U 11 21 1100 33000 0.48 590 5300 370 370 36 6.1 5.8 L	3.6 6800 79 0.22 L 6200 U 11 16 600 33000 0.16 L 500 5000 380 380 25 5.5	2.3 7600 88 0.39 7400 (12 11 310 34000 0.25 510 5500 390 540 24
Al B4 Ba 1 Be 0. Ca 76 Cd 76 Cd 76 Cd 76 Cd 76 Cd 77 C	400 120 0.49 600 U 15 20 630 000 27 L 700 900 550 520 32 5.9 U U U 110 81	7000 97 0.23 L 6300 U 11 16 520 33000 0.13 L 560 5200 400 26 2.9 U 94 74	8000 89 0.45 7600 U 12 21 720 34000 0.14 L 540 5600 400 500 33 4.9 U	7600 88 0.51 7200 U 12 22 910 34000 U 630 5300 380 510 31 4.9 4.9 L	7200 91 0.26 L 6600 U 12 23 620 33000 0.32 L 560 6500 440 440 41 4.9 U	8200 120 0.48 7600 U 12 22 620 35000 0.3 L 600 5400 410 440 37 4.8 U	8900 91 0.38 8500 U 12 18 700 35000 0.17 L 590 5300 410 770 31 5.4 6.5 L	7200 86 0.23 L 7000 U 11 22 550 33000 0.12 L 550 6200 380 500 37 5	6800 85 0.22 L 6300 U 10 13 450 32000 0.28 L 500 5200 360 370 24 4.6	7100 83 0.3 6700 U 111 21 1100 33000 0.48 590 5300 370 370 35 6.1 5.8 L	6800 79 0.22 L 6200 U 11 16 600 33000 0.16 L 500 5000 380 380 25 5.5 5.3 L	7600 88 0.39 7400 (12 11 310 34000 0.25 510 5500 390 540 24 4.3
Ba 1 Be 0. Ca 76 Cd 76 Cd 76 Cd 76 Co 76 Co 77 C	120 0.49 600 U 15 20 630 000 27 L 700 900 550 520 32 5.9 U U 110 81	97 0.23 L 6300 U 11 16 520 33000 0.13 L 560 5200 400 26 2.9 U U 94 74	89 0.45 7600 U 12 21 720 34000 0.14 L 540 5600 400 500 33 4.9 U U	88 0.51 7200 U 12 22 910 34000 U 630 5300 380 510 31 4.9 U U	91 0.26 L 6600 U 12 23 620 33000 0.32 L 560 6500 440 41 4.9 U	120 0.48 7600 U 12 22 620 35000 0.3 L 600 5400 410 440 37 4.8 U	91 0.38 8500 U 12 18 700 35000 0.17 L 590 5300 410 770 31 5.4 6.5 L	86 0.23 L 7000 U 11 22 550 33000 0.12 L 550 6200 380 500 37 5 4.5 L	85 0.22 L 6300 U 10 13 450 32000 0.28 L 500 5200 360 370 24 4.6	83 0.3 6700 U 11 21 1100 33000 0.48 590 5300 370 370 36 6.1 5.8 L	79 0.22 L 6200 U 11 16 600 33000 0.16 L 500 5000 380 25 5.5	98 0.39 7400 ( 12 11 310 34000 0.25 510 5500 390 540 24
Be 0. Ca 76 Cd 76	0.49 600 U 15 20 630 000 27 L 700 900 550 520 32 5.9 U U 110 81	0.23 L 6300 U 11 16 520 33000 0.13 L 560 5200 400 400 26 2.9 U U	0.45 7600 U 12 21 720 34000 0.14 L 540 5600 400 500 33 4.9 U 96	0.51 7200 U 12 22 910 34000 U 630 5300 380 510 31 4.9 4.9 L U	0.26 L 6600 U 12 23 620 33000 0.32 L 560 6500 440 41 4.9 U	0.48 7600 U 12 22 620 35000 0.3 L 600 5400 410 440 37 4.8 U	0.38 8500 U 12 18 700 35000 0.17 L 590 5300 410 770 31 5.4 6.5 L	0.23 L 7000  U 11 22 550 33000 0.12 L 550 6200 380 500 37 5	0.22 L 6300 U 10 13 450 32000 0.28 L 500 5200 360 370 24 4.6	0.3 6700 U 11 21 1100 33000 0.48 590 5300 370 370 35 6.1	0.22 L 6200 U 11 16 600 33000 0.16 L 500 5000 380 380 25 5.5	0.39 7400 (12 11 310 34000 0.25 510 5500 390 540 24 4.3
Ca 76 Cd Cd Cc	600 U 15 20 630 000 27 L 700 900 550 32 5.9 U U 110 81	6300 U 11 16 520 33000 0.13 L 560 5200 400 26 2.9 U 94 74	7600  U  12  21  720  34000  0.14 L  540  5600  400  500  33  4.9  U  U  96	7200 U 12 22 910 34000 U 630 5300 380 510 31 4.9 4.9 L U 100	6600 U 12 23 620 33000 0.32 L 560 6500 440 440 41 4.9 U	7600 U 12 22 620 35000 0.3 L 600 5400 410 440 37 4.8 U	8500 U 12 18 700 35000 0.17 L 590 5300 410 770 31 5.4 6.5 L	7000 U 11 22 550 33000 0.12 L 550 6200 380 500 37 5 4.5 L	6300 U 10 13 450 32000 0.28 L 500 5200 360 370 24 4.6	6700 U 11 21 1100 33000 0.48 590 5300 370 370 36 6.1 5.8 L	6200 U 11 16 600 33000 0.16 L 500 5000 380 380 25 5.5	7400 12 11 310 34000 0.25 510 5500 390 540 24 4.3
Cod Co	U 15 20 630 000 27 L 700 900 550 520 32 5.9 U U 110 81	U 11 16 520 33000 0.13 L 560 5200 400 26 2.9 U 94 74	U 12 21 720 34000 0.14 L 540 5600 400 500 33 4.9 U 96	U 12 22 910 34000 U 630 5300 380 510 31 4.9 4.9 L	U 12 23 620 33000 0.32 L 560 6500 440 41 4.9 U	U 12 22 620 35000 0.3 L 600 5400 410 440 37 4.8 U	U 12 18 700 35000 0.17 L 590 5300 410 770 31 5.4	U 11 22 550 33000 0.12 L 550 6200 380 500 37 5	U 10 13 450 32000 0.28 L 500 5200 360 370 24 4.6	U 11 21 1100 33000 0.48 590 5300 370 370 35 6.1	U 11 16 600 33000 0.16 L 500 5000 380 380 25 5.5	12 11 310 34000 0.25 510 5500 390 540 24
Co 6 6 6 7 6 7 7 7 7 7 7 7 7 7 7 7 7 7 7	15 20 630 000 27 L 700 900 550 520 32 5.9 U U 110 81	11 16 520 33000 0.13 L 560 5200 400 26 2.9 U	12 21 720 34000 0.14 L 540 5600 400 500 33 4.9 U	12 22 910 34000 U 630 5300 380 510 31 4.9 U	12 23 620 33000 0.32 L 560 6500 440 41 4.9	12 22 620 35000 0.3 L 600 5400 410 440 37 4.8 U	12 18 700 35000 0.17 L 590 5300 410 770 31 5.4 6.5 L	11 22 550 33000 0.12 L 550 6200 380 500 37 5	10 13 450 32000 0.28 L 500 5200 360 370 24 4.6	11 21 1100 33000 0.48 590 5300 370 370 36 6.1 5.8 L	11 16 600 33000 0.16 L 500 5000 380 380 25 5.5	12 11 310 34000 0.25 510 5500 390 540 24
6 360  7 360  Mb 0.2  7 59  Mh 55  Na 56  Sh 1  Zn	20 630 000 27 L 700 900 550 520 32 5.9 U U 110 81	16 520 33000 0.13 L 560 5200 400 26 2.9 U	21 720 34000 0.14 L 540 5600 400 500 33 4.9 U	22 910 34000 U 630 5300 380 510 31 4.9 U U	23 620 33000 0.32 L 560 6500 440 41 4.9	22 620 35000 0.3 L 600 5400 410 440 37 4.8 U	18 700 35000 0.17 L 590 5300 410 770 31 5.4 6.5 L	22 550 33000 0.12 L 550 6200 380 500 37 5	13 450 32000 0.28 L 500 5200 360 370 24 4.6	21 1100 33000 0.48 590 5300 370 370 35 6.1 5.8 L	16 600 33000 0.16 L 500 5000 380 380 25 5.5	34000 0.25 510 5500 390 540 24
Fe* 360  TO 36	630 000 27 L 700 900 550 520 32 5.9 U U 110 81	520 33000 0.13 L 560 5200 400 26 2.9 U 94 74	720 34000 0.14 L 540 5600 400 500 33 4.9 U	910 34000 U 630 5300 380 510 31 4.9 U U	620 33000 0.32 L 560 6500 440 41 4.9	620 35000 0.3 L 600 5400 410 440 37 4.8 U	700 35000 0.17 L 590 5300 410 770 31 5.4	550 33000 0.12 L 550 6200 380 500 37 5	450 32000 0.28 L 500 5200 360 370 24 4.6	1100 33000 0.48 590 5300 370 370 35 6.1 5.8 L	600 33000 0.16 L 500 5000 380 380 25 5.5	310 34000 0.25 510 5500 390 540 24
Fe* 360  10 0.2  7  10 59  10	000   27 L   700   900   550   520   32   5.9   U   U   110   81	33000 0.13 L 560 5200 400 400 26 2.9 U 94 74	34000 0.14 L 540 5600 400 500 33 4.9 U	34000 U 630 5300 380 510 31 4.9 U	33000 0.32 L 560 6500 440 440 41 4.9	35000 0.3 L 600 5400 410 440 37 4.8 U	35000 0.17 L 590 5300 410 770 31 5.4 6.5 L	33000 0.12 L 550 6200 380 500 37 5	32000 0.28 L 500 5200 360 370 24 4.6	33000 0.48 590 5300 370 370 35 6.1 5.8 L	33000 0.16 L 500 5000 380 380 25 5.5	34000 0.25 510 5500 390 540 24
Mi	27 L 700 900 550 520 32 5.9 U U 110 81	0.13 L 560 5200 400 400 26 2.9 U U 94 74	0.14 L 540 5600 400 500 33 4.9 U	U 630 5300 380 510 31 4.9 4.9 L	0.32 L 560 6500 440 440 41 4.9 U	0.3 L 600 5400 410 440 37 4.8 U	0.17 L 590 5300 410 770 31 5.4 6.5 L	0.12 L 550 6200 380 500 37 5	0.28 L 500 5200 360 370 24 4.6	0.48 590 5300 370 370 35 6.1 5.8 L	0.16 L 500 5000 380 380 25 5.5	0.25 510 5500 390 540 24 4.3
7	700 900 550 520 32 5.9 U U 110	560 5200 400 400 26 2.9  U	540 5600 400 500 33 4.9 U	630 5300 380 510 31 4.9 4.9 L U	560 6500 440 440 41 4.9 U	600 5400 410 440 37 4.8 U	590 5300 410 770 31 5.4 6.5 L	550 6200 380 500 37 5	500 5200 360 370 24 4.6	590 5300 370 370 35 6.1 5.8 L	500 5000 380 380 25 5.5	510 5500 390 540 24 4.3
Min 59 Min 55 Na 5 Ni	900 550 520 32 5.9 U U 110 81	5200 400 400 26 2.9 U 94 74	5600 400 500 33 4.9 U	5300 380 510 31 4.9 4.9 L U	6500 440 440 41 4.9 U	5400 410 440 37 4.8 U	5300 410 770 31 5.4 6.5 L	6200 380 500 37 5	5200 360 370 24 4.6	5300 370 370 35 6.1 5.8 L	5000 380 380 25 5.5 5.3 L	550C 39C 54C 24 4.3
Mh 5 Na 5 Ni 5 Ni 7 Pb 9 Sb 5 Sn 7 Zn	550 520 32 5.9 U U 110 81	400 400 26 2.9 . U U 94 74	400 500 33 4.9 U	380 510 31 4.9 4.9 L U	440 440 41 4.9 U	410 440 37 4.8 U	410 770 31 5.4 6.5 L	380 500 37 5 4.5 L	360 370 <b>24</b> 4.6	370 370 35 6.1 5.8 L	380 380 25 5.5 5.3 L	390 540 24 4.3
Na 5 Ni Pb 9 Sb 9 Sb 9 Sh 7 Zn 7 Co-60 0.2 Cs-137 0.2 Pb-212 0.5 Pb-214 0.4 Ra-224 0.5 Ra-226 0.3 Ru-106 -0.09 Sb-125 -0.00	520 32 5.9 U U 110 81	400 26 2.9 . U U 94 74	500 33 4.9 U	510 31 4.9 4.9 L U	440 41 4.9 U	440 37 4.8 U	770 31 5.4 6.5 L	500 37 5 4.5 L	370 24 4.6 U	370 36 6.1 5.8 L	380 25 5.5 5.3 L	540 24 4.3
Ni Pb 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	32 5.9 U U 110 81	26 2.9 . U U 94 74	33 4.9 U U 96	31 4.9 4.9 L U	41 4.9 . U	37 4.8 U	31 5.4 6.5 L	37 5 4.5 L	24 4.6 U	35 6.1 5.8 L	25 5.5 5.3 L	4.5
Pb	5.9 U U 110 81	2.9 . U U 94 74	4.9 U U 96	4.9 4.9 L U 100	4.9 U	4.8 U U	5.4 6.5 L	5 4.5 L	4.6 U	6.1 5.8 L	5.5 5.3 L	4.3
Sb Sn V 1 Zn P Co-60 0.2 Cs-137 0.2 Pb-212 0.5 Pb-214 0.4 Ra-224 0.5 Ra-226 0.3 Ru-106 -0.09 Sb-125 -0.00	U U 110 81	. U U 94 74	U U 96	4.9 L U 100	U	U U	6.5 L	4.5 L	U	5.8 L	5.3 L	
Sn V 1 Zn P Co-60 0.2 Cs-137 0.2 Pb-212 0.5 Pb-214 0.4 Ra-224 0.5 Ra-226 0.3 Ru-106 -0.09 Sb-125 -0.00	U 110 81	94 74	U 96	U 100	U	U						
V 1 Zn	110 81	94 74	96	100			U	U	U	U	U	
Zn PC-60 0.2 Cs-137 0.2 Pb-212 0.5 Pb-214 0.4 Ra-224 0.5 Ra-226 0.3 Ru-106 -0.09 Sb-125 -0.00	81	74	· · · · · · · · · · · · · · · · · · ·		92	110						
PCO-60 0.2 Cs-137 0.2 Pb-212 0.5 Pb-214 0.4 Ra-224 0.5 Ra-226 0.3 Ru-106 -0.09 Sb-125 -0.00			83			110	92	100	96	100	100	92
Co-60 0.2 Cs-137 0.2 Pb-212 0.5 Pb-214 0.4 Ra-224 0.5 Ra-226 0.3 Ru-106 -0.09 Sb-125 -0.00	pCi/g	- 0:1-		86	76	80	82	77	72	410	76	72
Cs-137 0.2 Pb-212 0.5 Pb-214 0.4 Ra-224 0.5 Ra-226 0.3 Ru-106 -0.09 Sb-125 -0.00		pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCì/g	pCi/g	pCi/g	pCi/
Pb-212 0.5 Pb-214 0.4 Ra-224 0.5 Ra-226 0.3 Ru-106 -0.09 Sb-125 -0.00	249	0.208	0.319	0.25	0.255	0.239	0.308	0.187	0.254	0.323	0.278	0.24
Pb-214 0.4 Ra-224 0.5 Ra-226 0.3 Ru-106 -0.09 Sb-125 -0.00	.251	0.209	0.281	0.199	0.253	0.243	0.312	0.221	0.259	0.331	0,276	0.23
Ra-224 0.5 Ra-226 0.3 Ru-106 -0.09 Sb-125 -0.00	565	0.61	0.775	0.662	0.588	0.614	0.654	0.628	0.717	0.803	0.766	0.674
Ra-226 0.3 Ru-106 -0.09 Sb-125 -0.00	417	0.375	0.417	0.462	0.465	0.456	0.42	0.39	0.351	0.476	0.558	0.472
Ru-106 -0.09 Sb-125 -0.00	568	0.614	0.779	0.666	0.592	0.618	0.657	0.632	0.72	0.808	0.771	0.679
Ru-106 -0.09 Sb-125 -0.00	375	0.455	0.424	0.388	0.496	0.39	0.399	0.43	0.355	0.433	0.418	0.439
Sb-125 -0.00	97 U	0. <b>008</b> U	-0.13 U	0.15 U	-0.03 U	-0.04 U	0.039 U	-0.015 U	0.0414 U	-0.016 U	-0.14 U	-0.108
	07 U	0.026 U	0.006 U	0.005 U	-0.07 U	-0.05 U	-0.029 U	-0.013 U	0.0558	-0.01 U	0.12	-0.0176
l b	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/g	pCi/
	23.8	4,07	14.9	23.5	9.61	6.19	17,9	9.63	16,8	4.62	4.18	9,3
	ng/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg	mg/k
Arocior-1016	U	U	U	U	U	U	U	U	U	U	Ų	
	υ	Ü	Ŭ	U	ł-	U	U	U	U	U	U	
Aroclor-1221	U	U	U	<u> </u>	U	U	U	U	U	U	U	
Aroclor-1232		U	1 0	U	U	U	U	U	U	U	U	
Aroclor-1242	U		<del> </del>		<del>-</del>			0.33	0.28	0.44	0.27	
	0.26	0.27	0.28	0.34	0.19	0.3 U	0.32 U	0.33 U	U.28	U.44 U	U.27	0.2
Aroclor-1254 Aroclor-1260	c	U	U	U	υ		ı V		, ,	U	U	

U=Analyzed for but undetected Q=Data can be used qualitatively

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	MINUS 0.425mm SLURRY		
		BER 1993 PROCESSING	,
	B07DS7 soil	B07DS8 soil	B07DS9 soil
	mg/kg	mg/kg	mg/kg
Ag	3.2	6.6	4.4
Al	8600	7800	7200
Ва	330	240	90
Ве	U	U	0.13
Ca	5500	4600	5100
Çd	U	U	
Co	7.5	7.6	8.3
Cr	54	46	24
Cu	360	700	680
Fe	25000	24000	24000
Hg	0.43	0.31 L	. 1
К	730	730	590
Mg	4100	4100	4300
Mn	250	300	310
Na	450	330	320
Ni	38	42	35
Ръ	16	16	6.9
Sb	U	U	
Sn	11	9.5 L	
v	71	68	73
Zn	52	92	83
	pCi/g	pCi/g	pCi/
Co 60	0.0412	0.255	0.431
Co-60	0.212	0.287	0.322
Cs-137	1.21	1.07	0.868
Pb-212	0.822	0.657	0.564
Pb-214		1.07	0.872
Ra-224	1.21		0.554
Ra-226	-0.285 U	0.622 -0. <b>292</b> U	-0.0898
Ru-106			0.0302
Sb-125	0.0271 U	0.0179 U	
	pCi/g	pCi/g	pCi/
U-Nat	115	134	31.9
	mg/kg	mg/kg	mg/k
Arocior-1016	U	U	
Aroclor-1221	U	U	
Aroclor-1232	U	U	
Aroclor-1242	υ	U	
Aroclor-1248	0.97	0.66	0.39
Aroclor-1254	υ	U	
Aroclor-1260	U	U	

U=Analyzed for but undetected Q=Data can be used qualitatively

				L WASHING RE 25 SLURRY WA				
			s	EPTEMBER 199	3 PROCESSING			
	BO7DT2	B07DT3	B07DT4	B07DT5	BO7DT6	BO7DT7	BO7DT8	807DV0
	water-uf	water-f	water-uf	water-f	water-uf	water-f	water-uf	water-uf
	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L
Ag	0.033	U	0.023	0.0042 L	0.014 L	U	0.0079 L	0.0076 L
Al	28	0.15 L	15	U	12	0.044 L	4.4	4.8
Ва	1.9	0.063	0.22	0.043	0,16	0.025	0.076	0,082
Be	U	0.0011 L	U	U	U	U	υ	U
Са	33	19	26	29	27	23	24	25
Cd	υ	υ	U	υ	U	U	U	U
Co	0.0064 L	υ	0.0074 L	U	0.006 L	U	U	U
Cr	0.27	5	0.097	٥	0.048	0.0066 L	0.019 L	0.022
Cu	3.8	0.019 L	1.7	0.039	0.71	0.029	0.24	0.33
Fe	18	0.059	11	0.056	11	0.077	3.3	3.5
Hg	0.0031	U	0.0019	U	0.0031	U	0.00047	0.00035
К	3.4	1.2	4.1	2.8	4.2	2.4	3.5	3.9
Mg	11	4.9	8.9	4.3	8.6	5.1	6.3	6.2
Mn	0.32	0.0051 L	0.27	0.02	0.26	0.015	0.068	0.092
Na	15	13	7.6	5.4	6	5.1	5.4	5.2
Ni	0.3	U	0.098		0.044	U	0.02 L	U
Pb	0.065	0.0006 L	0.013	u	0.0088	0.0012 L	0.0021 L	0.0035 L
Sb	U	υ	υ	U	U	U	U	U
Sn	U	U	U	U	U	U	U	U
V	0.017 L	U	0.02 L	U	0.022 L	U	0.0083 L	0.0092 L
Zn	0.18	U	0.079	Ü	0.052	0.0065 L	0.017	0.02
	<del></del>		I I					
Co-60	pCi/L 3.67 U	pCi/L -4.81 U	pCi/L -1.39 U	PCi/L -8,24 U	pCi/L -4.55 U	pCi/L -4,37 U	pCi/L 5.28 U	-7,29 U
	<del>-</del>							
Ca-137	2.26 U	-1.47 U	-7.4 U	-2.24 U	5.56	3.64 U	-4.72 U	-2.6 U
Ru-106	-2.91 U	5.8 U	25.1 U	-26.5 U	10.9 U	0 U	27.8 U	13 U
Sb-125	13.2 U	12.6	7. <b>7</b> 3 U	-4.7 U	-7.22 U	-18.4 U	14.4 U	-5.76 U
	ug/L	ug/L	ug/L	ug/L	ug/L	ug/L	ug/L	ug/L
U-Nat	2.68	19.7	664	510	3.16	3.68	1.49	10.9
	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L
Aroclor-1016	U	υ	U	Ú	U	U	υ	U
Aroclor-1221	U	U	U	U	U	U	U	U
Aroclor-1232	U	U	υ	U	U	C	U	U
Aroclar-1242	U	υ	U	U	υ	U	υ	U
Aroclor-1248	0.0013	U	0.00075 L	υ	0.00028 L	U	0.00025 L	0.00021 L
Aroclor-1254	U	υ	υ	U	U	U	U	U
Aroclor-1260	U		U	U	U	U	U	U

U=Analyzed for but undetected Q=Data can be used qualitatively uf=unfiltered f=filtered (0.2 μ)

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			TEST #2	SOIL WAS	HING RESU	JLTS				
				SEPTE	MBER 1993	PROCESS	ING			<del> </del>
	FRESH_WA	TER		INUS 0.4	25mm SLUE	RY WATER			BLANKS	
	807DQ4 water-uf	B07DX8 dupuf	B07DT2 water-uf	B07DT4 water-uf	B07DT6 water-uf	B07DT8 water-uf	B07DV0 water-uf	full blk	BO7DY2 trp blk	BO7DY3 trp blk
	mg/L	mg/L	mg/L	mg/L	mg/L	mg/i.	mg/L	mg/L	mg/L	mg/L
1,1,1-Trichloroethane	U	0.0018 L	U	0.0028 L	υ	U	0.0029 L	U	U	U
1,1,2-Trichloroethane	U	U	U	U	U	U	U	U	U	U.
1,1-Dichloroethane	υ	U	U	U	U	U	U	U	υ	U
1,2-Dichloroethane	U	U	U	U	υ	U	U	U	U	U
1,2-Dichloroethene	U	U	U	υ	U	U	υ	U	U	U
1,4-Dichlorobenzene	U	U	U	U	U	Ų	U	U	U	υ
1-Butanol	U	υ	U	U	U	U	U	U	υ	U
4-Methyl-2-pentanone	U	U	U	U	U	υ	υ	U	υ	U
Acetone	U	U	U	V	U	ប	U	U	U	U
Benzene	Ų	U	υ	Ų	U	U	U	υ	Ų	υ
Carbon disulfide	U	U	U	Ų	. U	U	U	U	Ų	υ
Carbon tetrachloride	U	υ	υ	U	כ	U	U	U	υ	U
Chloroform	0.0074	0.0069	υ	U	ט	U	U	٥	U	U
Ethyl cyanide	U	U	υ	U	J	U	U	υ	U	U
Methyl ethyl ketone	U	U	0.05	U	U	U	U	U	U	U
Methylene chloride	U	U	U	U	U	U	U	υ	υ	U
Tetrachioroethene	υ	U	U	U	υ	U	U	U	U	υ
Tetrahydrofuran	υα	0.007 LQ	0.042	0.018	0.011	0.0084 L	0.0074 L	٥	U	U
Toluene	U	U	U	C	5	U	υ	υ	V	U
Trichloroethene	υ	U	0.00092	U	υ	U	υ	υ	U	υ
Vinyl chloride	U	U	U	U	U	U	U	U	U	Ų
Xylenes (total)	U	U	υ	U	U	U	U	U	υ	U

L=Less than the CRDL and above the MDL

U=Analyzed for but undetected Q=Data can be used qualitatively uf=unfiltered f=filtered (0.2 μ)

Ag Al		SEPTEMBER 100		TEST #2 SOIL WASHING RESULTS TRIP BLANKS									
		TELLIBER 177	3 PROCESSING										
	B07DY5 soit mg/kg	B07DY6 soil mg/kg	BO7DYO water mg/L	807DY1 water mg/L									
_AI	U	U	0.0034 L	0.0029 L									
	69 Q	D 08	U	U									
Ва	0.28 LQ	0.33 LQ	0.00023 LQ	0.00046 LQ									
8e	U	U	U	U									
Ca	14 Q	14 Q	0.039 L	0.03 L									
Cd	U	U	U	U									
Co	U	U	U	0.0063 L									
Cr	υ	. U	U	<u> </u>									
Cu	1.1 L	U	Ú	U									
Fe	140 Q	150 Q	U	U									
Hg	U	U	U	U									
K	51 L	υ	0.88 L	0.82 L									
Mg	7.2 LQ	6.9 LQ	υ	U									
Mn	0.67 LQ	0.38 LQ	U	U									
Na	U	25 L	U	· U									
Ni	υ	υ	U	U									
Pb	. U	U	0.0031 L	0.0007 L									
Sb	U	U	U	Ų									
Sn	υ	U	U	U									
V	U	0.64 L	U	U									
Zn	0.63 L	0.7 L	U	U									
	pCi/g	pCi/g	pCi/L	pCi/L									
Co-60	-0.008 U	-0.006 U	-6.94 U	4.51 U									
Cs-137	0.012 U	-0.01 U	2.29 U	1.55 U									
Pb-212	0.0765	0.0852	16.7 U	44.5									
Pb-214	0.115	0.0949	4.41 U	-0.157 U									
Ra-224	0.077	0.0858											
Ra-226	0.151	0.0917											
Ru-106	-0.002 U	0.004 U											
Sb-125	-0. <b>042</b> U	0.016 U											
	pCi/g	pCi/g	ug/L	ug/L									
U-Nat	-0.232 U	-0.187 U	0.0675 U	0.0713 U									
	mg/kg	mg/kg	mg/L	mg/L									
Aroclor-1016	U	U	U	U									
Aroclor-1221	U	U	U	U									
Araclor-1232	U	U	U	υ									
Aroclor-1242	υ	U	U	U									
Aroclor-1248	U	U	U	U									
Aroclor-1254	U	U	υ	U									
Aroclor-1260	U	U	U	U									

U=Analyzed for but undetected Q=Data can be used qualitatively L=Less than CRDL and above the MDL

WHC HASM 345-H1<u>1113</u>

DOE/RL-93-96, Rev. 0

000015

THA Inc.

REPORT

Work Order # A3-09-023

: Received: 09/13/93

SAMPLE 10 809757

Results by Sample

FRACTION <u>01A</u> TEST CODE <u>TCV1</u> NAME <u>TCLP Volatiles Fors 1</u>
Date 2 Time Collected <u>09/08/95</u> Category

### TCLP VOLATILE ORGANICS

Sample Matrix (soil/water): 501L Lab File 10: 30917M06
Leschate vol analyzed (mt): 1 TCLP Extraction Date: 09/15/93
Date Received: 09/13/93 Date Leschate Extracted: 5
Lab File 10: 30917M06
Date Analyzed: 09/13/93 Date Leschate Extracted: 5
Lab File 10: 30917M06
Date Analyzed: 09/13/93 Date Leschate Extracted: 5
Lab File 10: 30917M06

CAS No.	COMPOUND	RESULT (mg/l)	PQL (mg/L)
71-43-2	Banzene	ΩK	0.025
56-23-5	Carbon Tetrachloride	чр	0.025
108-90-7	Chlarobenzene	ОИ	0.025
67-66-3	Chloroform	HD	0.025
107-06-2	1,2-Dichloroethane	нр	0.025
75-35-4	1,1-Dichloroethylene	ND	0.025
78-93-3	Nethyl Ethyl Ketone	ΝĐ	0.050
127-18-4	Tetrachioroethylene	KD	0.025
79-01-6	Trichloroethylene	ИО	0.025
75-01-4	Vinyl Chloride	ND	0.050

### % RECOVERY SURROGATE COMPOUND

d8-Toluene 95

Bromofluorobenzene \_\_\_\_95

1,2-Dichtoroethane-d4 \_\_\_\_99

FORH I

B.2-11

141

000071

THA Inc.

14:55

REPORT

Work Order & 43-09-023

Category \_\_\_\_

Ésceived: 09/13/93

SAMPLE TO BUSTST

Results by Sample

FRACTION OID TEST CODE ICS! HAHE ICLP Seri-Volatiles Form 1

Date & Fime Collected 09/08/93

TCLP SEMI-VOLATILE ORGANICS

Sample Matrix: SOIL Leachate vol (ml): 100

Lab file ID: 30922503 TCLP Extraction Date: 09/15/93

Date Received: 09/13/93\_\_\_

Date Leachate Extracted: 09/20/93

Conc. Extract Vol.(mL): 2\_\_\_

Date Analyzed: 09/22/93

injection Volume (uL): 1

Dilution Factor: \_\_\_\_\_\_20

Instrument ID: SEFPKA

CAS RO.	COMPOUND	RESULT (mg/L)	PCL (mg/L)
. 1319-77-3	C:esol (Total)	<b>D</b> K	0.1
87-86-5	Pentachlorophenol	ND	0.5
95-95-4	2,4,5-Trichlorophenol	ИĎ	0.1
88-96-2	2,4,6-Trichlorophenol	GK	0.1
106-46-7	1,4-Dichlorobenzene	NO	0.1
121-14-2	Z,4-Dinitrotoluene	HD	0.1
118-74-1	Hexachtorobenzene	МО	0.1
87-68-3	Hexachierobutadiena	HD	0,1
67-72-1	Hexachloroethane	פא	0.1
98-95-3	Hitrobenzene	NO	0.1
110-26-1	Pyridine	N D	0.2

% RECOVERY SURROGATE COMPOUND

2-Fluorophensi

Phenol-d5 66 68

2,4,6-Tribromophenal Witrobentane-d5

2. Fluorabiphenyl

Terphonyl-d14

FORM 1

000131

TKA Inc.

REPORT

Work Order # A3-09-023

'Received: 09/13/93

Results by Sample

SAMPLE ID COSTST

FRACTION 010 TEST CODE TCP1 NAME TOLP PERTICIDES FORE 1

Date & Time Collected 09/08/93 Category

### JCLP CHLORINATED PESTICIDES

Sample Matrix: SOIL
Leachete vol (mL): 10D
Date Received: 09/13/93
Camp. Lancet. Necessary: 10
Injection Volume (uL): 1
Column 10: 22-1701
Lab File 10: Bi10025
TCLP Extraction Date: 09/15/93
Date Leachete Extracted: 09/20/93
Date Analyzed: 10/10/93
Dilution Fector: 1

CAS No.	COMPOUND	RESULT (mg/L)	PQL (mg/L)
57-74-9	Chlordane	ОК	0.005
72-20-8	Endrin	но	0.001
76-44-8	Haptachior	ND	0.0005
1024-57-3	Reptachlor Epoxida	МO	0.0005
58-89-9	Lindane	ир	0.0005
72-43-5	Methoxychlor	ИÖ	0.005
8001-35-2	Toxaphene	ND	0.020

### X RECOVERY SURROGATE COMPOUND

oca <u>54</u>

FORM I

THA Inc.

14:55

REPORT

Vort Ordar € #3-09-023

"geceived: 09/13/93

SAMPLE 10 809757

Results by Sample

FRACTION OID TEST CODE TOHT HAME TELP METDICIDES FORM 1 Date & Time Collected 09/08/93

TOLP CHLORINATED HERBICIDES

Cample Matrix (soft/water): SOIL

Lab File ID: AJ11013

Leachate vol (mt): [7] TCLP Extraction Date: 09/15/93

Date Received: 09/13/93 Date Leachete Extracted: 09/28/93

Conc.Extract Vol.(mL): 2.5

Date Analyzed: 10/11/93

Injection Volume (uL): 1

Dilution Factor: \_\_\_\_\_1

Column ID: 08-608

ÇAS No.	COMPOUND	RESULT (mg/L)	PQL (mg/L)
94-75-7	2,4-0	ИD	0.01
93-72-1	2,4,5-TP	ND	0.001

X RECOVERY SURROGATE COMPOUND

DCAA 90

FORM I

000375

THA Inc.

14:55

REPORT

Work Order # A3-09-023

\* Recolved: 09/12/93

Results by Sampla

SAMPLE 10 809757

FRACTION 315 TEST CODE TONT - MAKE TOLD Form 1 Date & Time Collected 09/08/93

### TCLP METALS

Sample Matrix: 5011

TELP Extraction Date: 09/15/93

Date Reseived: 09/13/93

CAS No.	СОМРОИНО	RESULT (mg/L)	PQL (mg/L)	METHOD
7440-38-2	Artenic	0.003	0.001	F
7440-39-3	Bentum	2.65	0.001	P
7440-43-9	Cadmium	0.008	0.007	Р
7440-47-3	Chromium	0.057	0.006	Р
7439-92-1	Lead	0.019	0.001	F
7439-97-6	Hercury	0.0030	0.0002	cv
7782-49-2	setenium	ИD	0.002	F
7440-22-4	Silver	0.07	0.01	Α.

Analytical Hethods Used:

P . ICP A = Flame AA

CV = Cold Vapor AA

FORM (

From: Geochemistry & Hydrochemistry

Phone: 376-3324

Date: December 1, 1993

Subject: DATA VALIDATION OF 300-FF-1 SOIL WASHING COLLECTED SEPTEMBER 1993

To: R. D. Belden

cc: J. C. Johnston

D. G. Horton

This report is to document the validation of 300-FF-1 Soil Washing data collected during September 1993. The validation was based on WHC-CM-7-8 manual "Environmental Engineering and Geotechnology Function Procedures" (WHC 1992) and the "Annual Report for RCRA Groundwater Monitoring Projects at Hanford Site Facilities for 1992" Appendix B DOE/RL-93-09 (DOE-RL, 1993a).

The data were collected, analyzed and processed in a similar manner as the Resource Conservation and Recovery Act (RCRA) groundwater monitoring projects. The analytical laboratories utilized were Datachem Laboratory, Salt Lake City Utah and International Technology Analytical Services, Richland, Washington. Data validation was performed by Ms. P.B. Freeman, RCRA Sampling and Analysis Task Leader. A electronic copy of the data is provide in both paradox and lotus format. Hardcopies of data were provided prior to this report.

Data validation consisted of seven parts:

- a. 100% verification that requested data were received.
- b. 100% verification that holding times were meet.
- c. 100% evaluation of precision with field duplicates
- d. 100% evaluation of potential sample contamination with field blank data.
- e. 100% evaluation of laboratory MS/MSD and surrogate data , through laboratory incident reports.
- f. 100% evaluation of laboratory blanks.
- g. 100% evaluation of data completeness.

The outcome of the validation:

Part a: All data requested were received.

Part b: All analytical holding times were meet.

Part c:

1 .

Evaluation of Duplicate data was performed using procedure 2.1 "Evaluation of RCRA Groundwater Field Duplicate and Blank Sample Data" (WHC 1992) and using Appendix B (DOE-RL 1993).

There were two duplicate pairs evaluated. The paired sample numbers are BO7DX9 with BO7DQ5 and BO7DX8 with BO7DQ4, respectfully. The evaluation of BO7DX9 and BO7DQ5 resulted in three constituents which exceeded a required 25% relative percentage difference (WHC 1992) and were above the limit of detection as defined in Appendix B (DOE-RL 1993). The three constituents are copper, potassium and silver. All of these were analyzed by ICP metal method SW-846 6010.

The evaluation of B07DX8 and B07DQ4 resulted in twelve constituents which exceeded a required 25% relative percentage difference (WHC 1992) and were above the limit of detection as defined in Appendix B (D0E-RL 1993). The twelve constituents are: total uranium, tetrahydrofuran, barium, calcium, copper, magnesium, manganese, potassium, silver, sodium, zinc and lead. Uranium was analyzed by an inhouse method. Tetrahydrofuran was analyzed by method SW-846 8240. Lead was analyzed by method SW-846 7421 and the rest were analyzed by method SW-846 6010.

As a result of this evaluation all data associated with these sample numbers and constituents are flagged with a validation flag of Q. The Q-flagged data can be used qualitatively, but not regulatory decisions should be made based on a single flagged data point.

Part d: Evaluation of field blank data was performed using procedure 2.1 "Evaluation of RCRA Groundwater Field Duplicate and Blank Sample Data" (WHC 1992) and using Appendix B (DOE-RL 1993).

There were two water blanks and two soil blanks collected during the September 1993 sampling. The blanks exceeding two times the method detection limit (MDL) were flagged with a Q (WHC 1992). MDL are defined in Appendix B (DOE-RL 1993). The sample numbers for the water blanks are BO7DYO and BO7DY1. Each sample had one the same constituent exceed two times the MDL. The constituent was barium which is analyzed by method SW-846 6010. The sample numbers for the soil blanks are BO7DY5 and BO7DY6. Each sample had the same six constituents exceed two times the MDL. The constituents were aluminum, iron, magnesium, manganese, barium and calcium. These constituents were analyzed by method SW-846 6010.

As a result of this evaluation the above constituents associated with the collect and analyze dates of these sample numbers and constituents are flagged with a validation flag of Q. The Q-flagged data can be used qualitatively, but not regulatory decisions should be made based on a single flagged data point.

Part e: There were not laboratory incident reports for this data. Therefore, no matrix spike, matrix spike duplicate or surrogate samples associated with these samples exceeded laboratory acceptance criteria.

Part f: There were no "B" qualifiers associated with these data, therefore no laboratory blanks exceeded laboratory acceptance criteria.

Part g: The data completeness is determined after data validation is completed and is calculated by the number of unflagged divided by the total number of validated data expressed as a percentage. The RCRA using a 80% acceptance guidance. The total number of soil data are 1122 constituents and water data are 683 constituents. The total unflagged soil data are 918 constituents and water data are 639 constituents. The calculated completeness for soil and water data are 82% and 93%, respectfully. These data are within acceptable completeness criteria.

### References:

- DOE-RL, 1993, Annual Report for RCRA Groundwater monitoring Projects at Hanford Site Facilities for 1992, DOE/RL-93-09, U.S. Department of Energy, Richland Operations Office, Richland, Washington.
- WHC, 1992, Environmental Engineering and Geotechnology Function Procedures, WHC-CM-78, vol. 4, Westinghouse Hanford Company, Richland, Washington.

P. B. Freeman RCRA Sampling and Analysis Task Team Leader

pbf

# B.3 ANALYTICAL DATA FOR WATER TREATMENT

# DATA QUALIFIERS FOR ANALYTICAL DATA FOR WATER TREATMENT SAMPLES

- U Indicates that this constituent was analyzed for but undetected.
- P Indicates there is greater than 25% difference for detected concentrations between the two Gas Chromatagraph columns. The lower value is reported.
- J Indicates the result reported is below the contract quantitation limit.

	<del></del>		WATER	TREATMENT	RESULTS					· · · · · · · · · · · · · · · · · · ·
		Influent			Eff	luent		T	rip Blank	s
Constituents	BO9BR4 water mg/L	B09BR6 water mg/L	B09BR7 water mg/L	B09BR5 water mg/l	BO9BR8 water mg/L	BO9BR9 water mg/L	B09BS0 dup. mg/L	BO9BW2 water mg/L	B09BW5 water mg/L	BO9BW8 water mg/L
Ag	0.005	0.0037	0.0056	0.005	0.0037	0.0037	0.0037	N/A	N/A	N/A
Al	1.340	0,0422	0.291	0.155	0.104	0.103	0.078	N/A	N/A	N/A
As	0.0021	0.0022	0.0046	0.0021	0.0021	0.0027	0.0021	N/A	N/A	N/A
Ва	0.0873	0.061	0.0698	0.0629	0.0343	0.0533	0.0533	N/A	N/A	N/A
Ве	0.0002	0.0002	0.0002	0.0002	0.0002	0.0002	0.0002	N/A	N/A	N/A
Ca	19.3	19.8	20.7	19.5	9.79	15.5	15.1	N/A	N/A	N/A
Cd	0.001	0.0026	0.001	0.001	0.001	0.0019	0.0016	N/A	N/A	N/A
Со	0.003	0.003	0.003	0.003	0.003	0.003	0.003	N/A	N/A	N/A
Cr	0.0061	0.0041	0.0077	0.0041	0.0041	0.0041	0.0041	N/A	N/A	N/A
Cu	0.345	0.013	0.252	0.160	0.0131	0.0389	0.0341	N/A	N/A	N/A
Fe	42.1	0.549	47.8	41.4	0.762	4.52	3.33	N/A	N/A	N/A
Нд	0.0003	0.0002	0.0002	0.0002	0.0002	0.0002	0.0002	N/A	N/A	N/A
K	1.84	1.68	1.86	1.77	1.9	1.67	1.71	N/A	N/A	N/A
Mg	4.77	4,68	4.62	4.43	3.02	3,82	3.74	N/A	N/A	N/A
Mn	0.22	0.0832	0.269	0.218	0.0157	0.121	0.118	N/A	N/A	N/A
Na	21.9	22.7	22.4	22.0	38.2	29.7	29.0	N/A	N/A	N/A
Ni	0.0443	0.0119	0.0344	0.0272	0.0039	0.0136	0.0126	N/A_	N/A	N/A
Pb	0.216	0.0064	0.0628	0.0562	0.0043	0.0066	0,0048	N/A	N/A	N/A
Sb	0.023	0.0218	0.0123	0.0298	0.0092	0.0092	0.0092	. N/A.	N/A	N/A
Se	0.0028	0.0028	0.0028	0.0028	0.0028	0.0028	0.0028	N/A	N/A	N/A
Τl	0.0016	0.0028	0.0016	0.0016	0.0016	0.0021	0.0023	N/A	N/A	N/A
V	0.004	0.0026	0.0032	0.0026	0.0026	0.0026	0.0026	N/A	N/A	N/A
Zn	1.22	0.199	1.2	1.72	0.0839	0.232	0.353	N/A	N/A	N/A

 $\ensuremath{\text{N}/\text{A}}$  - Analysis is Not Applicable for Trip Blanks

DOE/RL-93-96, Rev. 0

			WATER	TREATMENT	RESULTS			• • •		
	Influent			Effluent				Trip Blanks		
Constituents	B09BR4 water pCi/L	809BR6 water pCi/L	809BR7 water pCi/L	BO9BR5 water pCi/l	B09BR8 Water pCi/L	B09BR9 water pCi/L	B09BS0 dup. pCi/L	809BW2 water pCi/L	B09BW5 water pCi/L	B09BW8 water pCi/L
<sup>22</sup> Na	u	C	ับ	u	U	U	U	N/A	N/A	N/A
40 <sub>K</sub>	U	U	U	บ	U	U	U	N/A	N/A	N/A
54 <sub>Mn</sub>	U	U	U	U	U	U	U	N/A	N/A	N/A
<sup>59</sup> Fe	U	U	บ	υ	U	U	U	N/A	N/A	N/A
<sup>58</sup> co	U	U	U	U	u	U	U	N/A	N/A	N/A
60 <sub>Co</sub>	U	U	U	υ	u	U	U	N/A	N/A	N/A
94 <sub>NB</sub>	U	U	U	U	U	U	U	N/A	N/A	N/A
103 <sub>P11</sub>	U	U	Ü	Ü	Ü	Ų	U	N/A	N/A	N/A
_106 <sub>Ru</sub>	U	U	Ü	U	U	U	U	N/A	N/A	N/A
. 113 <sub>Sn</sub>	U	U	Ų	U	U	U	U	N/A	N/A	N/A_
*134 <sub>Cs</sub>	U	U	U	U	U	U	U	N/A	N/A	N/A
:::137 <sub>Cs</sub>	U	U	U	U	9.1	U	U	N/A	N/A	N/A
1144 <sub>Ce</sub>	U	U	Ų	U	U	Ū ·	U .	N/A	N/A	N/A
152 <sub>FU</sub>	U	U	U	U	U	U	U	N/A	N/A	N/A
[" 154 <sub>EU</sub>	U	U	U	U	U	U	U	N/A	N/A	N/A
155 <sub>Eu</sub>	U	u	U	U	U	υ	U	N/A	N/A	N/A
226 <sub>pa</sub>	U	U	U	U	Ü	Ų	U	N/A	N/A	N/A
228 <sub>Ra</sub>	U	U	U	U	U	U	U	N/A	N/A	N/A
228 <sub>Th</sub>	U	U	U	U	U	U	U .	N/A	N/A	N/A
232 <sub>Th</sub>	υ	U	U	u	U	υ	U	N/A	N/A	N/A
238 <sub>U</sub>	2000	ANP	1500	1400	900	5800	460	N/A	N/A	N/A

U - Analyzed for but undetected N/A - Analysis is Not Applicable for Trip Blanks ANP - Analysis was Not Possible due to sample size

1 . . .

WATER TREATMENT RESULTS										
	Influent				Eff	luent	Trip Blanks			
Constituents	BO9BR4 water mg/L	B09BR6 water mg/L	B09BR7 water mg/L	809BR5 Water mg/l	B09BR8 water mg/L	B09BR9 water mg/L	B09BS0 dup. mg/L	B09BW2 water mg/L	B09BW5 water mg/L	B09BW8 water mg/L
Chloromethane	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U					
Bromomethane	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U					
Vinyl Chloride	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U					
Chloroethane	0.01 U	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U
Methylene Chloride	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U				
Acetone	0.01 บ	0.009 J	0.01 U	0.01 U	0.01 บ	0.01 U	0.01 U	0.013	0.015	0.016
Carbon Disulfide	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U					
1,1-Dichloroethene	0.01 U	0.01 U	0.01 U	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U
1,1-Dichloroethane	0.01 U	0.01 U	0.01 บ	0.01 บ	0.01 U					
1,2-Dichloroethene (total)	0.01 U	0.01 U	0.01 U	0.01 U	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U
Chloroform	0.01 U	0.01 U	0.01 U	0.01 น	0.01 บ	0.01 U	0.01 U	0.01 บ	0.01 U	0.01 U
1,2-dichloroethane	0.01 U	0.01 U	0.01 U	0.01 บ	0.01 U					
2-Butanone	0.01 U	0.01 U	0,01 U	0.01 U	0.01 U					
1,1,1-Trichloroethane	0.01 U	0.01 U	0.01 U	0.01 U	0.01 น	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U
Carbon Tetrachloride	0.01 U	0.01 U	0.01 U	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U
Bromodichloromethane	0.01 U	0.01 U	0.01 U	0.01 บ	0.01 U					
1,2-Dichloropropane	0.01 U	0.01 U	0.01 U	0.01 U	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 บ	0,01 U
cis-1,3-Dichloropropene	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U				
Trichloroethene	0.01 U	0.01 U	0.01 U	0.01 ປ	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 U	0.01 บ
Dibromochloromethane	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U					
1,1,2,-Trichloroethane	0.01 U	0.01 U	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 U	0.01 บ	0.01 U	0.01 U
Benzene	0.01 U	0.01 U	0.01 U	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 U	ט 0.01	0.01 U
trans-1,3- Dichloropropene	0.01 U	0.01 U	0.01 U	0.01 ບ	0.01 U					
Bromoform	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U					
4-Methyl-2-Pentanone	0.01 U	0.01 U	0.01 <u>U</u>	0,01 U	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U	0.01 ป
2-Hexanone	0.01 U	0.01 บ	0.01 U	0.01 U	0.01 ប					
Tetrachloroethene	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 ป	0.01 U	0.01 U	0.01 U	0.01 U	0.01 ป
1,1,2,2- Tetrachloroethane	0.01 U	0.01 U	0.01 U	0.01 U	ט 0.01					
Toluene	0.01 บ	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U				
Chlorobenzene	0.01 U	0.01 U	0,01 ປ	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U
Ethylbenzene	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U					
Styrene	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U					
Xylene (total)	0.01 U	0.01 U	0.01 U	0.01 U	0.01 U					

 $<sup>\</sup>mbox{\bf U}$  - Analyzed for but undetected  $\mbox{\bf J}$  - Indicates the result reported is below the contract quantitation limit.

			WATER 1	TREATMENT	RESULTS					
	Influent				Effl	uent	Trip Blanks			
Constituents	B09BR4 water μg/L	BO9BR6 water μg/L	B09BR7 water μg/L	B09BR5 water μg/l	B09BR8 water µg/L	B09BR9 water μg/L	B09BS0 dup. #g/L	B09BW2 water µg/L	B09BW5 water µg/L	B09BW8 water µg/L
alpha-BHC	0.05 U	0.0 <u>5</u> U	0.05 U	0.05 U	0.05 U	0.05 U	0.05 U	N/A	N/A	N/A
beta-BHC	0.1 P	0.11 P	0.05 U	0.05 U	0.05 U	0.05 U	0.05 U	N/A	N/A	N/A
delta-BHC	0.05 υ	0.05 ป	0.05 U	0.05 U	0.05 U	0.05 U	0.05 U	N/A	N/A	N/A
gamma-BHC (Lindane)	0.05 U	0.05 U	N/A	N/A	N/A					
Heptachlor	0.26	1.8	0.82	0.38	0.096 P	0.61	0.97	N/A	N/A	N/A
Aldrin	0.05 U	0.05 U	N/A	N/A	N/A					
Heptachlor epoxide	0.05 U	0.05 บ	0.05 U	0.05 U	0.05 U	0.05 U	0.05 U	N/A	N/A	N/A
Endosulfan I	0.05 U	0.05 U	0.05 ປ	0.05 ນ	0.05 U	0.05 U	0.05 U	N/A	N/A	N/A
Dieldrin	0.1 U	0.1 U	N/A	N/A	N/A					
4,4'-DDE	0.1 U	0.1 U	0.1 U	0.1 U	0.1 บ	0.1 U	0.1 U	N/A	N/A	N/A
Endrin	0.1 U	0.1 U	N/A	N/A	N/A					
Endosulfan II	0.1 U	0.1 U	N/A	N/A	N/A					
4,4'=DDD	0.1 U	0.1 U_	0.1 U	0.1 U	0.1 U	0.1 บ	0.1 U	N/A	N/A	N/A
"Endosulfan sulfate	0.1 U	0.1 U	0.1 บ	0.1 U	0.1 U	0.1 U	0.1 U	N/A	N/A	N/A
4,41-DDT	0.1 U	0.1 U	0.1 บ	. 0.1 U	0.1 U	0.1 U	0.1 U	N/A	N/A	N/A
Methoxychlor	0.5 U	0.5 U	0.5 U	0.5 ປ	0.5 U	0.5 U	0.5 U	N/A	N/A	N/A
Endrin ketone	0.1 U	0.1 U	0.1 U	0,1 U	0.1 U	0.1 ป	0.1 U	N/A	N/A	N/A
Endrin aldehyde	0.1 U	0.1 U	N/A	N/A	N/A					
alpha-Chlordane	0.05 U	0.05 U	0.05 ປ	0.05 U	0.05 U	0.05 U	0.05 U	N/A	N/A	N/A
gamma-Chlordane	0.05 U	0.05 U	N/A	N/A	N/A					
Toxaphene	5.0 U	5.0 U	N/A	N/A	N/A					
Aroclor-1016	1.0 U	1.0 U	N/A	N/A	N/A					
Aroclor-1221	2.0 U	2,0 U	2.0 U	N/A	N/A	N/A				
Aroclor-1232	1.0 U	1.0 U	N/A	N/A	N/A					
Aroclor-1242	1.0 U	1.0 U	N/A	N/A	N/A					
Aroclor-1248	1.0 U	1.0 U	N/A	N/A	N/A					
Aroctor-1254	1.0 U	1.0 U	N/A	N/A	N/A					
Aroclor-1260	1.0 U	1.0 U	N/A	N/A	N/A					

1 1 ...

Analyzed for but undetected
 Indicates there is greater than 25% difference for detected concentrations between the two Gas Chromatagraph columns.
 The lower value is reported.

 N/A - Analysis is Not Applicable for Trip Blanks

## APPENDIX C

# VENDOR TEST

(To be included in Rev. 1 of this document)

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